

Supersonic Air-to-Air Ejector

Introduction

This application models compressible turbulent gas flow in a supersonic air ejector using the High Mach Number Flow interface in COMSOL Multiphysics. Ejectors are simple mechanical components used to induce a secondary flow by momentum and energy transfer from a high-velocity primary jet. The high-energy fluid (primary flow) passes through a convergent-divergent nozzle and reaches supersonic conditions. After exiting the nozzle, it interacts with the secondary flow which is accelerated through an entrainment-induced effect. The mixing between both flows takes place along a constantarea duct called the mixing chamber where complex interactions between the mixing layer and shocks can be observed. A diffuser is usually placed before the outlet to recover pressure and bring the flow back to stagnation.

Ejectors are used for a wide range of applications, including industrial refrigeration, vacuum generation, gas recirculation, and thrust augmentation in aircraft propulsion systems. Great efforts have been made to determine their optimum design and operating conditions, as well as how to describe the flow within them (Ref. 1).

This application models an ejector working with air in both the primary and secondary streams. The geometry and boundary conditions are based on Ref. 2, and Ref. 3. The items of interest are the primary and secondary mass flows, the static pressure distribution along the centerline of the ejector, and the resolution of the flow in the mixing region.

Model Definition

Figure 1 shows the geometry of the ejector. Its dimensions can be found in Table 1. A two-dimensional axisymmetric geometry is used to approximate the 3D geometry of the device and to reduce the size of the problem.

The flow velocity in the ejector is large enough to introduce significant variations in the density and temperature of the fluid, and the flow is governed by the fully compressible Navier-Stokes equations. Moreover, the Mach number is expected to be larger than one in the divergent section of the primary nozzle, as well as in the mixing chamber. Interaction between the boundary layers and mixing layers cause the deceleration from supersonic to subsonic flow to take place through a complex succession of shocks called

shock train or pseudo-shock wave phenomenon (Ref. 4). Thus, the mesh has to be fine enough to accurately capture this phenomenon.



Figure 1: The geometry of the ejector.

TABLE I:	DIMENSIONS	OF THE	EJECTOR	IN	MM.
			-,		

dı	d ₂	d _t	d _{nd}	d _m	d _d
16	160	8	12	24	51
L	L ₂	L ₃	L _m	L _d	NXP
7	23	90	240	70	15

The problem is modeled using the Favre-averaged Navier-Stokes equations and the standard k- ε turbulence model.

Both primary and secondary flows are air with a specific gas constant of 287 J/(kg·K) and a ratio of specific heats of 1.4. The dynamic viscosity and thermal conductivity of the air are computed from Sutherland's law.

BOUNDARY CONDITIONS

Inlet

The flow at the inlets is specified in terms of its total properties: $T_0 = 300$ K and $P_0 = 5$ atm for the primary flow, and $T_0 = 300$ K and $P_0 = 0.55$ atm for the secondary flow.

The inlet conditions are applied using an Inlet feature, where the Flow condition is specified to be **Characteristics based**. This provides a numerically consistent boundary condition by evaluating the flow characteristics at the inlet.

The velocities at both inlets are unknown. However, they are expected to be very small compared to the velocities inside the nozzle and mixing chamber. The values that must be prescribed at the inlet are the total values of temperature and pressure, which define the energy of the flow. The Mach number can be set to 0 and will be determined by the characteristics based boundary condition at the inlet. This provides a good initial solution, but the total values of pressure and temperature may differ slightly. The solution can be improved if the problem is solved again setting the Mach number to the values computed by the characteristics based boundary condition at the inlets, which are approximately 0.14 and 0.01 for the primary and secondary inlets, respectively.

The inlet values for the turbulent kinetic energy, k, and the turbulent dissipation rate, ε , are approximated from the turbulent intensity, $I_{\rm T}$, and turbulence length scale, $L_{\rm T}$. Turbulent intensity is set by default to 0.05 (5%). The length scale can be approximated as 7% of the pipe diameter or hydraulic diameter. This is done automatically when Turbulence length scale is set to Geometry based.

