Created in COMSOL Multiphysics 6.0

Forchheimer Flow

Introduction

This is a tutorial of the coupling between flow of a fluid in an open channel and a porous block attached to one of the channel walls. The flow is described by the Navier-Stokes equation in the free region and a Forchheimer-corrected version of the Brinkman equations in the porous region.

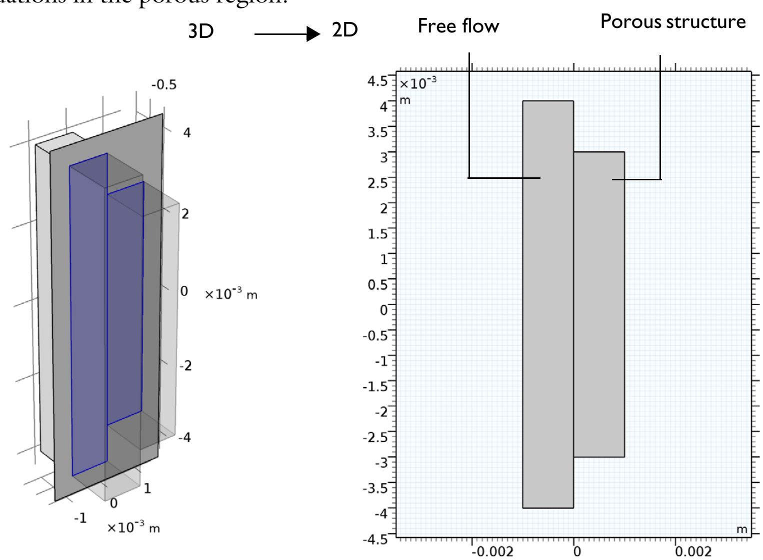


Figure 1: Depiction of the modeling geometry and domain. The 3D geometry can be reduced to a 2D representation assuming that changes through the thickness are negligible.

The coupling of free media flow with porous media flow is common in the fields of earth science and chemical engineering. Perhaps the most frequent way to deal with coupled free and porous media flow is to incorporate Darcy's law adjacent to Navier-Stokes because it is usually numerically easy to solve. However, this approach does not account for viscous effects arising from the free media flow, which may still be important in the region close to the free-porous structure interface. Depending on the pore size and pore distribution, but also the fluid's properties, it can therefore be an oversimplification to employ Darcy's law. The Brinkman equations account for momentum transport by macroscopic viscous effects as well as pressure gradients (stemming from microscopic shear effects inside each pore channel) and can be considered an extension of Darcy's Law.

Still, the Brinkman equations assume laminar flow. Looking at processes in relatively open structures, like gas flow through packed beds, there is also a turbulent contribution to the resistance to flow. In those cases, an additional term accounts for the turbulent contribution to the resistance to flow in the porous domain. The Forchheimer equation (also accredited to Ergun) is widely used to predict pressure drops in packed beds. This equation can generally be written as

$$\frac{\Delta p}{L} = \alpha_1 u + \alpha_2 u^2$$

The left-hand side is the pressure drop per unit length of traveled distance through the bed. The first term on the right-hand side represents the Blake-Kozeny equation for laminar flow. The pressure drop depends linearly on the average linear velocity u for laminar flow, corresponding to Darcy flow. The second term is from the purely turbulent Burke-Plummer equation where the pressure drop is proportional to the square of the velocity. Description of an intermediate flow, where both the laminar and turbulent effects are important, requires the two-term Forchheimer equation. The coefficients α_1 and α_2 are functions of porosity, viscosity, average pore diameter, and fluid density.

Model Definition

Figure 2 below shows the example domain and notations for the boundary conditions.

