

# Geothermal Heating from a Pond Loop

# Introduction

Ponds and lakes can serve as thermal reservoirs in geothermal heating applications. In this example, fluid circulates underwater through polyethylene piping in a closed system. The pipes are coiled in a slinky shape and mounted onto sleds. The Nonisothermal Pipe Flow interface sets up and solves the equations for the temperature and fluid flow in the pipe system, where the geometry is represented by lines in 3D.

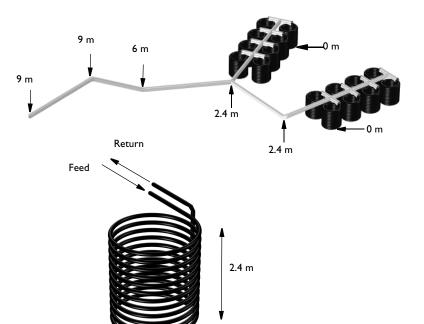


Figure 1: A sled carrying pipe coils shown before the system is submerged.

Model Definition

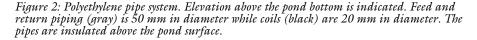
# GEOMETRY

High density polyethylene pipe (20 mm diameter) is rolled into sixteen coils. Groups of eight coils are mounted on two sleds. Each coil has a radius of 1 m and a length of approximately 75 m. The coil groups are connected to feed and return piping with a



diameter of 50 mm (see Figure 2). The coil groups are 2.4 m in height an sit at the bottom of a pond that is 6 m deep. The total length of the piping is 1446 m.

2 m



The heat exchange between pond water and pipe fluid depends on the temperature difference between the two. A slow current in the pond makes the heat transfer more effective than water at rest. The pond is warmer closer to the surface, as shown by the temperature data in Table 1 below.

Elevation (m)	Temperature (K)
0	284
2	288
4	291
6	293

TABLE	1:	POND	TEMPERATURE.

It is easy to set up a function in the software with linear interpolation between points so that the varying pond temperature can be taken into account in the simulation.

# FLOW EQUATIONS

The continuity and momentum equations below describe the stationary flow inside the pipe system:

$$\nabla \cdot (A\rho \mathbf{u}) = 0$$
  
$$0 = -\nabla p - f_{\rm D} \frac{\rho}{2d_{\rm h}} \mathbf{u} |\mathbf{u}| + \mathbf{F}$$
(1)

Above, *A* (SI unit: m<sup>2</sup>) is the cross section area of the pipe,  $\rho$  (SI unit: kg/m<sup>3</sup>) is the density, **u** (SI unit: m/s) is the fluid velocity, and *p* (SI unit: N/m<sup>2</sup>) is the pressure and **F** (SI unit: N/m<sup>3</sup>) is a volume force, like gravity.

Gravity can be included explicitly in the model, but since the variation in density is negligible, and the model is not pressure driven, the only effect of including gravity is a change in the total pressure level. It is therefore common modeling practice to exclude gravity by setting  $\mathbf{F}=0$  and interpret the pressure variable as the reduced pressure  $p_r = p - \rho g(z_0 - z)$ , where  $z_0$  is the datum level of the free liquid surface. This reduces the model complexity and yields the same results.

# Expressions for the Darcy Friction Factor

The right-hand side of Equation 1 describes the pressure drop due to internal viscous shear. The term contains the Darcy friction factor,  $f_D$ , which is a function of the Reynolds number and the surface roughness divided by the hydraulic pipe diameter,  $e/d_h$ . The

Nonisothermal Pipe Flow interface provides a library of built-in expressions for the Darcy friction factor,  $f_{\rm D}$ .

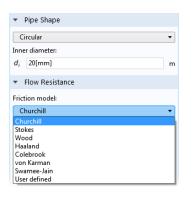


Figure 3: Select from different predefined Friction models in the Pipe Properties node.