For more background on this boundary condition, see the CFD Module User's Guide.

Outlet

The flow reaches supersonic conditions inside the ejector. However, it is expanded and decelerated along the mixing chamber and the diffuser, reaching subsonic conditions before being discharged into the atmosphere. The outlet is then subsonic with atmospheric static pressure. This is modeled using an Outlet node with the **Flow condition** set to subsonic.

Results and Discussion

The mass flows obtained are depicted in Table 2. The distributions of Mach number and velocity inside the ejector are depicted in Figure 2 and Figure 3. The primary flow is accelerated in the convergent section of the nozzle, reaching sonic conditions at the throat, and is expanded further in the divergent section. At the outlet of the primary nozzle, the secondary flow acts as an artificial wall for the primary flow. This leads to the formation of virtual nozzle throats, and a succession of expansion and compression waves can be observed in the region upstream of the mixing zone. Then, the flow decelerates along the constant-area duct and is brought back to stagnation in the diffuser. The region where both flows mix can be visualized by plotting the turbulent kinetic energy, see Figure 4.

Figure 5 plots the distribution of pressure along the centerline and walls of the mixing chamber. At the centerline of the duct, the flow successively changes from supersonic to subsonic flow via multiple shocks. However, this cannot be detected by wall pressure

measurements because the surface pressures tend to be smeared out due to the dissipation in the boundary layer (see Ref. 4). The distribution of temperature is shown in Figure 6. Very low temperatures can be observed inside the device. This must be taken into account when designing an ejector, specially when working with two-phase flows. The results obtained correlate well with Ref. 2 and Ref. 3.

TABLE	2:	MASS	FLOWS
IT OLL	÷.	117 (00	1 20 11 3

\dot{m}_1	\dot{m}_2	m _{mixed}
0.057 kg/s	0.036 kg/s	0.093 kg/s



Figure 2: Mach number distribution.



Figure 3: The distribution of velocity in the nozzle and the mixing chamber.



Figure 4: The distribution of turbulent kinetic energy. The mixing region is clearly identified.

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Figure 5: The distribution of pressure along the mixing chamber.



Figure 6: The distribution of temperature. Very low temperatures can be observed at the outlet of the nozzle. The temperature at the outlet of the ejector is lower than at both inlets.

The present application is highly nonlinear and sensitive to the solution procedure. The mesh needed to capture the interaction between the shocks and the mixing layer, and to resolve the solution near the walls, is extremely fine. However, convergence may be hard to achieve with such a fine mesh unless a good enough initial solution is used. A way to overcome this is to first solve the problem on a coarse mesh and then refine it. The solution on the coarse mesh provides good initial values, but lacks accuracy in three important areas: wall resolution, capture of shocks, and resolution of the mixing layer. The adaptive mesh refinement feature can be used to overcome this. However, in order to fully resolve the mesh, a high element growth rate would be needed, potentially leading to convergence problems. An alternative option is to first refine manually both on the boundary layers and in the nozzle, and then to use the adaptive mesh refinement feature to resolve the mixing layer.

References

1. S. He, Y. Li, and R.Z. Wang, "Progress of Mathematical Modeling on Ejectors," *Renew. Sustain. Energy Rev.*, vol. 13, pp 1760–1780, 2009.

2. Y. Bartosiewicz, Zine Aidoun, P. Desevaux, and Yves Mercadier, "Numerical and Experimental Investigations on Supersonic Ejectors," *Int. J. of Heat and Fluid Flow*, vol. 26, pp 56–70, 2005.

3. P. Desevaux, A. Bouhangel, and E. Gavignet, "Flow Visualization in Supersonic Ejectors Using Laser Tomography Techniques," *Int. J. of Refrigeration*, vol. 34, pp 1633–1640, 2010.