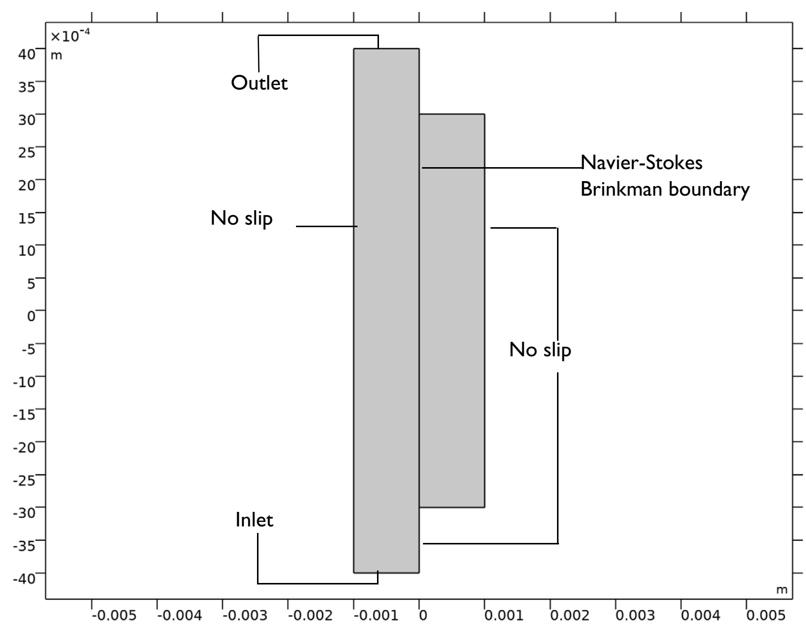


Figure 2: Modeled domain and boundary notations. Flow enters at the bottom and leaves at the top. The region of porous structure is not as long as the free channel.

Flow in the free channel is described by the stationary, incompressible Navier-Stokes equations:

$$\rho(\mathbf{u}\cdot\nabla)\mathbf{u} = -\nabla\cdot[-p\mathbf{I}+\mu(\nabla\mathbf{u}+(\nabla\mathbf{u})^T)]$$
$$\nabla\cdot\mathbf{u} = 0 \qquad (1)$$

where μ denotes the dynamic viscosity (Pa·s), **u** refers to the velocity in the open channel (m/s), ρ is the fluid's density (kg/m^3), and p is the pressure (Pa). In the porous domain, the Brinkman equations with Forchheimer correction describe the flow:

$$\frac{1}{\varepsilon_p}\rho(\mathbf{u}\cdot\nabla)\mathbf{u}\frac{1}{\varepsilon_p} = \nabla\cdot\left[-p\mathbf{I}+\frac{\mu}{\varepsilon_p}(\nabla\mathbf{u}+(\nabla\mathbf{u})^T)\right]-\left(\frac{\mu}{\kappa}+\frac{\rho\varepsilon_p C_f}{\sqrt{\kappa}}|\mathbf{u}|\right)\mathbf{u}$$
$$\rho\nabla\cdot\mathbf{u} = 0 \qquad (2)$$

Here κ denotes the permeability of the porous medium (m^2), ε_p is the porosity (dimensionless), and the dimensionless friction coefficient is (Ref. 1)

$$C_f = \frac{1.75}{\sqrt{150\varepsilon_p^3}}$$

As Equation 1 and Equation 2 reveal, the momentum transport equations are closely related. The term on the left-hand side of the Navier-Stokes formulation corresponds to momentum transferred by convection in free flow. The Brinkman formulation replaces this term by a contribution associated with the drag force experienced by the fluid flowing through a porous medium. In addition, the last term in the right-hand side of Equation 2 presents the Forchheimer correction for turbulent drag contributions.

In COMSOL Multiphysics, it is easy to set up and solve such a coupled flow regime. The implementation of the extra drag is done with a Forchheimer coefficient (kg/m^4) equal to

$$\beta_F = \frac{\rho\varepsilon_p C_f}{\sqrt{k}}$$

At the flow inlet a normal inflow velocity $\mathbf{u}=-U_0\mathbf{n}$ is defined. At the flow outlet the fluid can leave the domain. The outlet boundary condition with the pressure option selected sets the normal stress component equal to the pressure at the outlet. The tangential stress component vanishes. All other boundaries are defined as walls with a no slip condition $\mathbf{u}=0$.