This example uses the Churchill relation (Ref. 1) that is valid for laminar flow, turbulent flow, and the transitional region in between. The Churchill relation is:

$$f_{\rm D} = 8 \left[ \left( \frac{8}{\rm Re} \right)^{12} + \left( A + B \right)^{-1.5} \right]^{1/12}$$
(2)

where

$$A = \left[-2.457 \ln\left(\left(\frac{7}{\text{Re}}\right)^{0.9} + 0.27(e/d)\right)\right]^{16}$$
$$B = \left(\frac{37530}{\text{Re}}\right)^{16}$$

As seen from the equations above, the friction factor is a function of the surface roughness divided by diameter of the pipe. Surface roughness data can be selected from a predefined list in the Pipe Properties feature.

The Churchill equation is also a function of the fluid properties, through the Reynolds number:

Re = 
$$\frac{\rho u d}{\mu}$$

The physical properties of water as function of temperature are directly available from the software's built-in material library. Inspection of Equation 2 reveals that for low Reynold's

number (at laminar flow), the friction factor is 64/Re, and for very high Reynolds number, the friction factor is independent of Re.

# HEAT TRANSFER EQUATIONS

The energy equation for the pipeline flow is:

$$\rho A C_p \mathbf{u} \cdot \nabla T = \nabla \cdot A k \nabla T + f_{\mathrm{D}} \frac{\rho}{2d_{\mathrm{h}}} |\mathbf{u}|^3 + Q_{\mathrm{wall}}$$
(3)

where  $C_p$  (SI unit: J/(kg·K)) is the heat capacity at constant pressure, T is the temperature (SI unit: K), and k (SI unit: W/(m·K)) is the thermal conductivity. The second term on the right-hand side of Equation 3 corresponds to friction heat dissipated due viscous shear.  $Q_{wall}$  (SI unit: W/m) is a source/sink term due to heat exchange with the surroundings through the pipe wall:

$$Q_{\text{wall}} = hZ(T_{\text{ext}} - T) \tag{4}$$

Where Z (m) is the wetted perimeter of the pipe, h (W/(m<sup>2</sup>·K)) an overall heat transfer coefficient and  $T_{\text{ext}}$  (K) the external temperature outside of the pipe.

The overall heat transfer coefficient includes contribution from internal film resistance, wall resistance, and external film resistance. For a circular pipe, under assumption that the heat transfer through the wall is quasi static and that the temperature is equal around the circumference of the pipe, an effective hZ in Equation 4 is given by

$$(hZ)_{\rm eff} = \frac{2\pi}{\frac{1}{r_0 h_{\rm int}} + \frac{1}{r_{\rm N} h_{\rm ext}} + \sum_{n=1}^{N} \left(\frac{\ln\left(\frac{r_{\rm n}}{r_{\rm n-1}}\right)}{k_{\rm n}}\right)}$$

where  $r_n$  is the outer radius of wall n,  $h_{int}$  and  $h_{ext}$  are the film heat transfer coefficients on the inside and outside of the tube, and  $k_n$  is the thermal conductivity of wall n.

The film resistance inside the pipe is given by:

$$h_{\text{int}} = \text{Nu}_{\text{int}} \frac{k_{\text{water}}}{d}$$

The internal Nusselt number is taken as 3.66 for the laminar flow regime (Ref. 2), and for the turbulent flow regime the Gnielinski correlation for internal pipe flow is used (Ref. 3):

Nu<sub>int</sub> = 
$$\frac{(f_D/8)(\text{Re} - 1000)\text{Pr}}{1 + \sqrt{12.7}(\text{Pr}^{2/3} - 1)}$$

The external film resistance around the pipe is:

$$h_{\text{ext}} = \text{Nu}_{\text{ext}} \frac{k_{\text{water}}}{d}$$

A slow current is present in the pond. For external forced convection around a pipe, COMSOL uses the Churchill and Bernstein (Ref. 4) relation for Nu, valid for all Re and for Pr > 0.2,:

Nu<sub>ext</sub> = 
$$0.3 + \frac{0.62 \text{Re}^{1/2} \text{Pr}^{1/3}}{[1 + (0.4/\text{Pr})^{2/3}]^{1/4}} [1 + (\text{Re}/282000)^{5/8}]^{4/5}$$

where  $\Pr = C_p \mu / k$ .

