

# Effective Diffusivity in Porous Materials

This example introduces the concept of effective diffusivity in porous media by comparing the transport through an artificial porous structure described in a detailed model with a simplified homogeneous porous media approach using effective transport properties.

The exercise consists of two parts. The first part describes how to create the model with a detailed geometry. The second part shows how to define a homogeneous model for porous media using an effective diffusivity calculated using the detailed model from the first part.

## Introduction

Transport through porous structures is usually treated using simplified homogeneous models with effective transport properties. This is in most cases a necessity, since the typical dimensions of the pores and particles making up the porous structure are several orders of magnitude smaller than the size of the domain that is to be modeled.

However, it might be interesting to investigate the assumptions and simplifications done when homogenizing a porous structure by comparing a homogeneous model with a model defined using the detailed structure.





Figure 1: Artificial porous structure. The domain colored in red is accessible for diffusion.

## Model Definition

The model equation in the modeled domain shown in Figure 1 is the time-dependent equation

$$\frac{\partial c}{\partial t} + \nabla \cdot (-D\nabla c) = 0$$

where *c* denotes concentration (mol/m<sup>3</sup> using SI units) and *D* the diffusion coefficient  $(m^2/s)$  of the solute.

The boundary conditions are of three different types. A concentration boundary condition applies at the left vertical boundary in Figure 1. It is expressed as

$$c = c_0$$

where  $c_0$  is a given concentration.

The right vertical boundary in Figure 1 is set according to

$$(-D\nabla c) \cdot \mathbf{n} = k_m(c-c_1)$$

where  $k_m$  is the mass transfer coefficient (m/s), and  $c_1$  is the concentration in a bulk solution outside of the porous structure.

All other boundaries are insulating boundaries according to

$$(-D\nabla c)\cdot \mathbf{n} = 0$$

The initial condition is given by a bell-shaped profile along the *x*-axis with its maximum at x = 0 and a corresponding value of  $c = c_0$ :

$$c(t_0) = c_0 \exp(-ax^2)$$

Assume a gaseous solution with a solute content of 3 mol/m<sup>3</sup> at the concentration boundary. The diffusion coefficient is set to  $1 \cdot 10^{-5}$  m<sup>2</sup>/s.

The second part of this exercise uses a homogenized 1D model geometry with effective transport properties and an average porosity. The model equation then becomes:

$$\varepsilon \frac{\partial c}{\partial t} + \nabla \cdot (-D^{\text{eff}} \nabla c) = 0$$

where  $\varepsilon$  denotes the average porosity and  $D^{\text{eff}}$  is the effective diffusivity. These properties are calculated from the results of the detailed structure; see the next section. At the boundaries, the concentration and flux conditions described above apply.

## Results and Discussion

The simulations are run for t = 0 to 0.1 s, when the simulation reaches steady state. Figure 2 below shows the concentration profile after 0.05 s in the porous structure. Already at this stage, the concentration has almost reached steady state, which is visible by the nearly linear concentration profile across the structure.



Figure 2: Concentration profile in the modeled artificial porous structure at t = 0.05 s.

When modeling porous media, the exact concentration in the pore structure is not the most important issue because the description of the structure is homogenized and not detailed as in Figure 2. The most interesting issue is then the description of the flux. To calculate the average flux, integrate over the flux boundary and divide by its length,  $L_0$ , which yields the following expression:

$$N_{\text{average}} = \frac{1}{L_0} \int_0^{L_0} k_m (c - c_1) dS$$

Figure 3 shows the value of this integral as a function of time. If you let the process reach steady-state, the average flux becomes  $8.051 \cdot 10^{-3} \text{ mol}/(\text{m}^2/\text{s})$ . Considering the almost linear profile across the structure, it is natural to replace the porous structure with a 1D

homogenized structure along the *x*-axis. It is then possible to calculate the effective diffusivity according to the following:

$$D^{\text{eff}(c_0 - c_{\text{out}})}_{L_1} = N_{\text{average}}$$

where  $c_{out}$  is the average concentration (mol/m<sup>3</sup>) at the flux boundary, and  $L_1$  is the length of the geometry along the *x*-axis. The average concentration is obtained by integrating according to the expression below:

$$c_{\text{out}} = \frac{1}{L_0} \int_0^{L_0} c \, dy$$

This gives an average concentration  $c_{out} = 1.63 \cdot 10^{-3} \text{ mol/m}^3$ . Using  $L_1 = 8 \cdot 10^{-4} \text{ m}$ , the effective diffusivity is:

$$D^{\text{eff}} = \frac{8.051 \cdot 10^{-3} \times 8.0 \cdot 10^{-4}}{(3 - 1.63 \cdot 10^{-3})}$$

which yields a value for the effective diffusivity of  $2.15 \cdot 10^{-6} \text{ m}^2/\text{s}$  compared to the "free" diffusivity of  $1 \cdot 10^{-5} \text{ m}^2/\text{s}$ . The effective and "free" diffusivities are usually related according to the equation

$$D^{\mathrm{eff}} = D\frac{\varepsilon}{\tau}$$

where  $\varepsilon$  is the porosity of the structure and  $\tau$  is the tortuosity, which is a measure of the actual length per unit effective length a molecule has to diffuse in a porous structure. To calculate the porosity of the modeled structure, you integrate the value 1 over the structure and then divide this by the length and width of the structure:

$$\varepsilon = \frac{1}{L_0 L_1} \int_{0}^{L_1 L_0} \int_{0}^{1} 1 dx dy$$

resulting in a value of 0.383. The value of  $\tau$  can then be calculated to 1.62. In addition, the tortuosity is usually expressed as a power of the porosity, resulting in an expression for the effective diffusivity according to

$$D^{\rm eff} = D\epsilon^p$$

#### 5 | EFFECTIVE DIFFUSIVITY IN POROUS MATERIALS

If you use the calculated values for porosity and effective diffusivity, the value for p is 1.60. The experimental values for p for porous structures used for transport in catalysts, soils, and other porous structures is usually in the range 1.5–2.

Using the value of the effective diffusivity, a simple homogenized 1D model provides the possibility to compare the value of the flux using a homogenized model to the value using the detailed 2D structure. Figure 3 shows that there is an excellent agreement between the model using a detailed geometry and the homogenized model. The difference in the time-dependent flux is hardly visible between the two cases in the graph.



Figure 3: Average flux at the flux boundary in the detailed 2D model (solid blue line) and the 1D homogenized approximation (dashed green line).

Notes About the COMSOL Implementation

Both models described above are straightforward to define in COMSOL Multiphysics. One feature that is of great use in this example is the ability to define integration coupling operators to generate the values of the integrals needed to evaluate the results. The definition of these integrals is described in detail in the step-by-step instructions below.

## Application Library path: COMSOL\_Multiphysics/Diffusion/ effective\_diffusivity

## Modeling Instructions

From the File menu, choose New.

#### NEW

In the New window, click 🔗 Model Wizard.

#### MODEL WIZARD

- I In the Model Wizard window, click **2**D.
- 2 In the Select Physics tree, select Chemical Species Transport> Transport of Diluted Species (tds).
- 3 Click Add.
- 4 Click 🔿 Study.
- 5 In the Select Study tree, select General Studies>Time Dependent.
- 6 Click 🗹 Done.

Insert the geometry sequence to focus on the simulation. If you want to know how to build the geometry, you find instructions in the appendix.

#### GEOMETRY I

- I In the Geometry toolbar, click Insert Sequence and choose Insert Sequence.
- 2 Browse to the model's Application Libraries folder and double-click the file effective\_diffusivity\_geom\_sequence.mph.
- 3 In the Geometry toolbar, click 📗 Build All.

#### GLOBAL DEFINITIONS

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.

Name	Expression	Value	Description
D2	1e-5[m^2/s]	IE-5 m²/s	Diffusion coefficient
c_max	3[mol/m^3]	3 mol/m <sup>3</sup>	Peak initial concentration
k_f	5[m/s]	5 m/s	Mass transfer coefficient
а	1000	1000	Dimensionless constant

**3** In the table, enter the following settings:

Variables I

I In the Home toolbar, click a= Variables and choose Global Variables.

2 In the Settings window for Variables, locate the Variables section.

**3** In the table, enter the following settings:

Name	Expression	Unit	Description
c0	c_max*exp(a*(-(x/ 0.4[mm])^2))	mol/m³	Initial concentration

The geometry sequence contains several selections. They are useful when defining the boundary conditions and a nonlocal integration coupling, and also during postprocessing.

#### TRANSPORT OF DILUTED SPECIES (TDS)

- I In the Model Builder window, under Component I (compl) click Transport of Diluted Species (tds).
- **2** In the **Settings** window for **Transport of Diluted Species**, locate the **Transport Mechanisms** section.
- **3** Clear the **Convection** check box.

This setting gives a pure diffusion interface.

