

Syngas Combustion in a Round-Jet Burner

This model simulates turbulent combustion of syngas (synthesis gas) in a simple round jet burner. Syngas is a gas mixture, primarily composed of hydrogen, carbon monoxide and carbon dioxide. The name syngas relates to its use in creating synthetic natural gas.

The model setup corresponds to the one studied by Couci and others in Ref. 1. The temperature and composition resulting from the nonpremixed combustion in the burner setup have also been experimentally investigated by Barlow and coworkers (Ref. 2 and Ref. 3) as a part of the International Workshop on Measurement and Computation of Turbulent Nonpremixed Flames (Ref. 4). The model is solved in COMSOL Multiphysics by combining a Reacting Flow and a Heat Transfer in Fluids interface.

Model Definition

The burner studied in this model consists of a straight pipe placed in a slight coflow. The gas phase fuel is fed through the pipe using an inlet velocity of 76 m/s, while the coflow velocity outside of pipe is 0.7 m/s. At the pipe exit, the fuel gas mixes with the coflow, creating an unconfined circular jet. The gas fed through the tube consists of three compounds typical of syngas: carbon monoxide (CO), hydrogen (H_2) , and nitrogen (N_2) . The coflow gas consists of air. At the pipe exit, the fuel is ignited. Since the fuel and oxidizer enter the reaction zone separately, the resulting combustion is of the nonpremixed type. A continuous reaction requires that the reactants and the oxidizer are mixed to stoichiometric conditions. In this setup, the turbulent flow of the jet effectively mixes the fuel from the pipe with the coflowing oxygen. Furthermore, the mixture needs to be continuously ignited. In this burner the small recirculation zones generated by the pipe wall thickness provide the means to decelerate hot product gas. The recirculation zones hereby promote continuous ignition of the oncoming mixture and stabilizes the flame at the pipe orifice. In experiments (Ref. 4), no lift-off or localized extinction of the flame has been observed.

In the current model, the syngas combustion is modeled using two irreversible reactions:

$$CO + 0.5O_2 \rightarrow CO_2$$

$$H_2 + 0.5O_2 \rightarrow H_2O$$
 (1)

This assumption of a complete oxidation of the fuel corresponds to one of the approaches used in Ref. 1. The mass transport in the reacting jet is modeled by solving for the mass fractions of six species: the five species participating in the reactions and nitrogen N₂ originating in the coflowing air.

The Reynolds number for the jet, based on the inlet velocity and the inner diameter of the pipe, is approximately 16,700, indicating that the jet is fully turbulent. Under these circumstances, both the mixing and the reactions processes in the jet are significantly influenced by the turbulent nature of the flow. To account for the turbulence when solving for the flow field, the k- ω turbulence model is applied.

Taking advantage of the symmetry, a two-dimensional model using a cylindrical coordinate system is solved.

TURBULENT REACTION RATE

When using a turbulence model in a Reacting Flow interface, the production rate (SI unit: $kg/(m^3 \cdot s)$) of species i resulting from reaction j is modeled as the minimum of the mean-value-closure reaction rate and the eddy-dissipation-model rate:

$$R_{ij} = v_{ij} M_i \cdot \min \left[r_{\text{MVC},j}, r_{\text{ED},j} \right]$$

The mean-value-closure rate is the kinetic reaction rate expressed using the mean mass fractions. This corresponds to the characteristic reaction rate for reactions that are slow compared to the turbulent mixing, or the reaction rate in regions with negligible turbulence levels. This can be quantified through the Damköhler number, which compares the turbulent time scale (τ_T) to the chemical time scale (τ_c) . The mean-value-closure is appropriate for low Damköhler numbers:

$$Da = \frac{\tau_T}{\tau_c} \ll 1$$

The reaction rate defined by the eddy-dissipation model (Ref. 5) is

$$r_{\mathrm{ED},j} = \frac{\alpha_{j}}{\tau_{\mathrm{T}}} \rho \cdot \min \left[\min \left(\frac{\omega_{r}}{v_{rj} M_{r}} \right), \beta \sum_{\mathbf{p}} \left(\frac{\omega_{\mathbf{p}}}{v_{\mathbf{p}j} M_{\mathbf{p}}} \right) \right]$$
 (2)

where τ_T (SI unit: s) is the mixing time scale of the turbulence, ρ is the mixture density (SI unit: kg/m³), ω is the species mass fraction, ν denotes the stoichiometric coefficients, and M is the molar mass (SI unit: kg/mol). Properties of reactants of the reaction are indicated using a subscript "r," while product properties are denoted by a subscript "p".

The eddy-dissipation model assumes that both the Reynolds and Damköhler numbers are sufficiently high for the reaction rate to be limited by the turbulent mixing time scale τ_T . A global reaction can then at most progress at the rate at which fresh reactants are mixed, at the molecular level, by the turbulence present. The reaction rate is also assumed to be

limited by the deficient reactant; the reactant with the lowest local concentration. The model parameter β specifies that product species is required for reaction, modeling the activation energy. For gaseous nonpremixed combustion the model parameters have been found to be (Ref. 5):

$$\alpha = 4$$
, $\beta = 0.5$

In the current model the molecular reaction rate of the reactions is assumed to be infinitely fast. This is achieved in the model by prescribing unrealistically high rate constants for the reactions. This implies that the production rate is given solely by the turbulent mixing in Equation 2.

It should be noted that the eddy-dissipation model is a robust but simple model for turbulent reactions. The reaction rate is governed by a single time scale, the turbulent mixing time-scale. For this reason, the reactions studied should be limited to global onestep (as in Equation 1) or two-step reactions.

THERMAL PROPERTIES — HEAT OF REACTION AND HEAT CAPACITY

In this model, a thermodynamic system including all present species is set up. The system is used to define species as well as mixture properties dependent on temperature and composition. When coupling the Chemistry interface to the Thermodynamic system, all thermodynamic and transport properties needed are automatically defined.

Two of the thermal properties needed are the heat of reaction and the heat capacity of the mixture. Figure 1 shows the variation of enthalpy of formation with temperature for all individual species. The enthalpy of formation is seen to increase with temperature for all species, and accurate results will be obtained by taking the temperature-dependence into consideration.

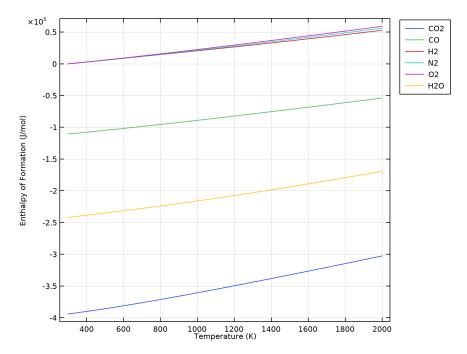


Figure 1: Enthalpy of formation for all individual species.

The heat capacities for all species in the system plotted against temperature are seen in Figure 2. As for the enthalpy of formation, all species' heat capacities increase with temperature, making it relevant to also take the temperature-dependence on heat capacity into consideration.

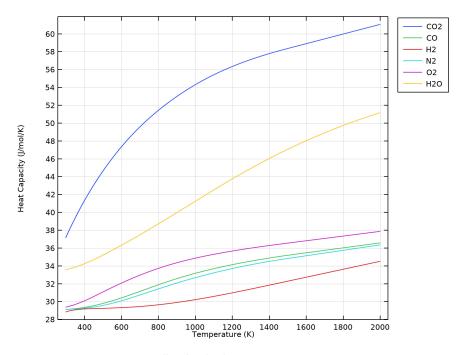


Figure 2: Heat capacity for all individual species.

The heat of formations for each species at T = 298 K are given in Table 1 and the heat capacities at T = 300 K and T = 2000 K are given in Table 2. Both tables compare data based on Ref. 6 and Ref. 7 to calculated values from COMSOL. By using these values in Equation 3, the heat of formation at T = 298 K can be calculated. Since the heat of formation of the products is lower than that of the reactants, both reactions are exothermic and release heat:

$$\Delta H_{\rm r} = \sum_{\rm products} \Delta H_{\rm f,298~K} - \sum_{\rm reactants} \Delta H_{\rm f,298~K}$$
 (3)

TABLE I: SPECIES ENTHALPY OF FORMATION AT 298.15 K FROM BOTH REFERENCE DATA AND COMSOL.

SPECIES	$\Delta H_{ m f}$ (kJ/mol)	$\Delta H_{ m f}$ (kJ/mol)
	T = 298.15 K (Ref. 6)	T = 298.15 K (COMSOL)
N_2	0	0
H_2	0	0
O_2	0	0
${\rm H_2O}$	-241.84	-241.82
CO	-110.54	-110.53
CO_2	-393.55	-393.98

TABLE 2: SPECIES HEAT CAPACITY AT 300 K AND 2000 K FROM BOTH REFERENCE DATA AND COMSOL.