Properties of the pipe wall is given in the table below.

TABLE 2: PIPE PROPERTIES.

Name	Value	Description
d <sub>wall</sub>	2 mm	Pipe wall thickness
k <sub>wall</sub>	0.46 W/(m·K)	Pipe wall thermal conductivity

# Results and Discussion

Figure 4 shows the pressure (Pa) in the 1446 m pipe system assuming that water enters the system at a rate of 4 l/s.

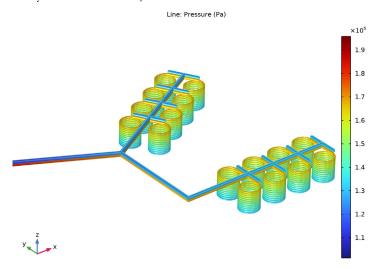


Figure 4: Pressure drop over the pipe system.

Line: Temperature (degC)

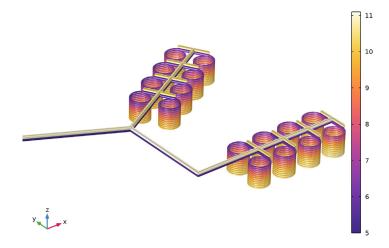


Figure 5: Temperature of the pipe fluid.

The plot below shows the temperature (K) distribution for the pipe fluid. It enters the pipe system at 5  $^{\circ}$ C and exits with a temperature of approximately 11  $^{\circ}$ C.

Turbulent flow conditions in the loop are important for good heat exchange between the pipes and the surroundings. A plot of the Reynolds number is shown in Figure 6, confirming that flow is turbulent (Re > 3000) throughout the system.

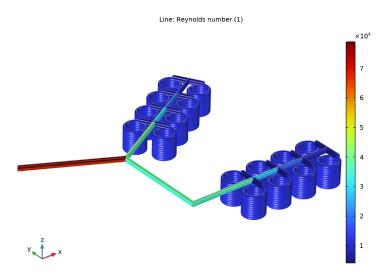


Figure 6: The Reynolds number in the pipe loop confirms that the flow conditions are turbulent.

**Note:** This model is also available in an extended version in the *Introduction to Pipe Flow Module* booklet.

# References

1. S.W. Churchill, "Friction factor equation spans all fluid-flow regimes," *Chem. Eng.*, vol. 84, no. 24, p. 91, 1997.

2. F.P. Incropera and D.P. DeWitt, *Fundamentals of Heat and Mass Transfer*, 4th ed., John Wiley & Sons, 1996. Eq 8.62 and Eq 9.34, respectively.

3. V. Gnielinski, "New Equation for Heat and Mass Transfer in Turbulent Pipe and Channel Flow," *Int. Chem. Eng.*, vol. 16, pp. 359–368, 1976.

4. S.W. Churchill and M. Bernstein, "A Correlating Equation for Forced Convection from Gases and Liquids to a Circular Cylinder in Crossflow," *J Heat Transfer*, vol. 99, p. 300, 1977.

**Application Library path:** Pipe\_Flow\_Module/Heat\_Transfer/ geothermal\_heating

# Modeling Instructions

From the File menu, choose New.

#### NEW

In the New window, click 🙆 Model Wizard.

# MODEL WIZARD

- I In the Model Wizard window, click 间 3D.
- 2 In the Select Physics tree, select Fluid Flow>Nonisothermal Flow> Nonisothermal Pipe Flow (nipfl).
- 3 Click Add.
- 4 Click 🔿 Study.
- 5 In the Select Study tree, select General Studies>Stationary.
- 6 Click M Done.