#### Transport Properties 1

- I In the Model Builder window, under Component I (compl)>
- Transport of Diluted Species (tds)  ${
  m click}$  Transport Properties I.
- 2 In the Settings window for Transport Properties, locate the Diffusion section.
- **3** In the  $D_c$  text field, type D2.

#### Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.

**3** In the c text field, type c0.

#### Concentration 1

- I In the Physics toolbar, click Boundaries and choose Concentration.
- 2 In the Settings window for Concentration, locate the Boundary Selection section.
- 3 From the Selection list, choose Left Boundary.
- 4 Locate the **Concentration** section. Select the **Species c** check box.
- **5** In the  $c_{0,c}$  text field, type c\_max.

#### Flux I

- I In the Physics toolbar, click Boundaries and choose Flux.
- 2 In the Settings window for Flux, locate the Boundary Selection section.
- 3 From the Selection list, choose Right Boundary.
- 4 Locate the Inward Flux section. From the Flux type list, choose External convection.
- 5 Select the Species c check box.
- **6** In the  $k_{c,c}$  text field, type k\_f.

### DEFINITIONS

Proceed to define a variable for the average flux through the porous structure. Begin by defining a nonlocal average coupling on the rightmost boundary.

Average 1 (aveop1)

- I In the Definitions toolbar, click *P* Nonlocal Couplings and choose Average.
- 2 In the Settings window for Average, locate the Source Selection section.
- **3** From the **Geometric entity level** list, choose **Boundary**.
- 4 From the Selection list, choose Right Boundary.

#### Variables 2

- I In the **Definitions** toolbar, click  $\partial =$  **Local Variables**.
- 2 In the Settings window for Variables, locate the Variables section.
- **3** In the table, enter the following settings:

Name	Expression	Unit	Description
flux_avg	aveop1(k_f*c)	mol/(m²·s)	Average flux

#### MESH I

In the Model Builder window, under Component I (comp1) right-click Mesh I and choose Build All.

#### STUDY I

Step 1: Time Dependent

- I In the Model Builder window, under Study I click Step I: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.
- 3 From the Time unit list, choose ms.
- 4 In the **Output times** text field, type range(0,2,100).
- **5** In the **Home** toolbar, click **= Compute**.

### RESULTS

#### Concentration (tds)

The first default plot shows concentration and flux streamlines.

#### Streamline 1

- I In the Model Builder window, expand the Concentration (tds) node, then click Streamline I.
- 2 In the Settings window for Streamline, locate the Streamline Positioning section.
- **3** From the **Positioning** list, choose **On selected boundaries**.
- **4** Locate the **Selection** section. Click to select the **Delivered Selection** toggle button.
- **5** Select Boundary 1 only.
- 6 Locate the Streamline Positioning section. In the Number text field, type 40.
- 7 In the Concentration (tds) toolbar, click **I** Plot.

#### Concentration (tds)

#### I Click the **Zoom Extents** button in the **Graphics** toolbar.

The plot shows the concentration at the end time, that is, 0.1 seconds.



You can also plot the concentration at different time steps.

- 2 In the Model Builder window, click Concentration (tds).
- 3 In the Settings window for 2D Plot Group, locate the Data section.
- 4 From the Time (ms) list, choose 50.
- 5 In the Concentration (tds) toolbar, click **9** Plot.

Compare this plot to the one shown in Figure 2.

#### ID Plot Group 2

Now, plot the average flux.

In the Home toolbar, click 🚛 Add Plot Group and choose ID Plot Group.

Point Graph 1

- I Right-click ID Plot Group 2 and choose Point Graph.
- 2 In the Settings window for Point Graph, locate the Selection section.
- 3 From the Selection list, choose Top-Right Vertex.

4 Click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Definitions>Variables>flux\_avg - Average flux - mol/ (m<sup>2</sup>·s).

Molar fluxes

- I In the Model Builder window, click ID Plot Group 2.
- 2 In the Settings window for ID Plot Group, click to expand the Title section.
- 3 In the Label text field, type Molar fluxes.
- 4 Locate the Title section. From the Title type list, choose None.
- 5 Locate the Plot Settings section.
- 6 Select the y-axis label check box. In the associated text field, type Average flux (mol/(m\*s)).



7 In the Molar fluxes toolbar, click **I** Plot.

To get the porosity of the domain for the 1D model, perform a surface integration.

Surface Integration 1

- I In the Results toolbar, click <sup>8,85</sup><sub>e-12</sub> More Derived Values and choose Integration> Surface Integration.
- 2 In the Settings window for Surface Integration, locate the Selection section.
- 3 From the Selection list, choose All domains.

