



# Nonisothermal Laminar Flow in a Circular Tube

## Introduction

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This validation model of laminar airflow through a tube validates the heat transfer coefficient obtained from the simulation against Nusselt-number-based correlation functions. The simulation results are in good agreement with experimental measurements.

## Model Definition

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The tube is modeled as a 2D axisymmetric geometry. The tube has a diameter of 0.05 m and a length of 3 m. A coupled heat transfer and fluid flow problem is solved using the Nonisothermal Flow interface.

At the inlet, a laminar velocity profile  $U$  with an average velocity  $U_{av}$  of 0.1 m/s is applied using the normal inflow option:

$$U = 1.5U_{av}\left(1 - 4\left(\frac{r}{b}\right)^2\right)$$

where  $r$  denotes the radial distance from the tube center and  $b$  the tube's diameter. The expression gives the typical parabolic velocity profile for fully developed laminar flow. The air enters with a temperature  $T_0$  of 283 K.

At the cylinder wall, a constant heat flux  $q_w$  of 10 W/m<sup>2</sup> is applied.

### NUSSELT NUMBER CORRELATIONS

Two different Nusselt number correlations are used to validate the numerical results.

First, in regions with fully developed laminar flow with a radial temperature profile, a constant Nusselt number  $Nu_c$  can be defined as follows:

$$Nu_c = \frac{hD_h}{k}$$

where  $k$  (SI unit: W/(m·K)) denotes the thermal conductivity,  $D_h$  (SI unit: m) the hydraulic diameter, and  $h$  (SI unit: W/(m<sup>2</sup>·K)) the heat transfer coefficient. In the case of a tube with uniform surface heat flux,  $Nu = 4.36$  (Ref. 1, p. 507).

Alternatively, a local Nusselt number  $Nu_l$  can be defined, based on the  $z$ -position along the cylinder, to describe both the entrance and fully developed regions of the flow (Ref. 2, p. 304):

$$\frac{Nu_l}{4.364 \left[ 1 + \left( \frac{Gz}{29.6} \right)^2 \right]^{1/6}} = \left[ 1 + \left( \frac{Gz/19.04}{\left[ 1 + \left( \frac{Pr}{0.0207} \right)^{2/3} \right]^{1/2} \left[ 1 + \left( \frac{Gz}{29.6} \right)^2 \right]^{1/3}} \right)^{3/2} \right]^{1/3}$$

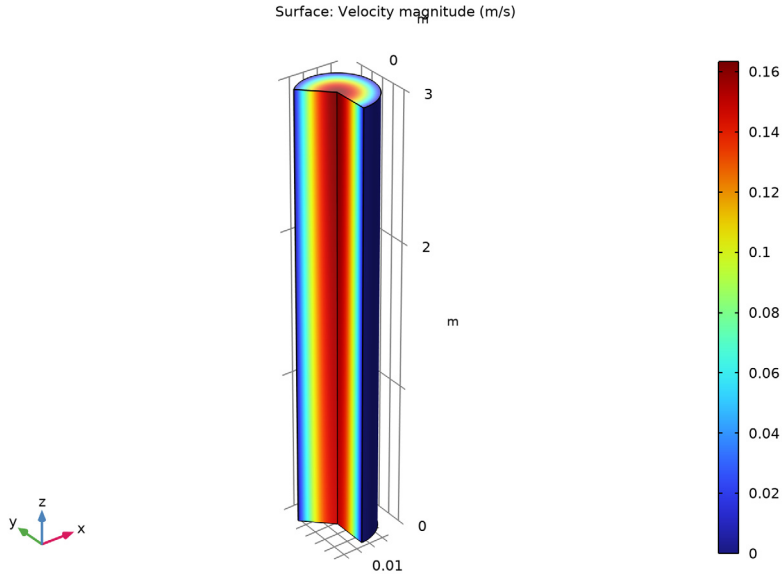
where  $Pr$  is the Prandtl number, and the Graetz number  $Gz$  is defined by:

$$Gz = \frac{\pi}{4} \cdot \frac{Re_b \cdot Pr \cdot b}{z}$$

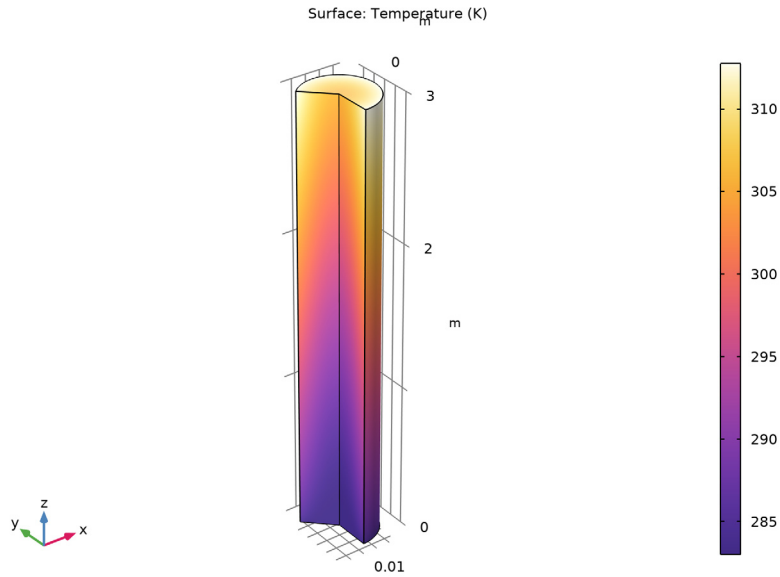
with  $Re_b$  the Reynolds number associated to the tube diameter  $b$ .

## Results and Discussion

The velocity field is shown in [Figure 1](#) and the temperature field in [Figure 2](#). Both are plotted in a scaled view to get a clearer visualization of the results.



*Figure 1: Velocity field.*



*Figure 2: Temperature field.*

The comparison of the computed heat transfer coefficient with the Nusselt number correlations shows that the Local Nusselt number provides a good approximation over the whole cylinder. On the other hand, constant Nusselt number represents the region where velocity and temperature profile are fully developed ([Figure 3](#)).

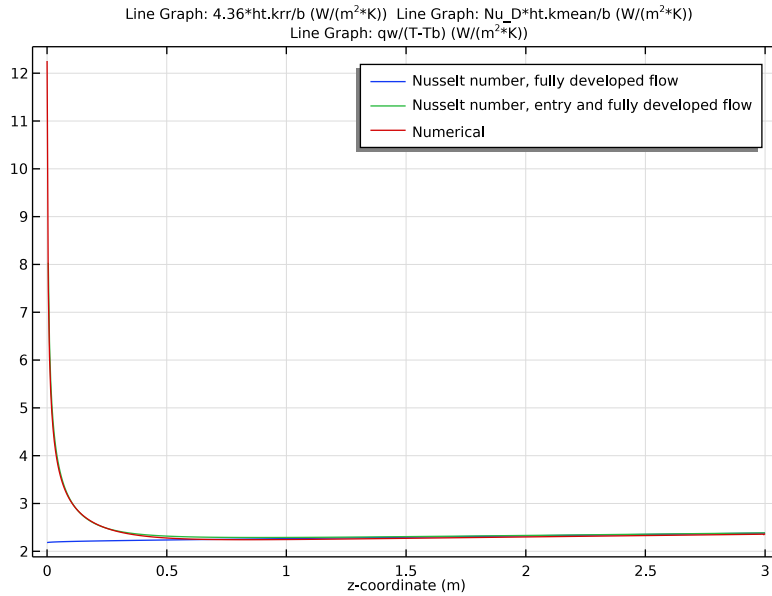


Figure 3: Comparison of the computed heat transfer coefficient with the heat transfer coefficient estimation based on Nusselt number correlations.

## References


1. F.P. Incropera, D.P. DeWitt, T.L. Bergman, and A.S. Lavine, *Fundamentals of Heat and Mass Transfer*, 6th Edition, John Wiley & Sons, 2006.
2. A. Bejan et al., *Heat Transfer Handbook*, John Wiley & Sons, 2003.

**Application Library path:** Heat\_Transfer\_Module/Verification\_Examples/  
circular\_tube\_nitf\_laminar




## Modeling Instructions

From the **File** menu, choose **New**.

## NEW

In the **New** window, click  **Model Wizard**.

## MODEL WIZARD

- 1 In the **Model Wizard** window, click  **2D Axisymmetric**.
- 2 In the **Select Physics** tree, select **Fluid Flow>Nonisothermal Flow>Laminar Flow**.
- 3 Click **Add**.
- 4 Click  **Study**.
- 5 In the **Select Study** tree, select **General Studies>Stationary**.
- 6 Click  **Done**.