4. F. Gnani, H. Zare-Behtash, and K. Kontis, "Pseudo-shock Waves and their Interactions in High-speed Intakes," *Progress in Aerospace Sciences*, vol. 82, pp 36–56, 2016.

Application Library path: CFD_Module/High_Mach_Number_Flow/ supersonic_ejector

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click 🚳 Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click 🚈 2D Axisymmetric.
- 2 In the Select Physics tree, select Fluid Flow>High Mach Number Flow>Turbulent Flow> High Mach Number Flow, k-ε (hmnf).
- 3 Click Add.
- 4 Click \bigcirc Study.
- 5 In the Select Study tree, select General Studies>Stationary.
- 6 Click **M** Done.

GEOMETRY I

The model geometry is available as a parameterized geometry sequence in a separate MPH-file.

- I In the Geometry toolbar, click Insert Sequence and choose Insert Sequence.
- 2 Browse to the model's Application Libraries folder and double-click the file supersonic_ejector_geom_sequence.mph.
- 3 In the Geometry toolbar, click 📗 Build All.

GLOBAL DEFINITIONS

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.

Name	Expression	Value	Description
P1	5[atm]	5.0663E5 Pa	Total pressure, primary flow
P2	0.55[atm]	55729 Pa	Total pressure, secondary flow
Pout	1[atm]	1.0133E5 Pa	Pressure, outlet
Τ1	300[K]	300 K	Total temperature, primary flow
T2	Т1	300 K	Total temperature, secondary flow
Rs	287[J/kg/K]	287 J/(kg·K)	Specific gas constant
gamma	1.41	1.41	Ratio of specific heats
iso_diff	0	0	Isotropic diffusion

3 In the table, enter the following settings:

Add isotropic diffusion to improve convergence when computing the initial solution with a coarse mesh.

- 4 Click the 🐱 Show More Options button in the Model Builder toolbar.
- 5 In the Show More Options dialog box, in the tree, select the check box for the node Physics>Stabilization.
- 6 Click OK.

HIGH MACH NUMBER FLOW, K- ϵ (HMNF)

- In the Model Builder window, under Component I (compl) click High Mach Number Flow, k-ε (hmnf).
- 2 In the Settings window for High Mach Number Flow, k-ε, click to expand the Inconsistent Stabilization section.
- 3 Find the Heat equation subsection. Select the Isotropic diffusion check box.
- **4** In the δ_{id} text field, type iso_diff.
- 5 Find the Navier-Stokes equations subsection. Select the Isotropic diffusion check box.
- **6** In the δ_{id} text field, type iso_diff.

Fluid I

- I In the Model Builder window, under Component I (compl)>High Mach Number Flow, k- ϵ (hmnf) click Fluid I.
- 2 In the Settings window for Fluid, locate the Thermodynamics section.

- 3 From the $R_{\rm s}$ list, choose User defined. In the associated text field, type Rs.
- **4** From the Specify Cp or γ list, choose Ratio of specific heats.
- **5** From the γ list, choose **User defined**. In the associated text field, type gamma.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** Specify the **u** vector as

0	r
100	z

4 In the *p* text field, type 2[atm].

Inlet 1

- I In the Physics toolbar, click Boundaries and choose Inlet.
- 2 In the Settings window for Inlet, locate the Boundary Selection section.
- 3 From the Selection list, choose Primary inlet.
- 4 Locate the Flow Properties section. From the Input state list, choose Total.
- **5** In the $p_{0,\text{tot}}$ text field, type P1.
- **6** In the $T_{0,\text{tot}}$ text field, type T1.
- 7 In the Ma_0 text field, type 0.14.

Inlet 2

- I In the Physics toolbar, click Boundaries and choose Inlet.
- 2 In the Settings window for Inlet, locate the Boundary Selection section.
- **3** From the Selection list, choose Secondary inlet.
- 4 Locate the Flow Properties section. From the Input state list, choose Total.
- **5** In the $p_{0,\text{tot}}$ text field, type P2.
- **6** In the $T_{0,\text{tot}}$ text field, type T2.
- 7 In the Ma_0 text field, type 0.01.