4 Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit
1/(0.8[mm])^2	1

The denominator in this expression represents the product of the length and the width of the 2D model structure.

5 Click **=** Evaluate.

#### TABLE

I Go to the Table window.

The evaluated value of the integral should be close to 0.383.

#### ROOT

Now turn to the 1D model.

#### ADD COMPONENT

In the Model Builder window, right-click the root node and choose Add Component>ID.

#### ADD PHYSICS

- I In the Home toolbar, click 🙀 Add Physics to open the Add Physics window.
- 2 Go to the Add Physics window.
- 3 In the tree, select Chemical Species Transport>Transport of Diluted Species (tds).
- 4 Find the Physics interfaces in study subsection. In the table, clear the Solve check box for Study 1.
- 5 Click Add to Component 2 in the window toolbar.
- 6 In the Home toolbar, click 🙀 Add Physics to close the Add Physics window.

#### ADD STUDY

- I In the Home toolbar, click  $\stackrel{\sim}{\sim}$  Add Study to open the Add Study window.
- 2 Go to the Add Study window.
- **3** Find the **Physics interfaces in study** subsection. In the table, clear the **Solve** check box for **Transport of Diluted Species (tds)**.
- 4 Find the Studies subsection. In the Select Study tree, select General Studies> Time Dependent.
- 5 Click Add Study in the window toolbar.
- 6 In the Model Builder window, click the root node.

7 In the Home toolbar, click  $\sim 2$  Add Study to close the Add Study window.

#### **GEOMETRY 2**

Interval I (i1)

- I In the Model Builder window, under Component 2 (comp2) right-click Geometry 2 and choose Interval.
- 2 In the Settings window for Interval, locate the Interval section.
- **3** In the table, enter the following settings:

Coordinates (m)

0

8e-4

4 Click 틤 Build Selected.

**5** Click the **Graphics** toolbar.

#### GLOBAL DEFINITIONS

Parameters 1

Add the following parameters to those you already defined.

#### I In the Model Builder window, under Global Definitions click Parameters I.

- 2 In the Settings window for Parameters, locate the Parameters section.
- **3** In the table, enter the following settings:

Name	Expression	Value	Description
epsilon	0.383	0.383	Porosity
D1	2.15e-6[m^2/s]	2.15E-6 m <sup>2</sup> /s	Diffusion coefficient, 1D

#### TRANSPORT OF DILUTED SPECIES 2 (TDS2)

- I In the Model Builder window, under Component 2 (comp2) click Transport of Diluted Species 2 (tds2).
- **2** In the **Settings** window for **Transport of Diluted Species**, locate the **Transport Mechanisms** section.
- **3** Clear the **Convection** check box.

#### Transport Properties 1

- I In the Model Builder window, under Component 2 (comp2)> Transport of Diluted Species 2 (tds2) click Transport Properties I.
- 2 In the Settings window for Transport Properties, locate the Diffusion section.
- **3** In the  $D_{c2}$  text field, type D1/epsilon.

#### Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the c2 text field, type c0.

#### Concentration 1

- I In the Physics toolbar, click Boundaries and choose Concentration.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Concentration, locate the Concentration section.
- 4 Select the **Species c2** check box.
- **5** In the  $c_{0,c2}$  text field, type c\_max.

#### Flux I

- I In the Physics toolbar, click Boundaries and choose Flux.
- **2** Select Boundary 2 only.
- 3 In the Settings window for Flux, locate the Inward Flux section.
- 4 From the Flux type list, choose External convection.
- 5 Select the **Species c2** check box.
- **6** In the  $k_{c,c2}$  text field, type k\_f/epsilon.

#### DEFINITIONS (COMP2)

Create a variable for the flux in the homogenized 1D model.

Variables 3

- I In the Home toolbar, click  $\partial =$  Variables and choose Local Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- **3** In the table, enter the following settings:

Name	Expression	Unit	Description
flux_hom	k_f*c2	mol/(m²·s)	Flux, 1D model

#### MESH 2

- I In the Model Builder window, under Component 2 (comp2) click Mesh 2.
- 2 In the Settings window for Mesh, locate the Physics-Controlled Mesh section.
- 3 From the Element size list, choose Extra fine.
- 4 Click 📗 Build All.

#### STUDY 2

- Step 1: Time Dependent
- I In the Model Builder window, under Study 2 click Step 1: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.
- 3 From the Time unit list, choose ms.
- 4 In the **Output times** text field, type range(0,2,100).
- **5** In the **Home** toolbar, click **= Compute**.