SPECIES	$C_{\rm p}$ (J/mol/K) T = 300 K (Ref. 6, Ref. 7 for CO and CO2)	$C_{\rm p}$ (J/mol/K) T = 300 K (COMSOL)	C _p (J/mol/K) T = 2000 K (Ref. 6)	$\begin{aligned} &C_{\mathrm{p}} \text{ (J/mol/K)} \\ &T = 2000 \text{ K} \\ &(COMSOL) \end{aligned}$
N_2	29.075	29.142	35.987	36.368
H_2	28.878	28.857	34.238	34.528
O_2	29.330	29.395	37.790	37.882
${\rm H_2O}$	33.468	33.602	51.145	51.193
СО	29.035	29.136	33.254	36.591
CO_2	37.101	37.225	54.363	61.078

Results and Discussion

The resulting velocity field in the nonisothermal reacting jet is visualized in Figure 3. The expansion and development of the hot free jet is clearly seen. The turbulent mixing in the outer parts of the jet acts to accelerate fluid originating in the co-flow, and incorporate it in the jet. This is commonly referred to as entrainment and can be observed in the co-flow streamlines which bend toward the jet downstream of the orifice.

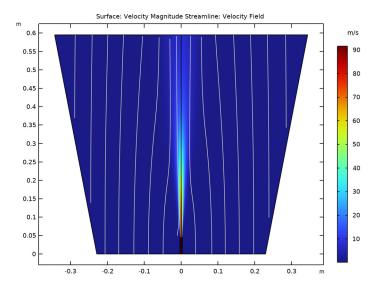


Figure 3: The velocity magnitude and flow paths (streamlines) of the reacting jet.

The temperature in the jet is shown in Figure 4 where a revolved dataset has been used to emphasize the structure of the round jet. The maximum temperature in the jet is seen to be approximately 2150 K. The carbon dioxide mass fraction in the reacting jet is plotted in Figure 5. The formation of CO₂ takes place in the outer shear layer of the jet. This is where the fuel from the pipe encounters oxygen in the coflow and reacts. The reactions are promoted by the turbulent mixing in the jet shear layer. It is also seen that the CO₂ formation starts just outside of the pipe. This is also the case for the temperature increase in Figure 4. This implies that there is no lift-off and the flame is attached to the pipe.

In Figure 6, Figure 7, and Figure 8 the results reached in the model are compared with the experimental results of Barlow and coworkers (Ref. 2, Ref. 3, and Ref. 4). In Figure 6 the jet temperature is further examined and compared with the experiments. In the left panel the temperature along the centerline is plotted. It is seen that the maximum temperature predicted in the model is close to that in the experiment. However in the model the temperature profile is shifted in the downstream direction. This is most likely due to the fact that radiation has not been included in the model.

In the right panel of Figure 6 temperature profiles at 20 and 50 pipe diameters downstream of the pipe exit are compared with the experiments. The axial velocity of the jet is compared with the experimental results in Figure 7, using the same down stream positions. The axial velocity is found to compare well with the experimental values at both positions.

In Figure 8 the species concentration along the jet centerline is analyzed and compared with the experimental results. For some species, N2, and CO2, the axial mass fraction development agrees well with the experimental results. For the fuel species CO and H₂ a fair agreement is observed. For the remaining species, O2 and H2O, the trend appears correct but the profiles are shifted downstream, as was the case with the temperature. The reason for the discrepancy in the mass fractions can in part be attributed to the fact that radiation is not included, but the accuracy is probably also significantly influenced by the simplified reaction scheme and the eddy-dissipation model.

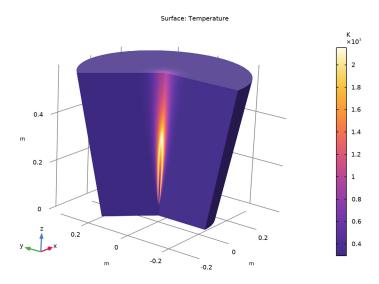


Figure 4: Jet temperature shown using a revolved dataset.

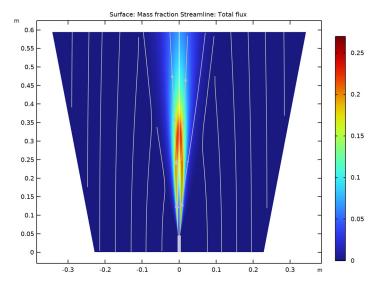


Figure 5: CO₂ mass fraction in the reacting jet.

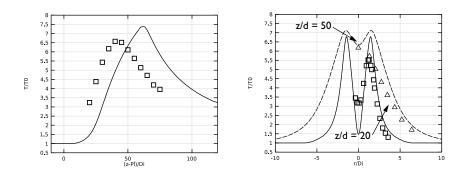


Figure 6: Jet temperature along the centerline (left), and radially at two different positions downstream of the pipe exit (right) scaled by the inlet temperature. The centerline and radial distance is scaled by the inner diameter of the pipe. Model results are plotted using lines, while experimental results are indicated using symbols. The downstream positions are defined in terms of the inner diameter of the pipe (d).

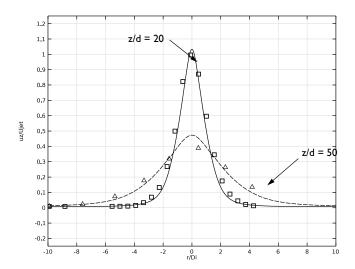


Figure 7: Axial velocity at two different positions downstream of the pipe exit, scaled by the inlet velocity. The radial distance is scaled by the inner diameter of the pipe. Model results are plotted using lines, while experimental results are indicated using symbols.

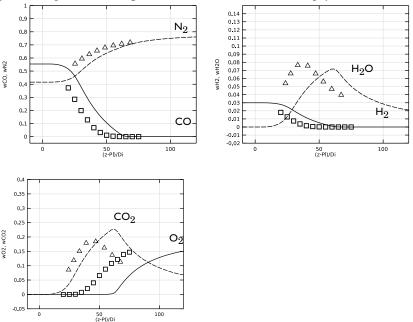


Figure 8: Species mass fractions along the jet centerline. The centerline distance is scaled by the

inner diameter of the pipe. Model results are plotted using lines, while experimental results are indicated using symbols.

References

- 1. A. Cuoci, A. Frassoldati, G. Buzzi Ferraris, T. Faravelli, and E. Ranzi, "The ignition, combustion and flame structure of carbon monoxide/hydrogen mixtures. Note 2: Fluid dynamics and kinetic aspects of syngas combustion," Int. J. Hydrogen Energy, vol. 32, pp. 3486-3500, 2007.
- 2. R.S. Barlow, G.J. Fiechtner, C.D. Carter, and J.-Y. Chen, "Experiments on the Scalar Structure of Turbulent CO/H2/N2 Jet Flames," Comb. and Flame, vol. 120, pp. 549-569, 2000.
- 3. M. Flury, Experimentelle Analyse der Mischungsstruktur in turbulenten nicht vorgemischten Flammen, Ph.D. Thesis, ETH Zurich, 1998.
- 4. R.S. Barlow and others, "Sandia/ETH-Zurich CO/H2/N2 Flame Data Release 1.1, "http://www.sandia.gov/TNF/DataArch/SANDchnWeb/SANDchnDocl1.pdf, 2002.
- 5. B.F. Magnussen and B.H. Hjertager, "On Mathematical Modeling of Turbulent Combustion with Special Emphasis on Soot Formation and Combustion," 16th Symp. (Int.) on Combustion. Comb. Inst., Pittsburgh, Pennsylvania, pp. 719–729, 1976.
- 6. A. Frassoldati, T. Faravelli, and E. Ranzi, "The Ignition, Combustion and Flame Structure of Carbon Monoxide/Hydrogen Mixtures. Note 1: Detailed Kinetic Modeling of Syngas Combustion Also in Presence of Nitrogen Compounds," Int. J. Hydrog. Energy, vol. 32, pp. 3471-3485, 2007.
- 7. B.E. Poling, J.M. Prausnitz, and J.P. O'Connell, The Properties of Gases and Liquids, McGraw-Hill, 2001.