The following table lists the input data for the example:

PROPERTY	VALUE	DESCRIPTION
μ	10^{-3} kg/(m·s)	Dynamic viscosity
ρ	1000 kg/m^3	Density
κ	10^{-7} m^2	Permeability
ε_p	0.4	Porosity
v_0	2 cm/s	Inlet velocity

Results and Discussion

Figure 3 shows the velocity field in the open channel and porous structure. The plot reveals that there are slight disturbances in the velocity at the porous wall, which suggests momentum transport by viscous effects.

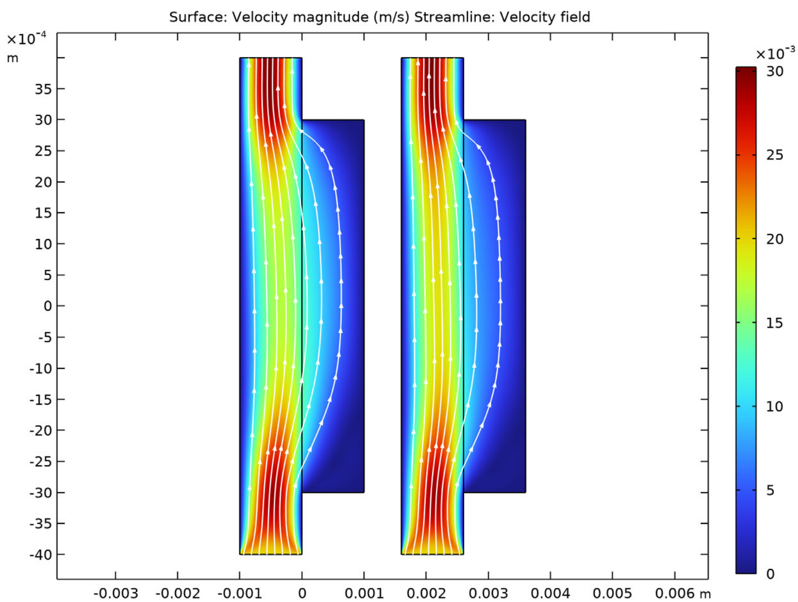


Figure 3: Velocity field without Forchheimer correction (left) and with Forchheimer correction (right).

Figure 4 contains a cross-sectional velocity plot. It shows that without the Forchheimer correction, the resistance to flow is underestimated in the porous domain. The added correction gives a solution with slower flow in the porous domain and a faster flow in the free domain, due to incompressibility.