#### GEOMETRY I

Start by creating the piping system geometry. You can simplify this by inserting a prepared geometry sequence from file:

- I In the Geometry toolbar, click Insert Sequence and choose Insert Sequence.
- 2 Browse to the model's Application Libraries folder and double-click the file geothermal\_heating\_geom\_sequence.mph.
- 3 In the Geometry toolbar, click 🟢 Build All.

The complete instructions for creating this geometry can be found in the appendix at the end of this document.

#### DEFINITIONS

Now add some external data in the form of interpolation tables and variables.

Interpolation 1 (int1)

- I In the Home toolbar, click f(X) Functions and choose Local>Interpolation.
- 2 In the Settings window for Interpolation, locate the Definition section.
- **3** In the table, enter the following settings:

t	f(t)
0	284
2	288
4	291
6	293

4 Locate the Units section. In the Argument table, enter the following settings:

Argument	Unit
t	m

5 In the Function table, enter the following settings:

Function	Unit
intl	К

#### Variables I

- I In the Home toolbar, click a = Variables and choose Local Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- 3 Click 📂 Load from File.
- **4** Browse to the model's Application Libraries folder and double-click the file geothermal\_heating\_variables.txt.

#### ADD MATERIAL

- I In the Home toolbar, click 🙀 Add Material to open the Add Material window.
- 2 Go to the Add Material window.
- 3 In the tree, select Built-in>Water, liquid.
- 4 Click Add to Component in the window toolbar.
- 5 In the Home toolbar, click 🙀 Add Material to close the Add Material window.

#### NONISOTHERMAL PIPE FLOW (NIPFL)

#### Pipe Properties 1

- I In the Model Builder window, under Component I (compl)> Nonisothermal Pipe Flow (nipfl) click Pipe Properties I.
- 2 In the Settings window for Pipe Properties, locate the Pipe Shape section.
- 3 From the list, choose Circular.
- **4** In the  $d_i$  text field, type 20[mm].

#### Temperature 1

- I In the Model Builder window, click Temperature I.
- 2 In the Settings window for Temperature, locate the Temperature section.
- **3** In the  $T_{in}$  text field, type 5[degC].

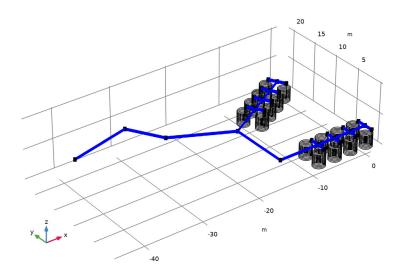
#### Pipe Properties 2

- I In the Physics toolbar, click 🔚 Edges and choose Pipe Properties.
- **2** Select Edges 1–12, 15, 17–21, 27–29, 33–35, 39, 41–45, 51–53, 57–59, 63, 65–69, 75–77, 81–83, 87, 89–91, 97, 98, 102, and 103 only.

To make the selection easily, first click **Go to XZ View** and then click **Select Box**. In the **Graphics** window, draw a box around the pipes to select them. Click the **Go to Default View** button. Alternatively, copy the entity numbers from the text, click in the selection box, and then press Ctrl+V.

- 3 In the Settings window for Pipe Properties, locate the Pipe Shape section.
- 4 From the list, choose Circular.
- **5** In the  $d_i$  text field, type 50[mm].

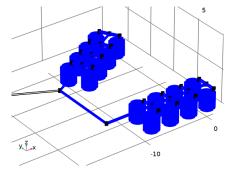
6 Click the **Zoom to Selection** button in the **Graphics** toolbar.



# Wall Heat Transfer 1

- I In the Physics toolbar, click 📄 Edges and choose Wall Heat Transfer.
- **2** Select Edges 7–104 only.

Use the same rubber band technique as in the previous selection step.



- 3 In the Model Builder window, click Wall Heat Transfer I.
- 4 In the Settings window for Wall Heat Transfer, locate the Heat Transfer Model section.
- **5** In the  $T_{ext}$  text field, type T\_pond.