Application Library path: Chemical Reaction Engineering Module/ Reactors with Mass and Heat Transfer/round jet burner

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click 2D Axisymmetric.
- 2 In the Select Physics tree, select Chemical Species Transport>
 Nonisothermal Reacting Flow>Turbulent Flow>Turbulent Flow, k-ω.
- 3 Click Add.
- 4 In the Added physics interfaces tree, select Transport of Concentrated Species (tcs).
- 5 In the Number of species text field, type 6.
- 6 In the Mass fractions table, enter the following settings:

wC0 w02 wC02 wH2 wH20 wN2

- 7 Click 🕣 Study.
- 8 In the Select Study tree, select General Studies>Stationary.
- 9 Click M Done.

GLOBAL DEFINITIONS

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- 3 Click **Load from File**.
- **4** Browse to the model's Application Libraries folder and double-click the file round_jet_burner_parameters.txt.

GEOMETRY I

Rectangle I (rI)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.

- 3 In the Width text field, type GeomW.
- 4 In the Height text field, type GeomH.
- 5 Click **Build Selected**.

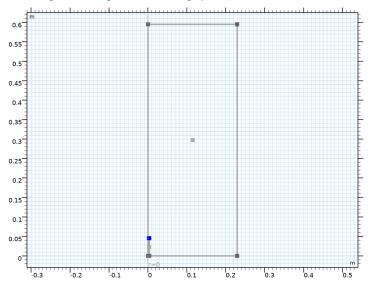
Rectangle 2 (r2)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type Pth.
- 4 In the Height text field, type P1.
- 5 Locate the **Position** section. In the **r** text field, type Di/2.
- 6 Click | Build Selected.

Chamfer I (chal)

- I In the **Geometry** toolbar, click Chamfer.
- 2 On the object r2, select Points 3 and 4 only.

It might be easier to select the points by using the **Selection List** window. To open this window, in the Home toolbar click Windows and choose Selection List. (If you are running the cross-platform desktop, you find **Windows** in the main menu.)



- 3 In the Settings window for Chamfer, locate the Distance section.
- 4 In the Distance from vertex text field, type Pth*0.15.

- 5 Click Pauld Selected.
- **6** Click the **Zoom Extents** button in the **Graphics** toolbar.

Polygon I (poll)

- I In the Geometry toolbar, click / Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- 3 From the Data source list, choose Vectors.
- 4 In the r text field, type GeomW GeomW*1.5 GeomW*1.5 GeomW.
- 5 In the z text field, type 0 GeomH GeomH.
- 6 Click Pauld Selected.

Union I (uni I)

- I In the Geometry toolbar, click Booleans and Partitions and choose Union.
- 2 Select the objects poll and rl only.
- 3 In the Settings window for Union, locate the Union section.
- 4 Clear the Keep interior boundaries check box.
- 5 Click | Build Selected.

Difference I (dif1)

- I In the Geometry toolbar, click Booleans and Partitions and choose Difference.
- 2 Select the object unil only.
- 3 In the Settings window for Difference, locate the Difference section.
- **4** Find the **Objects to subtract** subsection. Click to select the **Activate Selection** toggle button.
- **5** Select the object **chal** only.
- 6 Click **Build Selected**.

Line Segment I (Is I)

- I In the Geometry toolbar, click * More Primitives and choose Line Segment.
- 2 In the Settings window for Line Segment, locate the Starting Point section.
- **3** From the **Specify** list, choose **Coordinates**.
- 4 In the z text field, type P1-0.15*Pth.
- 5 Locate the **Endpoint** section. From the **Specify** list, choose **Coordinates**.
- 6 In the r text field, type Di/2.
- 7 In the z text field, type P1-0.15*Pth.

8 Click Pauld Selected.

Line Segment 2 (Is2)

- I In the Geometry toolbar, click * More Primitives and choose Line Segment.
- 2 In the Settings window for Line Segment, locate the Starting Point section.
- 3 From the Specify list, choose Coordinates.
- 4 In the r text field, type Di/2+Pth.
- 5 In the z text field, type P1-0.15*Pth.
- 6 Locate the Endpoint section. From the Specify list, choose Coordinates.
- 7 In the r text field, type GeomW+0.5*(Pl-0.15*Pth)*GeomW/GeomH.
- 8 In the z text field, type P1-0.15*Pth.
- 9 Click **P** Build Selected.

Line Segment 3 (Is3)

- I In the Geometry toolbar, click * More Primitives and choose Line Segment.
- 2 In the Settings window for Line Segment, locate the Starting Point section.
- 3 From the Specify list, choose Coordinates.
- 4 In the r text field, type Di/2.
- 5 In the z text field, type P1-0.15*Pth.
- 6 Locate the Endpoint section. From the Specify list, choose Coordinates.
- 7 In the r text field, type Di/2+(GeomH-Pl+Pth*0.15)*tan(pi/180).
- 8 In the z text field, type GeomH.
- 9 Click | Build Selected.

Line Segment 4 (Is4)

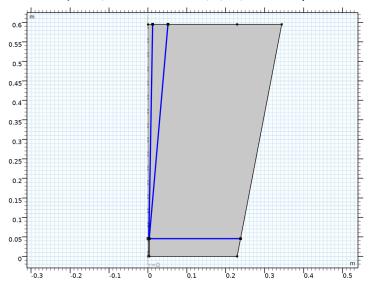
- I In the Geometry toolbar, click * More Primitives and choose Line Segment.
- 2 In the Settings window for Line Segment, locate the Starting Point section.
- 3 From the Specify list, choose Coordinates.
- 4 In the r text field, type Di/2+Pth.
- 5 In the z text field, type P1-0.15*Pth.
- **6** Locate the **Endpoint** section. From the **Specify** list, choose **Coordinates**.
- 7 In the r text field, type Di/2+Pth+(GeomH-Pl+Pth*0.15)*tan(5*pi/180).
- 8 In the z text field, type GeomH.
- 9 Click | Build Selected.

Form Union (fin)

- I In the Model Builder window, click Form Union (fin).
- 2 In the Settings window for Form Union/Assembly, click 📳 Build Selected.

Mesh Control Edges I (mcel)

- I In the Geometry toolbar, click \times \text{Virtual Operations} and choose Mesh Control Edges.
- **2** On the object **fin**, select Boundaries 4, 8, 13, and 14 only.



- 3 In the Settings window for Mesh Control Edges, click 📔 Build Selected.
- 4 Click the **Zoom Extents** button in the **Graphics** toolbar.

Form Composite Edges I (cmel)

- I In the Geometry toolbar, click "Virtual Operations and choose Form Composite Edges.
- 2 On the object mcel, select Boundaries 3 and 11 only.
- 3 In the Settings window for Form Composite Edges, click 📳 Build Selected.

Define a **Thermodynamic System** that can be used for several physical properties in the model. The system is in gas phase and consists of water, hydrogen, oxygen, nitrogen, carbon monoxide and carbon dioxide.

GLOBAL DEFINITIONS

In the Physics toolbar, click Thermodynamics and choose Thermodynamic System.

SELECT SYSTEM

- I Go to the Select System window.
- 2 Click Next in the window toolbar.

SELECT SPECIES

- I Go to the Select Species window.
- 2 In the Species list, select water (7732-18-5, H20).
- 3 Click + Add Selected.
- 4 In the Species list, select carbon monoxide (630-08-0, CO).
- 5 Click + Add Selected.
- 6 In the Species list, select carbon dioxide (124-38-9, CO2).
- 7 Click + Add Selected.
- 8 In the Species list, select nitrogen (7727-37-9, N2).
- 9 Click + Add Selected.
- **10** In the **Species** list, select **oxygen (7782-44-7, 02)**.
- II Click + Add Selected.
- 12 In the Species list, select hydrogen (1333-74-0, H2).
- **13** Click + Add Selected.
- 14 Click Next in the window toolbar.

SELECT THERMODYNAMIC MODEL

- I Go to the Select Thermodynamic Model window.
- 2 Click Finish in the window toolbar.

GLOBAL DEFINITIONS

Gas System I (ppI)

As stated in the Model Definition section, the heat of reaction and heat capacity of the mixture are dependent on temperature and composition. To display their dependence, plots where the enthalpy of formation and heat capacity are plotted against a temperature span between 298.15 and 2000 K are later created. The functions necessary for these plots will now be obtained.

I In the Model Builder window, under Global Definitions>Thermodynamics right-click Gas System I (ppI) and choose Species Property.

SELECT PROPERTIES

- I Go to the Select Properties window.
- 2 In the list, select Heat capacity (Cp) (J/(K*mol)).
- 3 Click + Add Selected.
- 4 In the list, select Enthalpy of formation (J/mol).
- 5 Click + Add Selected.
- 6 Click **Next** in the window toolbar.

SELECT PHASE

- I Go to the Select Phase window.
- 2 Click **Next** in the window toolbar.