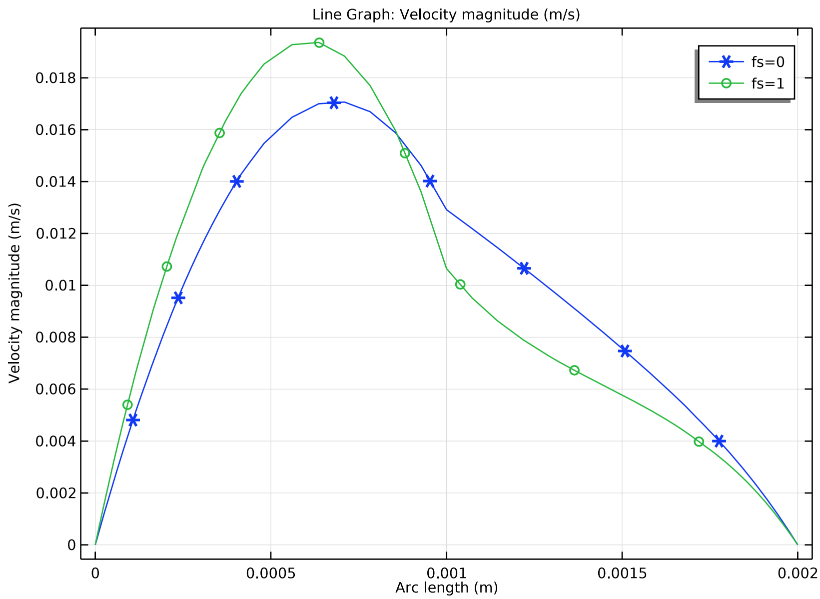


Figure 4: Cross section of the velocity field (velocity magnitude) in the middle of the modeling domain with and without the Forchheimer correction.

Further postprocessing would show that the shear rate perpendicular to the flow is also continuous. This implies that there is significant viscous momentum transfer across the interface and into the porous material, a transport that is not accounted for by Darcy's law.

Notes About the COMSOL Implementation

To implement the Forchheimer pressure drop relation in a differential equation framework, this example uses an approach suggested in Ref. 1 in which the Brinkman momentum balance is amended with a Forchheimer term. The system studied in this example is that of a 2D cross section of a rectangular channel with a porous layer attached to one of its walls. Flow enters the volume with a uniform velocity profile and develops throughout the length of the channel.

Reference

1. A. Amiri and K. Vafai, "Transient Analysis of Incompressible Flow Through a Packed Bed," *Int. J. Heat and Mass Transfer*, vol. 41, pp. 4259–4279, 1998.

Application Library path: `Subsurface_Flow_Module/Fluid_Flow/forchheimer_flow`

Modeling Instructions

From the **File** menu, choose **New**.

NEW

In the **New** window, click **Model Wizard**.

MODEL WIZARD

1 In the **Model Wizard** window, click **2D**.
2 In the **Select Physics** tree, select **Fluid Flow>Porous Media and Subsurface Flow>Free and Porous Media Flow (fp)**.
3 Right-click and choose **Add Physics**.
4 Click **Study**.
5 In the **Select Study** tree, select **General Studies>Stationary**.
6 Click **Done**.

GEOMETRY 1

Rectangle 1 (r1)

1 In the **Geometry** toolbar, click **Rectangle**.
2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.
3 In the **Width** text field, type `1e-3`.
4 In the **Height** text field, type `6e-3`.
5 Locate the **Position** section. In the **y** text field, type `-3e-3`.

Rectangle 2 (r2)

1 In the **Geometry** toolbar, click **Rectangle**.
2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.

3 In the **Width** text field, type `1e-3`.

4 In the **Height** text field, type `8e-3`.

5 Locate the **Position** section. In the **x** text field, type `-1e-3`.

6 In the **y** text field, type `-4e-3`.

7 In the **Geometry** toolbar, click **Build All**.

GLOBAL DEFINITIONS

Parameters 1

1 In the **Model Builder** window, under **Global Definitions** click **Parameters 1**.

2 In the **Settings** window for **Parameters**, locate the **Parameters** section.

3 In the table, enter the following settings:

Name	Expression	Value	Description
v0	2[cm/s]	0.02 m/s	Inlet velocity
eps_p	0.4	0.4	Porosity
Cf	1.75/sqrt(150*eps_p^3)	0.56481	Friction coefficient
fs	1	1	Switch for Forchheimer terms

FREE AND POROUS MEDIA FLOW (FP)

Porous Medium 1

1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Free and Porous Media Flow (fp)** and choose **Porous Medium**.

2 Select Domain 2 only.

MATERIALS

Fluid

1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Materials** and choose **Blank Material**.