# Internal Film Resistance 1

In the Physics toolbar, click 层 Attributes and choose Internal Film Resistance.

#### Wall Heat Transfer 1

In the Model Builder window, click Wall Heat Transfer I.

#### Wall Layer 1

- I In the Physics toolbar, click 🦳 Attributes and choose Wall Layer.
- 2 In the Settings window for Wall Layer, locate the Specification section.
- **3** From the *k* list, choose **User defined**.
- **4** In the text field, type k\_wall.
- **5** From the  $\Delta w$  list, choose **User defined**.
- **6** In the text field, type d\_wall.

#### Wall Heat Transfer 1

In the Model Builder window, click Wall Heat Transfer I.

External Film Resistance 1

I In the Physics toolbar, click 📃 Attributes and choose External Film Resistance.

The external slow flow of 0.2 m/s is the mild current in the pond. This is enough to consider it forced convection outside the tubes.

- 2 In the Settings window for External Film Resistance, locate the Specification section.
- 3 From the Surrounding fluid list, choose Water, liquid (matl).
- 4 In the  $u_{ext}$  text field, type 0.2[m/s].

#### Inlet 1

- I In the Physics toolbar, click 🗁 Points and choose Inlet.
- 2 Select Point 1 only.
- 3 In the Settings window for Inlet, locate the Inlet Specification section.
- 4 From the Specification list, choose Volumetric flow rate.
- **5** In the  $q_{v,0}$  text field, type 4[1/s].

# Heat Outflow I

- I In the Physics toolbar, click 📄 Points and choose Heat Outflow.
- 2 Select Point 2 only.

# MESH I

- I In the Model Builder window, under Component I (compl) click Mesh I.
- 2 In the Settings window for Mesh, locate the Physics-Controlled Mesh section.
- 3 From the Element size list, choose Extremely fine.

- 4 Click 📗 Build All.
- **5** Click the **J Go to Default View** button in the **Graphics** toolbar.

# STUDY I

In the **Home** toolbar, click = **Compute**.

#### RESULTS

## Pressure (nipfl)

Default plot groups show the pressure (Figure 4), velocity, and temperature (Figure 5) in the pipe system. To get a better view, do as follows:

I Click the **Zoom Box** button in the **Graphics** toolbar. Draw a box in the **Graphics** window to zoom in on the coils.

#### DEFINITIONS

View I

- I In the Model Builder window, under Component I (compl)>Definitions click View I.
- 2 In the Settings window for View, locate the View section.
- **3** Clear the **Show grid** check box.

# RESULTS

Temperature (nipfl)

The following instructions reproduce the plot on Figure 5.

Line 1

- I In the Model Builder window, expand the Temperature (nipfl) node, then click Line I.
- 2 In the Settings window for Line, locate the Expression section.
- 3 From the Unit list, choose degC.
- **4** In the **Temperature (nipfl)** toolbar, click **I** Plot.

Reproduce the Reynolds' number plot in Figure 6 with the following steps.

# Reynolds' number

- I In the Home toolbar, click 🚛 Add Plot Group and choose 3D Plot Group.
- 2 In the Settings window for 3D Plot Group, type Reynolds' number in the Label text field.

Line 1

- I Right-click **Reynolds' number** and choose Line.
- In the Settings window for Line, click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component I (compl)>
  Nonisothermal Pipe Flow>nipfl.Re Reynolds number.
- 3 Locate the Coloring and Style section. From the Line type list, choose Tube.
- **4** In the **Reynolds' number** toolbar, click **I** Plot.

# CREATING THE GEOMETRY

The previously inserted geometry can be created from scratch like this:

#### ADD COMPONENT

In the **Home** toolbar, click  $\bigotimes$  **Add Component** and choose **3D**.

