

Cross-Flow Heat Exchanger

Introduction

This application simulates the fluid flow and heat transfer in a micro heat exchanger of cross-flow type made of stainless steel. Heat exchangers of this type are found in lab-onchip devices in biotechnology and microreactors, for example for micro fuel cells. The application takes into account heat transferred through both convection and conduction. The geometry and material properties are taken from Ref. 1.

Model Definition

Figure 1 shows the heat exchanger's geometry. Notice that the fluid channels have a square cross section rather than the circular cross section more commonly used in micro heat exchangers. A cross-flow heat exchanger can typically consist of about 20 unit cells. However, because the unit cells are identical except for edge effects in the outer cells, you can restrict the model to a single unit cell.

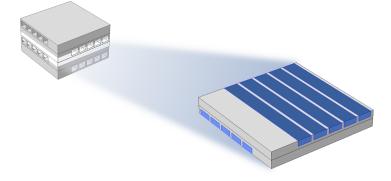


Figure 1: Depiction of the modeled part of the micro-heat exchanger.

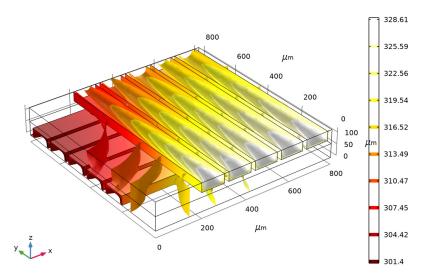
Because heat is transferred by convection and conduction, the model uses a Conjugate Heat Transfer interface in the laminar flow regime.

The boundary conditions are insulating for all outer surfaces except for the inlet and outlet boundaries. At the inlets for both cold and hot streams, the temperatures are constant and a laminar inflow profile with an average velocity of 50 mm/s is defined.

At the outlet, the heat transport is dominated by convection, which makes the outflow boundary condition suitable. For the flow field, the model applies the outlet boundary condition with a constant pressure. As shown in Figure 1, you can take advantage of the model's symmetries to model only half of the channel height. Therefore, the symmetry boundary condition applies to the channels.

Results and Discussion

Figure 2 shows the temperature at the channel walls as well as temperature isosurfaces in the device, which clearly reveal the influence of the convective term.



Isosurface: Temperature (K) Surface: Temperature (K)

Figure 2: Channel wall temperature and isotherms through the cell geometry.

As can be seen in Figure 3, the temperature differs significantly between the different outlets in both hot and cold streams. This implies that the hot stream is not cooled uniformly.

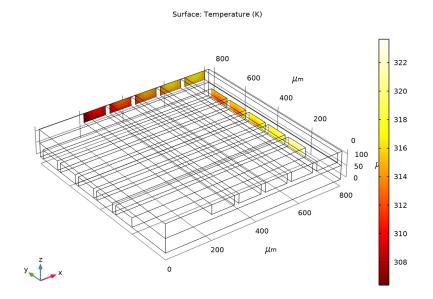
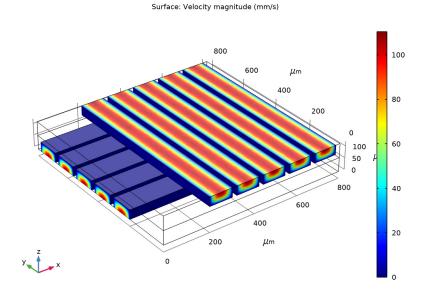


Figure 3: Temperature field at the outlet boundaries.



The flow field in the channels is a typical laminar velocity profile; see Figure 4.

Figure 4: Velocity profile in the channels.

There are several quantities that describe the characteristics and effectiveness of a heat exchanger. The mixing-cup temperature of the fluid leaving the heat exchanger is calculated according to (1.4 in Ref. 2).

$$\langle T \rangle = \frac{\int \rho C_p T u ds}{\int \rho C_p u ds}$$
(1)
outlet

COMSOL Multiphysics provides built-in variables to easily calculate $\langle T \rangle$. At the upper channels, the outlet mixing-cup temperature is about 40.5°C. At the lower channels, a higher value of 43°C is found for the outlet mixing-cup temperature. The maximum pressure drop in the heat exchanger is about 92 Pa.

The overall heat transfer coefficient is another interesting quantity. It is a measure of the performance of a heat exchanger design defined as

$$h_{\rm eq} = \frac{P}{A(T_{\rm hot} - T_{\rm cold})}$$
(2)

where *P* is the total exchanged power and *A* is the surface area through which *P* flows. In this model, the value of h_{eq} is about 3150 W/(m²·K).

References

1. W. Ehrfeld, V. Hessel, and H. Löwe, Microreactors, John Wiley & Sons, 2000.

2. P.K. Nag, Heat and Mass Transfer, 2nd ed., Tata McGraw-Hill, 2007.

Application Library path: Heat_Transfer_Module/Heat_Exchangers/ crossflow_heat_exchanger

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click 🙆 Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click 间 3D.
- 2 In the Select Physics tree, select Heat Transfer>Conjugate Heat Transfer>Laminar Flow.
- 3 Click Add.
- 4 Click \bigcirc Study.