SELECT SPECIES

- I Go to the **Select Species** window.
- 2 Click Add All.
- 3 Click **Next** in the window toolbar.

SPECIES PROPERTY OVERVIEW

- I Go to the Species Property Overview window.
- 2 Click Finish in the window toolbar.

CHEMISTRY (CHEM)

Reaction I

- I In the Model Builder window, under Component I (compl) right-click Chemistry (chem) and choose Reaction.
- 2 In the Settings window for Reaction, locate the Reaction Formula section.
- 3 In the Formula text field, type C0+02=>C02.
- 4 Click Apply.

Since all species in the reaction are written using their chemical formulas, their molar masses are pre-defined to come from thermodynamics. Moreover, the reaction can also be balanced using the **Balance** button.

Click Balance in the upper-right corner of the Reaction Formula section.

Reaction 2

I In the **Physics** toolbar, click **Domains** and choose **Reaction**.

- 2 In the Settings window for Reaction, locate the Reaction Formula section.
- 3 In the Formula text field, type H2+02=>H20.
- 4 Click Apply.
- 5 Click Balance in the upper-right corner of the Reaction Formula section.

Species 1

- I In the Physics toolbar, click **Domains** and choose Species.
- 2 In the Settings window for Species, locate the Name section.
- **3** In the text field, type N2.

Since a Thermodynamic system is defined earlier, the Thermodynamics check box can be selected that uses the values for density and heat capacity from the system.

- I In the Model Builder window, click Chemistry (chem).
- 2 In the Settings window for Chemistry, locate the Mixture Properties section.
- 3 Select the Thermodynamics check box.
- 4 Locate the Species Matching section. From the Species solved for list, choose **Transport of Concentrated Species.**
- **5** Find the **Bulk species** subsection. In the table, enter the following settings:

Species	Туре	Mass fraction	Value (I)	From Thermodynamics
СО	Variable	wCO	Solved for	СО
CO2	Variable	wCO2	Solved for	CO2
H2	Variable	wH2	Solved for	H2
H2O	Variable	wH2O	Solved for	H2O
N2	Free species	wN2	Solved for	N2
O2	Variable	wO2	Solved for	O2

- **6** Click to expand the **Calculate Transport Properties** section. From the Thermal conductivity list, choose User defined.
- **7** In the k text field, type k_mix .
- 8 From the Dynamic viscosity list, choose User defined.
- 9 In the \(\mu \) text field, type mu mix.

TRANSPORT OF CONCENTRATED SPECIES (TCS)

In the Model Builder window, under Component I (compl) click Transport of Concentrated Species (tcs).

Reaction I

- I In the **Physics** toolbar, click **Domains** and choose **Reaction**.

 Thanks to the balanced reactions, the stoichiometric coefficients are known.
- 2 Select Domain 1 only.
- 3 In the Settings window for Reaction, locate the Reaction Rate section.
- 4 In the v_{wCO} text field, type -2.
- **5** In the v_{wO2} text field, type -1.
- **6** In the v_{wCO2} text field, type 2.
- 7 Locate the Rate Constants section. In the $k^{\rm f}$ text field, type 1e100.
- **8** Locate the **Turbulent Flow** section. From the **Turbulent-reaction model** list, choose **Eddy-dissipation**.
- **9** Click to expand the **Regularization** section. Select the **Rate expressions** check box.

Reaction 2

- I Right-click Reaction I and choose Duplicate.
- 2 In the Settings window for Reaction, locate the Reaction Rate section.
- 3 In the v_{wCO} text field, type 0.
- **4** In the v_{wCO2} text field, type **0**.
- **5** In the v_{wH2} text field, type -2.
- **6** In the v_{wH2O} text field, type 2.

The reaction rates are now decided and can be used for each reaction.

CHEMISTRY (CHEM)

1: 2 CO + O2 = 2 CO2

- In the Model Builder window, under Component I (compl)>Chemistry (chem) click
 1: 2 CO + O2 = 2 CO2.
- 2 In the Settings window for Reaction, locate the Reaction Rate section.
- **3** From the list, choose **User defined**.
- **4** In the r_i text field, type tcs.treac1.r.
- 5 Find the Volumetric overall reaction order subsection. In the Forward text field, type 0.

- 2: 2 H2 + O2 = 2 H2O
- I In the Model Builder window, click 2: 2 H2 + O2 = 2 H2O.
- 2 In the Settings window for Reaction, locate the Reaction Rate section.
- **3** From the list, choose **User defined**.
- **4** In the r_i text field, type tcs.treac2.r.
- 5 Find the Volumetric overall reaction order subsection. In the Forward text field, type 0.

TRANSPORT OF CONCENTRATED SPECIES (TCS)

- I In the Model Builder window, under Component I (compl) click Transport of Concentrated Species (tcs).
- 2 In the Settings window for Transport of Concentrated Species, locate the **Transport Mechanisms** section.
- 3 From the Diffusion model list, choose Fick's law.
- 4 Locate the Species section. From the From mass constraint list, choose wN2.

Initial Values 1

- I In the Model Builder window, under Component I (compl)> Transport of Concentrated Species (tcs) click Initial Values 1.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the $\omega_{0,\text{wCO}}$ text field, type 0.
- **4** In the $\omega_{0,\text{wO}2}$ text field, type wcf_02.
- **5** In the $\omega_{0,wCO2}$ text field, type **0**.
- **6** In the $\omega_{0.wH2}$ text field, type 0.
- 7 In the $\omega_{0,wH2O}$ text field, type 0.

Inflow I

- I In the Physics toolbar, click Boundaries and choose Inflow.
- 2 Select Boundary 2 only.
- 3 In the Settings window for Inflow, locate the Inflow section.
- 4 From the Mixture specification list, choose Mole fractions.
- **5** In the $x_{0,\text{wCO}}$ text field, type x0_C0.
- **6** In the $x_{0,\text{wO}2}$ text field, type x0_02.
- 7 In the $x_{0,\text{wCO}2}$ text field, type x0_C02.
- **8** In the $x_{0,\text{wH}2}$ text field, type x0_H2.

9 In the $x_{0.\text{wH}2O}$ text field, type x0_H20.

Inflow 2

- I In the Physics toolbar, click Boundaries and choose Inflow.
- 2 In the Settings window for Inflow, locate the Inflow section.
- 3 In the $\omega_{0,wCO}$ text field, type 1e-5.
- **4** In the $\omega_{0,wO2}$ text field, type wcf_02.
- **5** In the $\omega_{0 \text{ wCO}2}$ text field, type 1e-5.
- **6** In the $\omega_{0,wH2}$ text field, type 1e-5.
- 7 In the $\omega_{0 \text{ wH}2O}$ text field, type 1e-5.
- 8 Select Boundaries 9 and 10 only.

Outflow I

- I In the Physics toolbar, click Boundaries and choose Outflow.
- 2 Select Boundary 3 only.

TURBULENT FLOW, K-ω(SPF)

Fluid Properties 1

- I In the Model Builder window, under Component I (compl)>Turbulent Flow, k-ω (spf) click Fluid Properties I.
- 2 In the Settings window for Fluid Properties, locate the Model Input section.
- **3** Click Make All Model Inputs Editable in the upper-right corner of the section.
- **4** Locate the Fluid Properties section. From the ρ list, choose Density (chem).
- **5** From the μ list, choose **User defined**. In the associated text field, type mu mix.

Inlet I

- I In the **Physics** toolbar, click **Boundaries** and choose **Inlet**.
- 2 Select Boundary 2 only.
- 3 In the Settings window for Inlet, locate the Boundary Condition section.
- **4** From the list, choose **Fully developed flow**.
- **5** Locate the **Fully Developed Flow** section. In the $U_{\rm av}$ text field, type Ujet.

Inlet 2

- I In the Physics toolbar, click Boundaries and choose Inlet.
- 2 Select Boundaries 9 and 10 only.
- 3 In the Settings window for Inlet, locate the Velocity section.

- 4 Click the **Velocity field** button.
- **5** Specify the \mathbf{u}_0 vector as

0	r
Ucf	z

- **6** Locate the **Turbulence Conditions** section. From the $I_{\rm T}$ list, choose **Low (0.01)**.
- 7 From the $L_{\rm T}$ list, choose User defined.
- 8 In the text field, type 0.1*Di.

Outlet I

- I In the Physics toolbar, click Boundaries and choose Outlet.
- 2 Select Boundary 3 only.
- 3 In the Settings window for Outlet, locate the Pressure Conditions section.
- 4 Select the Normal flow check box.