## GLOBAL DEFINITIONS

### *Parameters I*

- 1 In the **Model Builder** window, under **Global Definitions** click **Parameters I**.
- 2 In the **Settings** window for **Parameters**, locate the **Parameters** section.
- 3 In the table, enter the following settings:

Name	Expression	Value	Description
L	3[m]	3 m	Length
b	0.05[m]	0.05 m	Height
T0	283[K]	283 K	Inlet temperature
U_av	0.1[m/s]	0.1 m/s	Average inlet velocity
qw	10[W/m^2]	10 W/m <sup>2</sup>	Wall heat flux
Tw	293[K]	293 K	Wall temperature

## DEFINITIONS

### *Variables I*

Define several variables: A variable for the inlet velocity profile, a variable for the bulk temperature which is a radial weighted temperature, and similarly a variable for the bulk velocity. Finally, add variables to compare the simulation results with the literature values.



- 1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Definitions** and choose **Variables**.
- 2 In the **Settings** window for **Variables**, locate the **Variables** section.

3 In the table, enter the following settings:



Name	Expression	Unit	Description
U	$1.5*U_{av}*(1-4*(r/b)^2)$	m/s	Inlet velocity
Tb	$\text{integrate}(\text{comp1.at2}(r,z,2*\pi*r*w*T),r,0,b/2)/\text{integrate}(\text{comp1.at2}(r,z,2*\pi*r*w),r,0,b/2)$	K	Bulk temperature
Ub	$\text{integrate}(\text{comp1.at2}(r,z,2*\pi*r*w),r,0,b/2)/(pi*(b/2)^2)$	m/s	Bulk velocity
Tc	$\text{comp1.at2}(0,z,T)$	K	Center line temperature
Pr	$ht.Cp*spf.mu/ht.kmean$		Prandtl number
Re_D	$nitf1.rho*Ub*b/spf.mu$		Reynolds number
Gz	$b*Re\_D*Pr/z*pi/4$		Graetz number
Nu_D	$(1+(Gz/19.04/((1+(Pr/0.0207)^2/3)^{1/2}*(1+(Gz/29.6)^2)^{1/3}))^{3/2}))^{1/3}*4.364*(1+(Gz/29.6)^2)^{1/6}$		Local Nusselt number

## GEOMETRY I

*Rectangle I (rI)*

- 1 In the **Geometry** toolbar, click  **Rectangle**.
- 2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.
- 3 In the **Width** text field, type  $b/2$ .
- 4 In the **Height** text field, type  $L$ .
- 5 Click  **Build All Objects**.

## ADD MATERIAL

- 1 In the **Home** toolbar, click  **Add Material** to open the **Add Material** window.
- 2 Go to the **Add Material** window.
- 3 In the tree, select **Built-in>Air**.
- 4 Click **Add to Component** in the window toolbar.
- 5 In the **Home** toolbar, click  **Add Material** to close the **Add Material** window.

## LAMINAR FLOW (SPF)

### *Inlet I*

- 1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Laminar Flow (spf)** and choose **Inlet**.
- 2 Select Boundary 2 only.
- 3 In the **Settings** window for **Inlet**, locate the **Velocity** section.
- 4 In the  $U_0$  text field, type U.


### *Outlet I*

- 1 In the **Physics** toolbar, click  **Boundaries** and choose **Outlet**.
- 2 Select Boundary 3 only.

## HEAT TRANSFER IN FLUIDS (HT)

In the **Model Builder** window, under **Component 1 (comp1)** click **Heat Transfer in Fluids (ht)**.


### *Inflow I*

- 1 In the **Physics** toolbar, click  **Boundaries** and choose **Inflow**.
- 2 Select Boundary 2 only.
- 3 In the **Settings** window for **Inflow**, locate the **Upstream Properties** section.
- 4 In the  $T_{\text{ustr}}$  text field, type T0.

### *Outflow I*


- 1 In the **Physics** toolbar, click  **Boundaries** and choose **Outflow**.
- 2 Select Boundary 3 only.

### *Heat Flux I*

- 1 In the **Physics** toolbar, click  **Boundaries** and choose **Heat Flux**.
- 2 Select Boundary 4 only.
- 3 In the **Settings** window for **Heat Flux**, locate the **Heat Flux** section.
- 4 In the  $q_0$  text field, type qw.