2 In the **Settings** window for **Material**, type `Fluid` in the **Label** text field.

3 Locate the **Material Contents** section. In the table, enter the following settings:

Property	Variable	Value	Unit	Property group
Density	rho	1000[kg/m^3]	kg/m³	Basic
Dynamic viscosity	mu	1e-3[Pa*s]	Pa·s	Basic

Porous Material 1 (pmat1)

1 Right-click **Materials** and choose **More Materials>Porous Material**.

2 Select Domain 2 only.

3 In the **Settings** window for **Porous Material**, locate the **Porosity** section.

4 In the εp text field, type `eps_p`.

5 Locate the **Homogenized Properties** section. In the table, enter the following settings:

Property	Variable	Value	Unit	Property group
Permeability	kappa_iso ; kappaii = kappa_iso, kappaij = 0	1e-7	m²	Basic

6 Locate the **Phase-Specific Properties** section. Click **Add Required Phase Nodes**.

Fluid 1 (pmat1.fluid1)

1 In the **Model Builder** window, click **Fluid 1 (pmat1.fluid1)**.

2 In the **Settings** window for **Fluid**, locate the **Fluid Properties** section.

3 From the **Material** list, choose **Fluid (mat1)**.

FREE AND POROUS MEDIA FLOW (FP)

Porous Medium 1

1 In the **Model Builder** window, under **Component 1 (comp1)> Free and Porous Media Flow (fp)** click **Porous Medium 1**.

2 In the **Settings** window for **Porous Medium**, locate the **Porous Medium** section.

3 From the **Flow model** list, choose **Non-Darcian flow**.

Porous Matrix 1

1 In the **Model Builder** window, expand the **Porous Medium 1** node, then click **Porous Matrix 1**.

2 In the **Settings** window for **Porous Matrix**, locate the **Matrix Properties** section.

3 In the c_F text field, type `fs*Cf`.

Inlet 1

1 In the **Physics** toolbar, click **Boundaries** and choose **Inlet**.

2 Select Boundary 2 only.

3 In the **Settings** window for **Inlet**, locate the **Velocity** section.

4 In the U_0 text field, type v0.

Outlet 1

1 In the **Physics** toolbar, click **Boundaries** and choose **Outlet**.

2 Select Boundary 3 only.

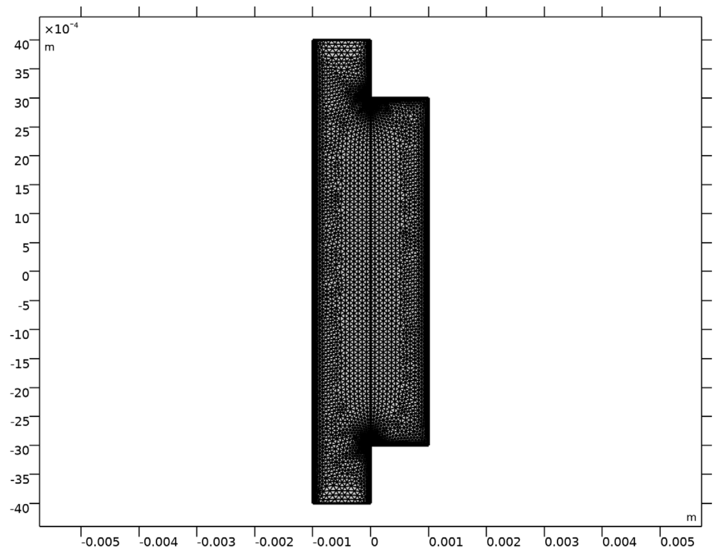
MESH 1

1 In the **Model Builder** window, under **Component 1 (comp1)** click **Mesh 1**.

2 In the **Settings** window for **Mesh**, locate the **Physics-Controlled Mesh** section.

3 From the **Element size** list, choose **Fine**.

4 Click **Build All**.



The physics-controlled mesh automatically generates a boundary layer mesh at the walls where steep velocity gradients are expected.