Outlet I

- I In the Physics toolbar, click Boundaries and choose Outlet.
- 2 In the Settings window for Outlet, locate the Boundary Selection section.
- 3 From the Selection list, choose Outlet.

- 4 Locate the Flow Condition section. From the Flow condition list, choose Subsonic.
- 5 Locate the Flow Properties section. From the Boundary condition list, choose Pressure.
- **6** In the p_0 text field, type Pout.

The next step is to generate a coarse mesh to compute an initial solution.

MESH I

- I In the Model Builder window, under Component I (compl) click Mesh I.
- 2 In the Settings window for Mesh, locate the Physics-Controlled Mesh section.
- **3** From the **Element size** list, choose **Coarse**.
- 4 Click 📗 Build All.

COMPONENT I (COMPI)

Generate a second mesh. Refine the boundary layer mesh and increase the mesh resolution on the walls and in the nozzle.

MESH 2

In the Mesh toolbar, click Add Mesh and choose Add Mesh.

Size 1

- I Right-click Mesh 2 and choose Size.
- 2 In the Settings window for Size, locate the Geometric Entity Selection section.
- 3 From the Geometric entity level list, choose Boundary.







6 From the Predefined list, choose Extremely fine.

Size 2

- I Right-click Mesh 2 and choose Size.
- 2 In the Settings window for Size, locate the Geometric Entity Selection section.
- 3 From the Geometric entity level list, choose Boundary.
- 4 From the Selection list, choose Walls.
- 5 In the list, choose 4 and 5.
- 6 Click Remove from Selection.
- **7** Select Boundaries 6–9 and 11–15 only.
- 8 Locate the Element Size section. From the Calibrate for list, choose Fluid dynamics.
- 9 From the Predefined list, choose Fine.

Size 3

- I Right-click Mesh 2 and choose Size.
- 2 In the Settings window for Size, locate the Geometric Entity Selection section.
- 3 From the Geometric entity level list, choose Domain.





6 From the Predefined list, choose Extremely fine.

Size 4

- I Right-click Mesh 2 and choose Size.
- 2 In the Settings window for Size, locate the Geometric Entity Selection section.
- 3 From the Geometric entity level list, choose Domain.





6 From the Predefined list, choose Coarser.

Size

- I In the Model Builder window, click Size.
- 2 In the Settings window for Size, locate the Element Size section.
- 3 From the Calibrate for list, choose Fluid dynamics.
- 4 From the Predefined list, choose Fine.

Corner Refinement I

- I In the Mesh toolbar, click 🔌 More Attributes and choose Corner Refinement.
- 2 In the Settings window for Corner Refinement, locate the Boundary Selection section.
- 3 Click to select the 🔲 Activate Selection toggle button.
- 4 From the Selection list, choose Walls.

Free Triangular 1

In the Mesh toolbar, click Kree Triangular.

Boundary Layers 1

In the Mesh toolbar, click **Boundary Layers**.

Boundary Layer Properties

- I In the Model Builder window, click Boundary Layer Properties.
- **2** In the **Settings** window for **Boundary Layer Properties**, locate the **Boundary Selection** section.
- 3 From the Selection list, choose Walls.
- 4 In the list, choose 4, 5, and 8.
- **5** Click **Remove from Selection**.
- 6 Select Boundaries 6, 7, 9, and 11–15 only.
- 7 Locate the Layers section. In the Number of layers text field, type 5.
- 8 From the Thickness specification list, choose First layer.
- 9 In the Thickness text field, type 5e-5.