## MESH I

### *Mapped I*

In the **Mesh** toolbar, click  **Mapped**.



### *Distribution I*

- 1 Right-click **Mapped I** and choose **Distribution**.




- 2 Select Boundary 4 only.
- 3 In the **Settings** window for **Distribution**, locate the **Distribution** section.
- 4 In the **Number of elements** text field, type 600.

#### *Distribution 2*

- 1 In the **Model Builder** window, right-click **Mapped 1** and choose **Distribution**.
- 2 Click the  **Zoom Extents** button in the **Graphics** toolbar.
- 3 Select Boundaries 2 and 3 only.
- 4 In the **Settings** window for **Distribution**, locate the **Distribution** section.
- 5 From the **Distribution type** list, choose **Predefined**.
- 6 In the **Number of elements** text field, type 33.
- 7 In the **Element ratio** text field, type 5.
- 8 Click  **Build All**.

#### **STUDY 1**

In the **Home** toolbar, click  **Compute**.

#### **RESULTS**



##### *Velocity, 3D (spf)*

For better visualization of the results, use a scaled the view.


##### *View 3D 2*

In the **Model Builder** window, expand the **Results>Views** node.

##### *Camera*

- 1 In the **Model Builder** window, expand the **View 3D 2** node, then click **Camera**.
- 2 In the **Settings** window for **Camera**, locate the **Camera** section.
- 3 From the **View scale** list, choose **Manual**.
- 4 In the **z scale** text field, type 0.1.
- 5 Click  **Update**.
- 6 Click the  **Zoom Extents** button in the **Graphics** toolbar.

##### *Velocity, 3D (spf)*

Click the  **Zoom Extents** button in the **Graphics** toolbar.

##### *Heat transfer coefficient*

- 1 In the **Home** toolbar, click  **Add Plot Group** and choose **ID Plot Group**.

- 2 In the **Settings** window for **ID Plot Group**, type Heat transfer coefficient in the **Label** text field.

*Line Graph 1*

- 1 Right-click **Heat transfer coefficient** and choose **Line Graph**.
- 2 Select Boundary 4 only.
- 3 In the **Settings** window for **Line Graph**, locate the **y-Axis Data** section.
- 4 In the **Expression** text field, type  $4.36 \cdot h_t \cdot k_{rr} / b$ .
- 5 Locate the **x-Axis Data** section. From the **Parameter** list, choose **Expression**.
- 6 In the **Expression** text field, type  $z$ .
- 7 Click to expand the **Legends** section. Select the **Show legends** check box.
- 8 From the **Legends** list, choose **Manual**.
- 9 In the table, enter the following settings:

Legends
Nusselt number, fully developed flow

*Line Graph 2*

- 1 In the **Model Builder** window, right-click **Heat transfer coefficient** and choose **Line Graph**.
- 2 Select Boundary 4 only.
- 3 In the **Settings** window for **Line Graph**, locate the **y-Axis Data** section.
- 4 In the **Expression** text field, type  $Nu_D \cdot h_t \cdot k_{mean} / b$ .
- 5 Locate the **x-Axis Data** section. From the **Parameter** list, choose **Expression**.
- 6 In the **Expression** text field, type  $z$ .
- 7 Locate the **Legends** section. Select the **Show legends** check box.
- 8 From the **Legends** list, choose **Manual**.
- 9 In the table, enter the following settings:

Legends
Nusselt number, entry and fully developed flow


*Line Graph 3*

- 1 Right-click **Heat transfer coefficient** and choose **Line Graph**.
- 2 Select Boundary 4 only.
- 3 In the **Settings** window for **Line Graph**, locate the **y-Axis Data** section.

- 4 In the **Expression** text field, type  $qw/(T-T_b)$ .
- 5 Locate the **x-Axis Data** section. From the **Parameter** list, choose **Expression**.
- 6 In the **Expression** text field, type  $z$ .
- 7 Locate the **Legends** section. Select the **Show legends** check box.
- 8 From the **Legends** list, choose **Manual**.
- 9 In the table, enter the following settings:

Legends
Numerical

*Heat transfer coefficient*

- 1 In the **Model Builder** window, click **Heat transfer coefficient**.
- 2 In the **Heat transfer coefficient** toolbar, click  **Plot**.