HEAT TRANSFER IN FLUIDS (HT)

Initial Values 1

- I In the Model Builder window, under Component I (compl)>Heat Transfer in Fluids (ht) click Initial Values 1.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the *T* text field, type T0.

Fluid 1

- I In the Model Builder window, click Fluid I.
- 2 In the Settings window for Fluid, locate the Model Input section.
- 3 Click Make All Model Inputs Editable in the upper-right corner of the section.
- 4 Locate the Heat Convection section. From the **u** list, choose Velocity field (spf).
- 5 Locate the Heat Conduction, Fluid section. From the k list, choose User defined. In the associated text field, type k mix.
- **6** Locate the Thermodynamics, Fluid section. From the ρ list, choose Density (chem).
- 7 From the C_p list, choose Heat capacity at constant pressure (chem).

Inflow I

- I In the Physics toolbar, click Boundaries and choose Inflow.
- 2 Select Boundaries 2, 9, and 10 only.

- 3 In the Settings window for Inflow, locate the Upstream Properties section.
- **4** In the T_{ustr} text field, type T0.

Outflow I

- I In the Physics toolbar, click Boundaries and choose Outflow.
- 2 Select Boundary 3 only.

MESH I

Mapped I

- I In the Mesh toolbar, click Mapped.
- 2 In the Settings window for Mapped, click to expand the Control Entities section.
- 3 Clear the Smooth across removed control entities check box.

Distribution I

- I Right-click Mapped I and choose Distribution.
- **2** Select Boundaries 2 and 15 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 20.
- 6 In the Element ratio text field, type 4.
- 7 From the Growth rate list, choose Exponential.

Distribution 2

- I In the Model Builder window, right-click Mapped I and choose Distribution.
- **2** Select Boundaries 11, 16, and 17 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 200.
- **6** In the **Element ratio** text field, type 250.
- 7 From the Growth rate list, choose Exponential.

Distribution 3

- I Right-click Mapped I and choose Distribution.
- **2** Select Boundaries 9 and 18 only.
- 3 In the Settings window for Distribution, locate the Distribution section.

- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 20.
- **6** In the **Element ratio** text field, type 400.
- 7 From the Growth rate list, choose Exponential.
- 8 Select the Reverse direction check box.

Distribution 4

- I Right-click Mapped I and choose Distribution.
- **2** Select Boundaries 1, 4, and 8 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- **5** In the **Number of elements** text field, type 20.
- 6 In the Element ratio text field, type 200.
- 7 From the Growth rate list, choose Exponential.
- 8 Select the Reverse direction check box.

Distribution 5

- I Right-click Mapped I and choose Distribution.
- **2** Select Boundary 12 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 20.
- 6 In the Element ratio text field, type 8.
- 7 From the Growth rate list, choose Exponential.

Distribution 6

- I Right-click Mapped I and choose Distribution.
- **2** Select Boundaries 3 and 13 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 20.
- 6 In the Element ratio text field, type 4.
- 7 From the Growth rate list, choose Exponential.
- 8 Click III Build All.

STUDY I

Solution I (soll)

- I In the Model Builder window, expand the Study I>Solver Configurations> Solution I (soll)>Stationary Solver I node, then click Segregated I.
- 2 In the Settings window for Segregated, locate the General section.
- 3 In the PID controller proportional text field, type 0.65.
- **4** In the **PID** controller derivative text field, type 0.025.
- 5 In the Target error estimate text field, type 0.1.
- 6 In the Model Builder window, expand the Study I>Solver Configurations>
 Solution I (solI)>Stationary Solver I>Segregated I node, then click Velocity u, Pressure p.
- 7 In the Settings window for Segregated Step, locate the General section.
- 8 Under Variables, click + Add.
- 9 In the Add dialog box, in the Variables list, choose Wall temperature, downside (compl.nirfl.TWall_d), Wall temperature, upside (compl.nirfl.TWall_u), and Temperature (compl.T).
- IO Click OK.
- II In the Model Builder window, under Study I>Solver Configurations>Solution I (soll)> Stationary Solver I>Segregated I click Turbulence variables.
- 12 In the Settings window for Segregated Step, click to expand the Method and Termination section.
- 13 In the Damping factor text field, type 0.4.
- 14 In the Number of iterations text field, type 2.
- 15 In the Model Builder window, under Study I>Solver Configurations>Solution I (soll)> Stationary Solver I>Segregated I right-click Temperature and choose Disable.

GLOBAL DEFINITIONS

The enthalpy of formation and heat capacity plots will now be created (Figure 1 and Figure 2).

Gas System I (pp I)

In the Model Builder window, expand the Global Definitions>Thermodynamics> Gas System 1 (pp1)>Mixture node.

Enthalpy of formation I (EnthalpyF_carbon_dioxide_Gas I 2, EnthalbyF carbon dioxide Gas 12 Dtemperature, EnthalpyF carbon dioxide Gas 12 Dpressure)

I In the Model Builder window, expand the Global Definitions>Thermodynamics> Gas System I (ppI)>Mixture>Vapor node, then click Global Definitions>Thermodynamics> Gas System I (ppI)>carbon dioxide>Vapor>

Enthalpy of formation I (EnthalpyF_carbon_dioxide_Gas I2,

EnthalpyF_carbon_dioxide_Gas12_Dtemperature,

EnthalpyF_carbon_dioxide_Gas I 2_Dpressure).

- 2 In the Settings window for Species Property, click to expand the Plot Parameters section.
- **3** In the table, enter the following settings:

Argument	Lower limit	Upper limit
temperature	298.15	2000

RESULTS

When working with the functions, they tend to load for a while. By choosing to manually save data in the model under **Results**, it will be possible to enable **Save plot data** under each plot group and therefore shorten the loading time.

- I In the Settings window for Results, locate the Save Data in the Model section.
- 2 From the Save plot data list, choose Manual.

Enthalby of Formation

- I In the Model Builder window, under Results click ID Plot Group I.
- 2 In the Settings window for ID Plot Group, type Enthalpy of Formation in the Label text field.
- 3 Locate the Save Data in the Model section. Select the Save plot data check box.
- 4 In a similar fashion, repeat the steps above, to create plots with the same temperature limits for the rest of the species.

ID Plot Group 2

In the Model Builder window, expand the Results>ID Plot Group 2 node.

Function I

In the Model Builder window, expand the Results>Enthalpy of Formation node, then click Function 1.

Function 2

- I Drag and drop below Enthalpy of Formation Function I.
- **2** Drag-drop all functions into the same plot group to plot them in the same graph.

Since ID Plot Group 2 - ID Plot Group 6 are empty now, delete them.

ID Plot Group 2, ID Plot Group 3, ID Plot Group 4, ID Plot Group 5, ID Plot Group 6

- In the Model Builder window, under Results, Ctrl-click to select ID Plot Group 2,
 ID Plot Group 3, ID Plot Group 4, ID Plot Group 5, and ID Plot Group 6.
- 2 Right-click and choose Delete.

The same procedure will now be performed for the heat capacity functions. As before, start by creating plots for each of the heat capacity functions.

GLOBAL DEFINITIONS

Heat capacity (Cp) | (HeatCapacityCp_carbon_dioxide_Gas | I, HeatCapacityCp_carbon_dioxide_Gas | I_Dtemperature, HeatCapacityCp_carbon_dioxide_Gas | I_Dpressure)

I In the Model Builder window, under Global Definitions>Thermodynamics>
Gas System I (ppI)>carbon dioxide>Vapor click

Heat capacity (Cp) I (HeatCapacityCp_carbon_dioxide_GasII, HeatCapacityCp_carbon_dioxide_GasII_Dtemperature, HeatCapacityCp_carbon_dioxide_GasII_Dpressure).

- 2 In the Settings window for Species Property, locate the Plot Parameters section.
- **3** In the table, enter the following settings:

Argument	Lower limit	Upper limit
temperature	298.15	2000

RESULTS

Heat Capacity

- I In the Settings window for ID Plot Group, type Heat Capacity in the Label text field.
- 2 Locate the Save Data in the Model section. Select the Save plot data check box.
- 3 Repeat creating plots for the functions **Heat capacity (Cp) 2 Heat capacity (Cp) 6** using the same temperature limits.

ID Plot Group 3

In the Model Builder window, expand the Results>ID Plot Group 3 node.

Function I

In the Model Builder window, expand the Results>Heat Capacity node, then click Function 1.

Function 2

- I Drag and drop below Heat Capacity Function I.
- 2 Repeat the drag-dropping of functions 3-6 into the **Heat Capacity** plot group.

ID Plot Group 3, ID Plot Group 4, ID Plot Group 5, ID Plot Group 6, ID Plot Group 7 Since ID Plot Group 3 - ID Plot Group 7 are empty now, delete them.