STUDY 1

Step 1: Stationary

1 In the **Model Builder** window, under **Study 1** click **Step 1: Stationary**.

2 In the **Settings** window for **Stationary**, click to expand the **Study Extensions** section.

3 Select the **Auxiliary sweep** check box.

4 Click **Add**.

5 In the table, enter the following settings:

Parameter name	Parameter value list	Parameter unit
fs (Switch for Forchheimer terms)	0 1	

6 In the **Home** toolbar, click **Compute**.

RESULTS

Velocity (fp)

Visualize the velocity fields as in Figure 3.

1 In the **Settings** window for **2D Plot Group**, locate the **Data** section.

2 From the **Parameter value (fs)** list, choose **0**.

Streamline 1

1 Right-click **Velocity (fp)** and choose **Streamline**.

2 In the **Settings** window for **Streamline**, locate the **Streamline Positioning** section.

3 In the **Number** text field, type `8`.

4 Select Boundary 2 only.

5 Locate the **Coloring and Style** section. Find the **Point style** subsection. From the **Type** list, choose **Arrow**.

6 From the **Arrow distribution** list, choose **Equal time**.

7 From the **Color** list, choose **White**.

Create a plot for the solution including the Forchheimer drag (`fs=1`) next to the plot as follows.

Velocity (fp)

1 In the **Model Builder** window, click **Velocity (fp)**.

2 In the **Settings** window for **2D Plot Group**, click to expand the **Title** section.

3 From the **Title type** list, choose **Manual**.

4 Clear the **Parameter indicator** text field.

5 Click to expand the **Plot Array** section. Select the **Enable** check box.

Streamline 1

1 In the **Model Builder** window, click **Streamline 1**.

2 In the **Settings** window for **Streamline**, click to expand the **Plot Array** section.

3 Select the **Manual indexing** check box.

Streamline 1, Surface

1 In the **Model Builder** window, under **Results>Velocity (fp)**, Ctrl-click to select **Surface** and **Streamline 1**.

2 Right-click and choose **Duplicate**.

Surface 2

1 In the **Settings** window for **Surface**, locate the **Data** section.

2 From the **Dataset** list, choose **Study 1/Solution 1 (sol1)**.

3 Click to expand the **Inherit Style** section. From the **Plot** list, choose **Surface**.

Streamline 2

1 In the **Model Builder** window, click **Streamline 2**.

2 In the **Settings** window for **Streamline**, locate the **Data** section.

3 From the **Dataset** list, choose **Study 1/Solution 1 (sol1)**.

4 Locate the **Plot Array** section. In the **Index** text field, type `1`.

5 Click to expand the **Inherit Style** section. In the **Velocity (fp)** toolbar, click **Plot**.

6 Click the **Zoom Extents** button in the **Graphics** toolbar.

Create the plot from Figure 4.

Cut Line 2D 1

1 In the **Results** toolbar, click **Cut Line 2D**.

2 In the **Settings** window for **Cut Line 2D**, locate the **Line Data** section.

3 In row **Point 1**, set **x** to `-1e3`.

4 In row **Point 2**, set **x** to `1e3`.

Velocity magnitude

1 In the **Results** toolbar, click **1D Plot Group**.

2 In the **Settings** window for **1D Plot Group**, type `Velocity magnitude` in the **Label** text field.

Line Graph 1

1 Right-click **Velocity magnitude** and choose **Line Graph**.

2 In the **Settings** window for **Line Graph**, locate the **Data** section.

3 From the **Dataset** list, choose **Cut Line 2D 1**.

4 In the **Velocity magnitude** toolbar, click **Plot**.

5 Click to expand the **Coloring and Style** section. Find the **Line markers** subsection. From the **Marker** list, choose **Cycle**.

6 Click to expand the **Legends** section. Select the **Show legends** check box.

7 Find the **Prefix and suffix** subsection. Click the button. From the menu, choose **Global definitions>Parameters>fs - Switch for Forchheimer terms**.

8 In the **Prefix** text field, type `fs=`.

9 In the **Velocity magnitude** toolbar, click **Plot**.