Boundary Layer Properties 1

- I In the Mesh toolbar, click A More Attributes and choose Boundary Layer Properties.
- 2 In the Settings window for Boundary Layer Properties, locate the Layers section.
- 3 In the Number of layers text field, type 10.
- **4** From the **Thickness specification** list, choose **First layer**.
- 5 In the Thickness text field, type 1e-5.
- **6** Select Boundaries **4**, **5**, and **8** only (select the walls of both the primary inlet and the nozzle).



7 Click 📗 Build All.

STUDY I

Step 1: Stationary

- I In the Model Builder window, under Study I click Step I: Stationary.
- 2 In the Settings window for Stationary, click to expand the Mesh Selection section.
- **3** In the table, enter the following settings:

Component	Mesh
Component I	Mesh I

Edit the study step to solve the model in two steps in order to increase the robustness of the solution procedure. First, solve for $P_2=P_{out}$ (no adverse gradient of pressure), and then solve the problem again adding the adverse gradient of pressure (P_2 smaller than P_{out}). Disable the continuation solver since it is mainly suitable for linear applications.

- 4 Click to expand the **Study Extensions** section. Select the **Auxiliary sweep** check box.
- 5 Click + Add.
- 6 In the table, enter the following settings:

Parameter name	Parameter value list	Parameter unit
P2 (Total pressure, secondary flow)	Pout 0.55[atm]	Ра

7 Click + Add.

8 In the table, enter the following settings:

Parameter name	Parameter value list	Parameter unit
iso_diff (lsotropic diffusion)	0.5 0	

9 From the Run continuation for list, choose No parameter.

IO From the **Reuse solution from previous step** list, choose **Yes**.

Solve the problem with a finer mesh, and use the adaptive mesh refinement feature to resolve the mixing layer. The solution of study step 1 is used as the initial guess.

Stationary 2

- I In the Study toolbar, click 🔁 Study Steps and choose Stationary>Stationary.
- 2 In the Settings window for Stationary, click to expand the Mesh Selection section.

3 In the table, enter the following settings:

Component	Mesh
Component I	Mesh 2

- 4 Click to expand the Adaptation and Error Estimates section. From the Adaptation and error estimates list, choose Adaptation and error estimates.
- **5** Clear the **Allow coarsening** check box.

The amount of computational resources needed to solve the problem after refining the mesh can be reduced by means of an iterative solver.

Solution 1 (soll)

- I In the Study toolbar, click **The Show Default Solver**.
- 2 In the Model Builder window, expand the Solution I (soll) node.
- In the Model Builder window, expand the Study I>Solver Configurations>
 Solution I (soll)>Stationary Solver 2>Segregated I node, then click Flow variables u, p, T.
- 4 In the Settings window for Segregated Step, locate the General section.
- 5 From the Linear solver list, choose AMG, fluid flow variables (hmnf).
- 6 In the Model Builder window, under Study I>Solver Configurations>Solution I (solI)> Stationary Solver 2>Segregated I click Turbulence variables.
- 7 In the Settings window for Segregated Step, locate the General section.
- 8 From the Linear solver list, choose AMG, turbulence variables (hmnf).
- **9** In the **Study** toolbar, click **= Compute**.

Now, use Evaluation Group to compute individual mass flows and the difference between inlet and outlet mass flows to verify the mass conservation.

RESULTS

Evaluation mass flow group

- I In the **Results** toolbar, click **LEvaluation Group**.
- 2 Right-click Evaluation Group I and choose Rename.
- **3** In the **Rename Evaluation Group** dialog box, type Evaluation mass flow group in the **New label** text field.
- 4 Click OK.

Line Integration 1

I Right-click Evaluation mass flow group and choose Integration>Line Integration.

2 In the Settings window for Line Integration, locate the Expressions section.

3 In the table, enter the following settings:

Expression	Unit	Description
hmnf.rho*w	kg/s	

Line Integration 2

Right-click Line Integration I and choose Duplicate.

Line Integration 3

In the Model Builder window, right-click Line Integration 2 and choose Duplicate.