- I In the Model Builder window, under Results, Ctrl-click to select ID Plot Group 3, ID Plot Group 4, ID Plot Group 5, ID Plot Group 6, and ID Plot Group 7.
- 2 Right-click and choose **Delete**.

Now we have two plots: one contains all enthalpy of formation functions, one contains all heat capacity functions.

Enthalpy of Formation

- I In the Model Builder window, under Results click Enthalpy of Formation.
- 2 In the Settings window for ID Plot Group, click to expand the Title section.
- **3** From the **Title type** list, choose **None**.
- 4 Locate the **Plot Settings** section.
- 5 Select the x-axis label check box. In the associated text field, type Temperature (K).
- 6 Select the y-axis label check box. In the associated text field, type Enthalpy of Formation (J/mol).
- 7 Locate the Legend section. From the Layout list, choose Outside graph axis area.

Function 1

- I In the Model Builder window, click Function I.
- 2 In the Settings window for Function, click to expand the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.

5 In the table, enter the following settings:

Legends	
C02	

Function 2

- I In the Model Builder window, click Function 2.
- 2 In the Settings window for Function, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends CO

Function 3

- I In the Model Builder window, click Function 3.
- 2 In the Settings window for Function, locate the Legends section.
- 3 Select the Show legends check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends H2

Function 4

- I In the Model Builder window, click Function 4.
- 2 In the Settings window for Function, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.
- 5 In the table, enter the following settings:

Legends N2

Function 5

I In the Model Builder window, click Function 5.

- 2 In the Settings window for Function, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends 02

Function 6

- I In the Model Builder window, click Function 6.
- 2 In the Settings window for Function, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends H20

6 In the Enthalpy of Formation toolbar, click **Plot**.

Heat Capacity

All datasets Grid ID I - Grid ID Ik contain the same information. Therefore, change the dataset to be the same as for the **Enthalpy of Formation** plot group.

- I In the Model Builder window, under Results click Heat Capacity.
- 2 In the Settings window for ID Plot Group, locate the Data section.
- 3 From the Dataset list, choose Grid ID 1.
- 4 Locate the Title section. From the Title type list, choose None.
- 5 Locate the **Plot Settings** section.
- 6 Select the x-axis label check box. In the associated text field, type Temperature (K).
- 7 Select the y-axis label check box. In the associated text field, type Heat Capacity (J/ mol/K).
- 8 Locate the Legend section. From the Layout list, choose Outside graph axis area.

Function I

- I In the Model Builder window, click Function I.
- 2 In the Settings window for Function, locate the Legends section.

- 3 Select the Show legends check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends C02

Function 2

- I In the Model Builder window, click Function 2.
- 2 In the Settings window for Function, locate the Legends section.
- 3 Select the Show legends check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends CO

Function 3

- I In the Model Builder window, click Function 3.
- 2 In the Settings window for Function, locate the Legends section.
- 3 Select the Show legends check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends	
H2	

Function 4

- I In the Model Builder window, click Function 4.
- 2 In the Settings window for Function, locate the Legends section.
- 3 Select the Show legends check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends	
N2	

Function 5

- I In the Model Builder window, click Function 5.
- 2 In the Settings window for Function, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends 02

Function 6

- I In the Model Builder window, click Function 6.
- 2 In the Settings window for Function, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 From the Legends list, choose Manual.
- **5** In the table, enter the following settings:

Legends H20

6 In the Heat Capacity toolbar, click **Plot**.

The datasets that are not used can now be deleted.

I Delete all datasets Grid ID Ia to Grid ID Ik.

Now are the graphs for enthalpy of formation and heat capacity finished and are presented as Figure 1 and Figure 2 in the Model Definition section. To obtain the values presented in Table 1 and Table 2, Evaluation Groups are used, which gives the values for each function at the specific temperature.

Evaluation Group 1

- I In the Results toolbar, click Evaluation Group.
- 2 In the Settings window for Evaluation Group, locate the Transformation section.
- **3** Select the **Transpose** check box.

Enthalpy of Formation, 298 K

- I Right-click Evaluation Group I and choose Global Evaluation.
- 2 In the Settings window for Global Evaluation, type Enthalpy of Formation, 298 Kin the Label text field.

3 Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
EnthalpyF_carbon_dioxide_Gas 12(298.15[K],1.0133E5[Pa])	J/mol	Enthalpy of formation 1
EnthalpyF_carbon_monoxide_Ga s14(298.15[K],1.0133E5[Pa])	J/mol	Enthalpy of formation 2
EnthalpyF_hydrogen_Gas16(298 .15[K],1.0133E5[Pa])	J/mol	Enthalpy of formation 3
EnthalpyF_nitrogen_Gas18(298 .15[K],1.0133E5[Pa])	J/mol	Enthalpy of formation 4
EnthalpyF_oxygen_Gas110(298. 15[K],1.0133E5[Pa])	J/mol	Enthalpy of formation 5
EnthalpyF_water_Gas112(298.1 5[K],1.0133E5[Pa])	J/mol	Enthalpy of formation 6

If clicking the **Evaluate** button now, no values will be given. This is because the datasets are empty. Using the feature Get initial values under Study I enables evaluation of the function values in Enthalpy of Formation, 298 K.

STUDY I

In the Study toolbar, click $t_{=0}^{U}$ Get Initial Value.

RESULTS

Enthalpy of Formation, 298 K

- I In the Model Builder window, under Results>Evaluation Group I click Enthalpy of Formation, 298 K.
- 2 In the Evaluation Group I toolbar, click **= Evaluate**.

Heat Capacity, 300 K

- I In the Model Builder window, right-click Evaluation Group I and choose Global Evaluation.
- 2 In the Settings window for Global Evaluation, type Heat Capacity, 300 K in the Label text field.

3 Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
HeatCapacityCp_carbon_dioxi de_Gas11(300[K], 1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 1
<pre>HeatCapacityCp_carbon_monox ide_Gas13(300[K], 1.0133E5[Pa])</pre>	J/(mol*K)	Heat capacity (Cp) 2
HeatCapacityCp_hydrogen_Gas 15(300[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 3
<pre>HeatCapacityCp_nitrogen_Gas 17(300[K],1.0133E5[Pa])</pre>	J/(mol*K)	Heat capacity (Cp) 4
HeatCapacityCp_oxygen_Gas19 (300[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 5
HeatCapacityCp_water_Gas111 (300[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 6

4 In the Evaluation Group I toolbar, click **= Evaluate**.

Heat Capacity, 2000 K

- I Right-click Evaluation Group I and choose Global Evaluation.
- 2 In the Settings window for Global Evaluation, type Heat Capacity, 2000 K in the Label text field.
- **3** Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
HeatCapacityCp_carbon_dioxi de_Gas11(2000[K], 1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 1
HeatCapacityCp_carbon_monox ide_Gas13(2000[K], 1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 2
HeatCapacityCp_hydrogen_Gas 15(2000[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 3
HeatCapacityCp_nitrogen_Gas 17(2000[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 4
HeatCapacityCp_oxygen_Gas19 (2000[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 5
HeatCapacityCp_water_Gas111 (2000[K],1.0133E5[Pa])	J/(mol*K)	Heat capacity (Cp) 6

4 In the Evaluation Group I toolbar, click **= Evaluate**.

The values in rows 7-12 in the table from **Evaluation Group 1** are for 300 K, while the values for rows 13-18 are for 2000 K. Together with the values in rows 1-6, these are presented in Table 1 and Table 2.

STUDY I

Solution I (soll)

I In the Model Builder window, under Study I>Solver Configurations right-click Solution I (solI) and choose Compute.

The default plots that are supposed to be generated when clicking **Compute** were not generated this time because they had already been generated when performing the **Get initial values** step. Therefore, they need to be reset.

2 In the Study toolbar, click Reset Default Plots.

Now move on to postprocess the result from the nonisothermal jet. Start by creating a **Mirror 2D** dataset as well as a revolved 3D dataset.

RESULTS

Mirror 2D | In the Results toolbar, click | More Datasets and choose Mirror 2D.

Cut Line 2D I

- I In the Results toolbar, click Cut Line 2D.
- 2 In the Settings window for Cut Line 2D, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D 1.
- 4 Locate the Line Data section. From the Line entry method list, choose Point and direction.
- 5 Find the Point subsection. In the y text field, type P1+20*Di.
- 6 Click to expand the **Advanced** section. Find the **Space variable** subsection. In the **x** text field, type r mirr20.