# GEOMETRY I

Parametric Curve I (pcI)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Parametric Curve.
- 2 In the Settings window for Parametric Curve, locate the Parameter section.
- 3 In the Maximum text field, type 24.
- 4 Locate the **Expressions** section. In the **x** text field, type cos(pi\*s).
- 5 In the y text field, type sin(pi\*s).
- 6 In the z text field, type 0.1\*s.
- 7 Click 틤 Build Selected.

#### Polygon I (poll)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- 3 In the table, enter the following settings:

x (m)	y (m)	z (m)
1	0	0
1.1	0	0
1.1	0	2.6
1.1	1.5	2.6

4 Click 📄 Build Selected.

#### Polygon 2 (pol2)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- **3** In the table, enter the following settings:

x (m)	y (m)	z (m)
1	0	2.4
1	1.5	2.4

#### 4 Click 틤 Build Selected.

Mirror I (mirl)

- I In the Geometry toolbar, click 💭 Transforms and choose Mirror.
- 2 Click in the Graphics window and then press Ctrl+A to select all objects.
- 3 In the Settings window for Mirror, locate the Point on Plane of Reflection section.
- 4 In the y text field, type 1.5.
- 5 Locate the Normal Vector to Plane of Reflection section. In the y text field, type 1.
- 6 In the z text field, type 0.
- 7 Locate the Input section. Select the Keep input objects check box.
- 8 Click 🔚 Build Selected.

#### Array I (arr I)

- I In the Geometry toolbar, click 💭 Transforms and choose Array.
- 2 Click in the Graphics window and then press Ctrl+A to select all objects.
- 3 In the Settings window for Array, locate the Size section.
- **4** In the **x size** text field, type 4.
- 5 Locate the Displacement section. In the x text field, type -3.
- 6 Click 📄 Build Selected.

#### Polygon 3 (pol3)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- **3** In the table, enter the following settings:

x (m)	y (m)	z (m)	
1	1.5	2.4	
- 15	1.5	2.4	

# 4 Click 틤 Build Selected.

Polygon 4 (pol4)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.

3 In the table, enter the following settings:

x (m)	y (m)	z (m)
1.1	1.5	2.6
- 15	1.5	2.6

4 Click 틤 Build Selected.

Array 2 (arr2)

- I In the Geometry toolbar, click 💭 Transforms and choose Array.
- 2 Click in the Graphics window and then press Ctrl+A to select all objects.
- 3 In the Settings window for Array, locate the Size section.
- 4 In the y size text field, type 2.
- 5 Locate the **Displacement** section. In the **y** text field, type 10.
- 6 Click 틤 Build Selected.

Polygon 5 (pol5)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- **3** In the table, enter the following settings:

x (m)	y (m)	z (m)	
<b>x (m)</b> -15	1.5	2.4	
- 15 - 28 - 35 - 45	11.5	2.4	
-28	11.5	6	
-35	11.5	10	
- 45	9	10	

# 4 Click 틤 Build Selected.

Polygon 6 (pol6)

- I In the Geometry toolbar, click  $\bigoplus$  More Primitives and choose Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.

**3** In the table, enter the following settings:

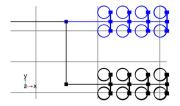
x (m)	y (m)	z (m)	
-15	1.5	2.6	
- 15	11.5	2.6	
-28	11.5	6.2	
x (m) -15 -15 -28 -35 -45	11.5	10.2	
- 45	9	10.2	

4 Click 틤 Build Selected.

**5** Click the  $\leftarrow$  **Zoom Extents** button in the **Graphics** toolbar.

Rotate I (rot I)

- I In the Geometry toolbar, click 📿 Transforms and choose Rotate.
- 2 Click the **Context** Go to XY View button in the Graphics toolbar.



- 3 In the Settings window for Rotate, locate the Rotation section.
- 4 In the Angle text field, type 30.
- 5 Locate the Point on Axis of Rotation section. In the x text field, type 15.
- 6 In the y text field, type 11.5.
- 7 Click 틤 Build Selected.
- 8 Click the  $\sqrt[1]{}$  Go to Default View button in the Graphics toolbar.