#### RESULTS

#### Concentration (tds2)

The default plot for the 1D model shows the concentration for all time steps.



Finally, plot the result for the flux at the flux boundary in the homogenized 1D model in the same plot as the 2D result for comparison.

#### Point Graph 2

- I In the Model Builder window, right-click Molar fluxes and choose Point Graph.
- 2 In the Settings window for Point Graph, locate the Data section.
- 3 From the Dataset list, choose Study 2/Solution 2 (3) (sol2).
- **4** Select Boundary 2 only.
- 5 Click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)>Definitions>Variables>flux\_hom Flux, ID model mol/(m<sup>2</sup>·s).
- 6 Click to expand the Coloring and Style section. Find the Line style subsection. From the Line list, choose Dashed.
- 7 In the Molar fluxes toolbar, click **O** Plot.

Compare the result with that shown in Figure 3.

## Appendix — Geometry Modeling Instructions

This section describes the individual steps for building the geometry sequence.

These steps replace the Insert Sequence step in the previous instruction.

#### GEOMETRY I

In the **Geometry** toolbar, click *A* Sketch.

Square 1 (sq1)

- I In the **Geometry** toolbar, click Square.
- 2 In the Settings window for Square, locate the Size section.
- **3** In the **Side length** text field, type **0.08**[mm].
- 4 Locate the Position section. In the x text field, type 0.01[mm].
- **5** In the **y** text field, type 0.01[mm].
- **6** Locate the **Selections of Resulting Entities** section. Select the **Resulting objects selection** check box.
- 7 From the Show in physics list, choose Off.

With the last step, the square can be used as an input object for various geometry operations.

Fillet I (fill)

- I In the **Geometry** toolbar, click **Fillet**.
- 2 In the Settings window for Fillet, locate the Points section.

- 3 From the Vertices to fillet list, choose Square 1. This rounds all four corners.
- 4 Locate the Radius section. In the Radius text field, type 0.016[mm].



5 Click 틤 Build Selected.

## Array I (arr1)



- 2 Select the object fill only.
- 3 In the Settings window for Array, locate the Size section.
- 4 In the **x size** text field, type 8.
- **5** In the **y size** text field, type **9**.
- 6 Locate the **Displacement** section. In the **x** text field, type 0.1[mm].
- 7 In the y text field, type 0.1[mm].



There is an offset between the individual rows.

Move I (movI)

- I In the Geometry toolbar, click 💭 Transforms and choose Move.
- 2 In the Settings window for Move, locate the Displacement section.
- 3 In the y text field, type -0.05[mm].
- **4** Select every second row of the array.



The array of squares forms the holes in the geometry. Create the outer domain.

#### Rectangle 1 (r1)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 0.8[mm].
- 4 In the **Height** text field, type 0.8[mm].

#### Difference I (dif1)

- I In the Geometry toolbar, click i Booleans and Partitions and choose Difference.
- 2 Select the object rI only.
- 3 In the Settings window for Difference, locate the Difference section.
- **4** Find the **Objects to subtract** subsection. Click to select the **Selection** toggle button.
- 5 From the **Objects to subtract** list, choose **Square I** since the first square creates a **Selection of Resulting Entities**, all squares are included in this selection.



Form Union (fin)

I In the Model Builder window, click Form Union (fin).

2 In the Settings window for Form Union/Assembly, click 틤 Build Selected.

To facilitate physics settings and postprocessing, define **Selection** features at Point and Boundary levels.

Top-Right Vertex

- I In the Geometry toolbar, click 🝖 Selections and choose Explicit Selection.
- 2 In the Settings window for Explicit Selection, locate the Entities to Select section.
- 3 From the Geometric entity level list, choose Point.
- 4 In the Label text field, type Top-Right Vertex.



**5** On the object **fin**, select Point 532 only.

Left Boundary

- I In the Geometry toolbar, click 🕞 Selections and choose Explicit Selection.
- 2 In the Settings window for Explicit Selection, locate the Entities to Select section.
- **3** From the **Geometric entity level** list, choose **Boundary**.
- 4 In the Label text field, type Left Boundary.



5 On the object fin, select Boundary 1 only.

Right Boundary

- I In the Geometry toolbar, click 🐚 Selections and choose Explicit Selection.
- 2 In the Settings window for Explicit Selection, locate the Entities to Select section.
- **3** From the **Geometric entity level** list, choose **Boundary**.
- 4 On the object fin, select Boundary 276 only.



5 In the Label text field, type Right Boundary.