Cut Line 2D 2

- I In the Results toolbar, click Cut Line 2D.
- 2 In the Settings window for Cut Line 2D, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D 1.

- 4 Locate the Line Data section. From the Line entry method list, choose Point and direction.
- 5 Find the Point subsection. In the y text field, type P1+50*Di.
- 6 Locate the Advanced section. Find the Space variable subsection. In the x text field, type r mirr50.

Now apply the mirror dataset to the relevant plot groups.

Velocity (spf)

- I In the Model Builder window, under Results click Velocity (spf).
- 2 In the Settings window for 2D Plot Group, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D 1.
- 4 In the Velocity (spf) toolbar, click Plot.

Streamline 1

Right-click Velocity (spf) and choose Streamline.

Streamline 1

- I In the Model Builder window, expand the Results>Velocity (spf) node, then click Streamline 1.
- 2 In the Settings window for Streamline, click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component I (compl)> Heat Transfer in Fluids>Velocity and pressure>ht.ur,ht.uz - Velocity field.
- 3 Locate the Streamline Positioning section. From the Positioning list, choose Uniform density.
- 4 In the Separating distance text field, type 0.035.
- 5 Locate the Coloring and Style section. Find the Point style subsection. From the Color list, choose Gray.
- 6 In the Velocity (spf) toolbar, click Plot.
- 7 Click the Zoom Extents button in the Graphics toolbar.

Pressure (sbf)

- I In the Model Builder window, under Results click Pressure (spf).
- 2 In the Settings window for 2D Plot Group, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D 1.
- 4 In the Pressure (spf) toolbar, click Plot.

Wall Resolution (spf)

- I In the Model Builder window, click Wall Resolution (spf).
- 2 In the Settings window for 2D Plot Group, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D 1.

Mass fraction, CO2

- I In the Model Builder window, right-click Concentration, CO2 (tcs) and choose Duplicate.
- 2 In the Settings window for 2D Plot Group, type Mass fraction, CO2 in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Mirror 2D 1.
- 4 Locate the Plot Settings section. From the Color list, choose White.

Surface I

- I In the Model Builder window, expand the Mass fraction, CO2 node, then click Surface I.
- 2 In the Settings window for Surface, locate the Expression section.
- **3** In the **Expression** text field, type wCO2.
- 4 In the Mass fraction, CO2 toolbar, click Plot.
- **5** Click the **Zoom Extents** button in the **Graphics** toolbar.

Temperature, 3D (ht)

- I In the Model Builder window, under Results click Temperature, 3D (ht).
- 2 In the Settings window for 3D Plot Group, locate the Plot Settings section.
- 3 Clear the Plot dataset edges check box.

Import the experimental data files. The files correspond to the ones published online (Ref. 2) by R. Barlow and coworkers. The name of the model, round_jet_burner, has been prepended to the filenames.

Centerline data

- I In the Results toolbar, click Table.
- 2 In the Settings window for Table, type Centerline data in the Label text field.
- **3** Locate the **Data** section. Click **Import**.
- **4** Browse to the model's Application Libraries folder and double-click the file round_jet_burner_chnAclY.fav.

z/Di = 20, Radial Data

I In the Results toolbar, click **Table**.

- 2 In the Settings window for Table, type z/Di = 20, Radial Data in the Label text field.
- 3 Locate the Data section. Click Import.
- **4** Browse to the model's Application Libraries folder and double-click the file round_jet_burner_chnAd20Y.fav.

z/Di = 50, Radial Data

- I In the Results toolbar, click **Table**.
- 2 In the Settings window for Table, type z/Di = 50, Radial Data in the Label text field.
- 3 Locate the Data section. Click Import.
- 4 Browse to the model's Application Libraries folder and double-click the file round jet burner chnAd50Y.fav.

z/Di = 20, Radial Velocity Data

- I In the **Results** toolbar, click **Table**.
- 2 In the Settings window for Table, type z/Di = 20, Radial Velocity Data in the Label text field.
- 3 Locate the Data section. Click Import.
- 4 Browse to the model's Application Libraries folder and double-click the file round jet burner seg1420.dat.

z/Di = 50, Radial Velocity Data

- I In the Results toolbar, click Table.
- 2 In the Settings window for Table, type z/Di = 50, Radial Velocity Data in the Label text field.
- 3 Locate the Data section. Click Import.
- **4** Browse to the model's Application Libraries folder and double-click the file round jet burner seq1450.dat.

ID Plot Group 22

In the Results toolbar, click \sim ID Plot Group.

- I Right-click ID Plot Group 22 and choose Line Graph.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Line Graph, locate the y-Axis Data section.
- 4 In the Expression text field, type T/T0.
- 5 Locate the x-Axis Data section. From the Parameter list, choose Expression.

- 6 In the Expression text field, type (z-P1)/Di.
- 7 Click to expand the Coloring and Style section. From the Color list, choose Black.
- 8 Click to expand the **Legends** section. Select the **Show legends** check box.
- 9 From the Legends list, choose Manual.
- **10** In the table, enter the following settings:

LegendsModel

Table Graph 1

- I In the Model Builder window, right-click ID Plot Group 22 and choose Table Graph.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 From the x-axis data list, choose r(mm).
- 4 From the Plot columns list, choose Manual.
- 5 In the Columns list, select T(K).
- 6 Click to expand the **Preprocessing** section. Find the **x-axis column** subsection. From the **Preprocessing** list, choose **Linear**.
- 7 In the Scaling text field, type 1/(Di*1000).
- 8 Find the y-axis columns subsection. From the Preprocessing list, choose Linear.
- **9** In the **Scaling** text field, type 1/T0.
- 10 Locate the Coloring and Style section. Find the Line style subsection. From the Line list, choose None.
- II From the Color list, choose Black.
- 12 Find the Line markers subsection. From the Marker list, choose Square.
- 13 Click to expand the Legends section. Select the Show legends check box.
- 14 From the Legends list, choose Manual.
- **I5** In the table, enter the following settings:

LegendsExp.

T @ centerline

- I In the Model Builder window, under Results click ID Plot Group 22.
- 2 In the Settings window for ID Plot Group, type T @ centerline in the Label text field.
- 3 Locate the Plot Settings section.

- 4 Select the x-axis label check box. In the associated text field, type (z-Pl)/Di.
- **5** Select the **y-axis label** check box. In the associated text field, type T/T0.
- 6 Locate the Axis section. Select the Manual axis limits check box.
- 7 In the x minimum text field, type -10.
- 8 In the x maximum text field, type 120.
- **9** In the **y minimum** text field, type **0.5**.
- **10** In the y maximum text field, type 8.
- II Locate the Legend section. From the Layout list, choose Outside graph axis area.
- 12 Click to expand the Title section. From the Title type list, choose Manual.
- 13 In the Title text area, type Temperature Along the Centerline.
- 14 In the T @ centerline toolbar, click Plot.

ID Plot Group 23

- I In the Home toolbar, click Add Plot Group and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, locate the Data section.
- 3 From the Dataset list, choose None.

Line Grabh I

- I Right-click ID Plot Group 23 and choose Line Graph.
- 2 In the Settings window for Line Graph, locate the Data section.
- 3 From the Dataset list, choose Cut Line 2D 1.
- **4** Locate the **y-Axis Data** section. In the **Expression** text field, type T/T0.
- 5 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 6 In the Expression text field, type r mirr20/Di.
- 7 Locate the Coloring and Style section. From the Color list, choose Black.
- **8** Locate the **Legends** section. Select the **Show legends** check box.
- 9 From the Legends list, choose Manual.
- **10** In the table, enter the following settings:

Legends		
z/Di =	20,	Model

- I Right-click Line Graph I and choose Duplicate.
- 2 In the Settings window for Line Graph, locate the Data section.

- 3 From the Dataset list, choose Cut Line 2D 2.
- 4 Locate the x-Axis Data section. In the Expression text field, type r_mirr50/Di.
- 5 Locate the Coloring and Style section. Find the Line style subsection. From the Line list, choose Dashed.
- **6** Locate the **Legends** section. In the table, enter the following settings:

Legends				
z/Di	=	50,	Model	

7 In the ID Plot Group 23 toolbar, click **Plot**.

Table Graph 1

- I In the Model Builder window, right-click ID Plot Group 23 and choose Table Graph.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 From the Table list, choose z/Di = 20, Radial Data.
- 4 From the x-axis data list, choose r(mm).
- 5 From the Plot columns list, choose Manual.
- 6 In the Columns list, select T(K).
- **7** Locate the **Preprocessing** section. Find the **x-axis column** subsection. From the **Preprocessing** list, choose **Linear**.
- 8 In the Scaling text field, type 1/(Di*1000).
- 9 Find the y-axis columns subsection. From the Preprocessing list, choose Linear.
- 10 In the Scaling text field, type 1/T0.
- II Locate the Coloring and Style section. Find the Line style subsection. From the Line list, choose None.
- 12 From the Color list, choose Black.
- 13 Find the Line markers subsection. From the Marker list, choose Square.
- **14** Locate the **Legends** section. Select the **Show legends** check box.
- 15 From the Legends list, choose Manual.
- **16** In the table, enter the following settings:

Legend	ds		
z/Di	=	20,	Exp

Table Graph 2

I Right-click Table Graph I and choose Duplicate.