Primary mass flow

- I In the Model Builder window, right-click Line Integration I and choose Rename.
- 2 In the Rename Line Integration dialog box, type Primary mass flow in the New label text field.
- 3 Click OK.
- **4** Select Boundary 2 only.
- 5 In the Settings window for Line Integration, locate the Expressions section.
- 6 In the table, enter the following settings:

Expression	Unit	Description
hmnf.rho*w	kg/s	Primary mass flow

Secondary mass flow

- I In the Model Builder window, right-click Line Integration 2 and choose Rename.
- 2 In the **Rename Line Integration** dialog box, type Secondary mass flow in the **New label** text field.
- 3 Click OK.
- **4** Select Boundary 10 only.
- 5 In the Settings window for Line Integration, locate the Expressions section.
- 6 In the table, enter the following settings:

Expression	Unit	Description
hmnf.rho*w	kg/s	Secondary mass flow

Mixed mass flow

I In the Model Builder window, right-click Line Integration 3 and choose Rename.

- 2 In the Rename Line Integration dialog box, type Mixed mass flow in the New label text field.
- 3 Click OK.
- **4** Select Boundary 3 only.
- 5 In the Settings window for Line Integration, locate the Expressions section.
- 6 In the table, enter the following settings:

Expression	Unit	Description
hmnf.rho*w	kg/s	Mixed mass flow

Now, write the expression and evaluate the difference between inlet (**int1+int2**) and outlet (**int3**).

Evaluation mass flow group

- I In the Model Builder window, click Evaluation mass flow group.
- 2 In the Settings window for Evaluation Group, locate the Transformation section.
- **3** From the **Transformation type** list, choose **General**.
- **4** In the **Expression** text field, type int1+int2-int3.
- **5** Select the **Keep child nodes** check box.
- 6 In the Column header text field, type Difference between Inflow and Outflow.
- 7 In the Evaluation mass flow group toolbar, click **=** Evaluate.

Check if the average of the Mach number at the primary inlet is similar to the value defined in **Inlet 1**.

Mach number, primary inlet

- I In the Results toolbar, click ^{8,85}_{e-12} More Derived Values and choose Average>Line Average.
- 2 In the Settings window for Line Average, type Mach number, primary inlet in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Study I/ Adaptive Mesh Refinement Solutions I (sol3).
- 4 From the Parameter selection (Refinement level) list, choose Last.
- 5 Locate the Selection section. From the Selection list, choose Primary inlet.
- **6** Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
hmnf.Ma	1	Mach number

7 Click **= Evaluate**.

Check if the average of the Mach number at the secondary inlet is similar to the value defined in **Inlet 2**.

Mach number, secondary inlet

- I In the Results toolbar, click ^{8,85}_{e-12} More Derived Values and choose Average>Line Average.
- 2 In the Settings window for Line Average, type Mach number, secondary inlet in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Study I/ Adaptive Mesh Refinement Solutions I (sol3).
- 4 From the Parameter selection (Refinement level) list, choose Last.
- 5 Locate the Selection section. From the Selection list, choose Secondary inlet.

6 Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
hmnf.Ma	1	Mach number

7 Click **=** Evaluate.

TABLE

I Go to the **Table** window.

In case that the Mach number at one or both inlets diverge from the imposed values, the problem should be solved again using the new Mach numbers at the inlet.

RESULTS

Mirror 2D I

- I In the **Results** toolbar, click **More Datasets** and choose **Mirror 2D**.
- 2 In the Settings window for Mirror 2D, locate the Data section.
- 3 From the Dataset list, choose Study I/Adaptive Mesh Refinement Solutions I (sol3).
- 4 Click 🗿 Plot.

Plot the turbulent kinetic energy.

Turbulent Kinetic Energy

- I In the **Results** toolbar, click **2D Plot Group**.
- 2 In the Settings window for 2D Plot Group, type Turbulent Kinetic Energy in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Mirror 2D I.