- 2 In the Settings window for Table Graph, locate the Data section.
- 3 From the Table list, choose z/Di = 50, Radial Data.
- 4 Locate the Coloring and Style section. Find the Line markers subsection. From the Marker list, choose Triangle.
- 5 From the Positioning list, choose Interpolated.
- **6** Locate the **Legends** section. In the table, enter the following settings:

Legend	ds			
z/Di	=	50,	Exp	

$$T @ z/Di = 20, 50$$

- I In the Model Builder window, under Results click ID Plot Group 23.
- 2 In the Settings window for ID Plot Group, type T @ z/Di = 20, 50 in the Label text field.
- 3 Locate the Title section. From the Title type list, choose Manual.
- 4 In the Title text area, type Temperature Downstream of the Pipe Exit.
- 5 Locate the Plot Settings section.
- 6 Select the x-axis label check box. In the associated text field, type r/Di.
- 7 Select the y-axis label check box. In the associated text field, type T/T0.
- **8** Locate the **Axis** section. Select the **Manual axis limits** check box.
- **9** In the **x minimum** text field, type -10.
- 10 In the x maximum text field, type 10.
- II In the y minimum text field, type 0.5.
- 12 In the y maximum text field, type 8.
- 13 Locate the Legend section. From the Layout list, choose Outside graph axis area.
- **14** In the **T @ z/Di = 20**, **50** toolbar, click **◎ Plot**.

$$uz @ z/Di = 20, 50$$

- I In the Model Builder window, right-click T @ z/Di = 20, 50 and choose Duplicate.
- 2 In the Settings window for ID Plot Group, type uz @ z/Di = 20, 50 in the Label text field.

Line Graph 1

I In the Model Builder window, expand the uz @ z/Di = 20, 50 node, then click Line Graph 1.

- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- 3 In the Expression text field, type w/Ujet.

Line Graph 2

- I In the Model Builder window, click Line Graph 2.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- 3 In the Expression text field, type w/Ujet.

Table Graph 1

- I In the Model Builder window, click Table Graph I.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 From the x-axis data list, choose Fblgr.
- 4 From the Table list, choose z/Di = 20, Radial Velocity Data.
- 5 In the Columns list, select uz.
- **6** Locate the **Preprocessing** section. Find the **y-axis columns** subsection. In the **Scaling** text field, type 1/Ujet.

Table Graph 2

- I In the Model Builder window, click Table Graph 2.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 From the x-axis data list, choose Fblgr.
- 4 From the Table list, choose z/Di = 50, Radial Velocity Data.
- 5 In the Columns list, select uz.
- 6 Locate the **Preprocessing** section. Find the **y-axis columns** subsection. In the **Scaling** text field, type 1/Ujet.

$$uz @ z/Di = 20.50$$

- I In the Model Builder window, click uz @ z/Di = 20, 50.
- 2 In the Settings window for ID Plot Group, locate the Title section.
- 3 From the Title type list, choose Manual.
- 4 In the Title text area, type Axial Velocity Downstream of the Pipe Exit.
- 5 Locate the Plot Settings section. In the y-axis label text field, type uz/Ujet.
- 6 Locate the Axis section. In the y minimum text field, type -0.25.
- 7 In the y maximum text field, type 1.25.
- 8 In the uz @ z/Di = 20, 50 toolbar, click Plot.

CO, N2 @ centerline

- I In the Model Builder window, right-click T @ centerline and choose Duplicate.
- 2 In the Settings window for ID Plot Group, type CO, N2 @ centerline in the Label text field.
- 3 Locate the Title section. In the Title text area, type Mass Fraction Along the Centerline.
- 4 Locate the Plot Settings section. In the y-axis label text field, type wCO, wN2.
- 5 Locate the Axis section. In the y minimum text field, type -0.05.
- 6 In the y maximum text field, type 1.
- 7 In the CO, N2 @ centerline toolbar, click Plot.

Line Graph 1

- I In the Model Builder window, expand the CO, N2 @ centerline node, then click Line Graph 1.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type wCO.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends CO, Model

Table Graph 1

- I In the Model Builder window, click Table Graph I.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 In the Columns list, select YCO.
- 4 Locate the Preprocessing section. Find the y-axis columns subsection. In the Scaling text field, type 1.
- **5** Locate the **Legends** section. In the table, enter the following settings:

Legends CO, Exp.

6 In the CO, N2 @ centerline toolbar, click Plot.

Line Graph 2

I In the Model Builder window, under Results>CO, N2 @ centerline right-click Line Graph I and choose **Duplicate**.

- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type wN2.
- 4 Locate the Coloring and Style section. Find the Line style subsection. From the Line list, choose Dashed.
- **5** Locate the **Legends** section. In the table, enter the following settings:

Legends N2, Model

Table Graph 2

- I In the Model Builder window, under Results>CO, N2 @ centerline right-click
 Table Graph I and choose Duplicate.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 In the Columns list, select YN2.
- 4 Locate the Coloring and Style section. Find the Line markers subsection. From the Marker list, choose Triangle.
- 5 From the Positioning list, choose Interpolated.
- **6** Locate the **Legends** section. In the table, enter the following settings:

Legends N2, Exp

7 In the CO, N2 @ centerline toolbar, click Plot.

H2, H20 @ centerline

- I In the Model Builder window, right-click CO, N2 @ centerline and choose Duplicate.
- 2 In the Settings window for ID Plot Group, type H2, H20 @ centerline in the Label text field.
- 3 Locate the Title section. From the Title type list, choose Manual.
- 4 In the Title text area, type Mass Fraction Along the Centerline.

- I In the Model Builder window, expand the H2, H20 @ centerline node, then click Line Graph I.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type wH2.

4 Locate the **Legends** section. In the table, enter the following settings:

Legends H2, Model

Table Graph 1

- I In the Model Builder window, click Table Graph I.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 In the Columns list, select YH2.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends H2, Exp.

Line Graph 2

- I In the Model Builder window, click Line Graph 2.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type wH20.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends H2O, Model

Table Graph 2

- I In the Model Builder window, click Table Graph 2.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 In the Columns list, select YH20.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends H2O, Exp

H2, H20 @ centerline

- I In the Model Builder window, click H2, H20 @ centerline.
- 2 In the Settings window for ID Plot Group, locate the Plot Settings section.
- 3 In the y-axis label text field, type wH2, wH20.
- 4 Locate the Axis section. In the y maximum text field, type 0.15.

- 5 In the y minimum text field, type -0.02.
- 6 In the H2, H20 @ centerline toolbar, click Plot.

02, CO2 @ centerline

- I In the Model Builder window, right-click H2, H20 @ centerline and choose Duplicate.
- 2 In the Settings window for ID Plot Group, type 02, CO2 @ centerline in the Label text field.
- 3 Locate the Title section. From the Title type list, choose Manual.
- 4 In the Title text area, type Mass Fraction Along the Centerline.

Line Graph 1

- I In the Model Builder window, expand the 02, CO2 @ centerline node, then click Line Graph 1.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type w02.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends 02, Model

Table Graph 1

- I In the Model Builder window, click Table Graph I.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 In the Columns list, select YO2.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends 02, Exp.

- I In the Model Builder window, click Line Graph 2.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- 3 In the Expression text field, type wCO2.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends		
CO2,	Model	

Table Graph 2

- I In the Model Builder window, click Table Graph 2.
- 2 In the Settings window for Table Graph, locate the Data section.
- **3** In the **Columns** list, select **YCO2**.
- **4** Locate the **Legends** section. In the table, enter the following settings:

Legends CO2, Exp

O2, CO2 @ centerline

- I In the Model Builder window, click 02, CO2 @ centerline.
- 2 In the Settings window for ID Plot Group, locate the Plot Settings section.
- 3 In the y-axis label text field, type w02, wC02.
- 4 Locate the Axis section. In the y minimum text field, type -0.05.
- 5 In the y maximum text field, type 0.4.
- 6 In the **02**, **C02** @ centerline toolbar, click **Plot**.