Surface 1

- I Right-click Turbulent Kinetic Energy and choose Surface.
- 2 In the Settings window for Surface, locate the Expression section.
- **3** In the **Expression** text field, type k.
- **4** In the **Turbulent Kinetic Energy** toolbar, click **I** Plot (see Figure 4).

Plot the temperature.

Temperature, 2D

- I In the Home toolbar, click 🚛 Add Plot Group and choose 2D Plot Group.
- 2 In the Settings window for 2D Plot Group, type Temperature, 2D in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Mirror 2D I.

Surface 1

- I Right-click Temperature, 2D and choose Surface.
- 2 In the Settings window for Surface, locate the Expression section.
- **3** In the **Expression** text field, type T.
- 4 Locate the Coloring and Style section. From the Color table list, choose Thermal.
- **5** In the **Temperature**, **2D** toolbar, click **Plot** (see Figure 6).

Plot the evolution of pressure along the mixing chamber.

Center-line

- I In the **Results** toolbar, click \frown **Cut Line 2D**.
- 2 In the Settings window for Cut Line 2D, type Center-line in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Study I/ Adaptive Mesh Refinement Solutions I (sol3).
- 4 Locate the Line Data section. In row Point 2, set r to 0.
- 5 In row **Point 2**, set z to L_mixing.
- 6 Click 💿 Plot.

Wall

- I In the **Results** toolbar, click \frown **Cut Line 2D**.
- 2 In the Settings window for Cut Line 2D, type Wall in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Study I/ Adaptive Mesh Refinement Solutions I (sol3).
- 4 Locate the Line Data section. In row Point I, set r to d_mixing/2.

- 5 In row **Point 2**, set **r** to d_mixing/2.
- 6 In row **Point 2**, set **z** to L_mixing.
- 7 Click 💽 Plot.

ID Plot Group 10

- I In the Results toolbar, click \sim ID Plot Group.
- 2 In the Settings window for ID Plot Group, locate the Legend section.
- **3** From the **Position** list, choose **Lower right**.

Line Graph 1

- I Right-click ID Plot Group 10 and choose Line Graph.
- 2 In the Settings window for Line Graph, locate the Data section.
- **3** From the **Dataset** list, choose **Center-line**.
- **4** From the **Parameter selection (Refinement level)** list, choose **Last**.
- **5** Locate the **y-Axis Data** section. In the **Expression** text field, type p.
- 6 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 7 In the **Expression** text field, type z.
- 8 Click to expand the Legends section. Select the Show legends check box.
- 9 From the Legends list, choose Manual.
- **IO** In the table, enter the following settings:

Legends

Center-line

Line Graph 2

- I In the Model Builder window, right-click ID Plot Group 10 and choose Line Graph.
- 2 In the Settings window for Line Graph, locate the Data section.
- **3** From the **Dataset** list, choose **Wall**.
- 4 From the Parameter selection (Refinement level) list, choose Last.
- 5 Locate the y-Axis Data section. In the Expression text field, type p.
- 6 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 7 In the **Expression** text field, type z.
- 8 Locate the Legends section. Select the Show legends check box.
- 9 From the Legends list, choose Manual.

IO In the table, enter the following settings:

Legends

Walls

ID Plot Group 10

- I In the Model Builder window, click ID Plot Group 10.
- 2 In the ID Plot Group 10 toolbar, click I Plot (see Figure 5).

Velocity (hmnf)

- I In the Model Builder window, click Velocity (hmnf).
- 2 In the Settings window for 2D Plot Group, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D I.
- **4** In the **Velocity (hmnf)** toolbar, click **I** Plot.



Mach Number (hmnf)

- I In the Model Builder window, click Mach Number (hmnf).
- 2 In the Settings window for 2D Plot Group, locate the Data section.
- 3 From the Dataset list, choose Mirror 2D I.
- 4 In the Mach Number (hmnf) toolbar, click 💿 Plot.
- **5** Click the **1 Zoom Extents** button in the **Graphics** toolbar (see Figure 2).