In this model, you consider the flow to be nearly incompressible and independent from temperature variations. For this assumption, the **Stationary** study sequence is the most performant.

- 5 In the Select Study tree, select Preset Studies for Selected Multiphysics>Stationary, One-Way NITF.
- 6 Click M Done.

GLOBAL DEFINITIONS

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.

3 In the table, enter the following settings:

Name	Expression	Value	Description
T_cold	300[K]	300 K	Temperature, cold stream
T_hot	330[K]	330 K	Temperature, hot stream
u_avg	50[mm/s]	0.05 m/s	Average inlet velocity

GEOMETRY I

- I In the Model Builder window, under Component I (compl) click Geometry I.
- 2 In the Settings window for Geometry, locate the Units section.
- 3 From the Length unit list, choose µm.

First, create the cross-section of one unit cell and extrude it.

Block I (blkI)

- I In the **Geometry** toolbar, click 🗍 **Block**.
- 2 In the Settings window for Block, locate the Size and Shape section.
- 3 In the Width text field, type 800.
- 4 In the **Depth** text field, type 800.
- 5 In the **Height** text field, type 60.
- 6 Click 틤 Build Selected.

Block 2 (blk2)

- I In the **Geometry** toolbar, click 🗍 Block.
- 2 In the Settings window for Block, locate the Size and Shape section.
- 3 In the Width text field, type 800.
- 4 In the **Depth** text field, type 100.
- 5 In the **Height** text field, type 40.
- 6 Locate the **Position** section. In the **y** text field, type 200.
- 7 Click 틤 Build Selected.

Array I (arr I)

- I In the Geometry toolbar, click 💭 Transforms and choose Array.
- 2 Select the object **blk2** only.
- 3 In the Settings window for Array, locate the Size section.
- 4 From the Array type list, choose Linear.
- 5 In the Size text field, type 5.
- 6 Locate the Displacement section. In the y text field, type 120.
- 7 Locate the Selections of Resulting Entities section. Find the Cumulative selection subsection. Click New.
- 8 In the New Cumulative Selection dialog box, type Channels in the Name text field.
- 9 Click OK.

Rotate | (rot])

- I In the Geometry toolbar, click 💭 Transforms and choose Rotate.
- 2 Click in the Graphics window and then press Ctrl+A to select all objects.
- 3 In the Settings window for Rotate, locate the Rotation section.
- 4 In the Angle text field, type 180.
- 5 Locate the Point on Axis of Rotation section. In the z text field, type 60.
- 6 Locate the Rotation section. From the Axis type list, choose Cartesian.
- 7 In the **x** text field, type 1.
- 8 In the y text field, type 1.
- **9** In the **z** text field, type **0**.

Keep the existing unit cell by the following step.

- 10 Locate the Input section. Select the Keep input objects check box.
- II Click 🟢 Build All Objects.

12 Click the \longleftrightarrow **Zoom Extents** button in the **Graphics** toolbar.

Define several selections that help you throughout the model set-up.

DEFINITIONS

Upper Inlets

- I In the Definitions toolbar, click http://www.explicit.
- 2 In the Settings window for Explicit, type Upper Inlets in the Label text field.
- **3** Locate the Input Entities section. From the Geometric entity level list, choose Boundary.

4 Select Boundaries 41, 48, 55, 62, and 69 only.

Lower Inlets

- I In the **Definitions** toolbar, click **here Explicit**.
- 2 In the Settings window for Explicit, type Lower Inlets in the Label text field.
- 3 Locate the Input Entities section. From the Geometric entity level list, choose Boundary.
- 4 Select Boundaries 8, 14, 20, 26, and 32 only.

Upper Outlets

- I In the **Definitions** toolbar, click **here Explicit**.
- 2 In the Settings window for Explicit, type Upper Outlets in the Label text field.
- 3 Locate the Input Entities section. From the Geometric entity level list, choose Boundary.
- 4 Select Boundaries 44, 51, 58, 65, and 72 only.

Lower Outlets

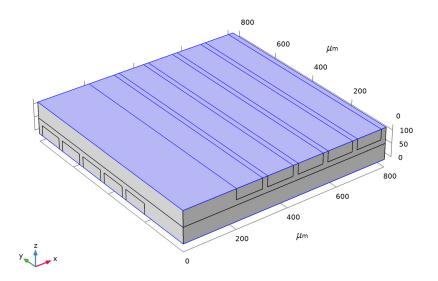
- I In the **Definitions** toolbar, click **here Explicit**.
- 2 In the Settings window for Explicit, type Lower Outlets in the Label text field.
- **3** Locate the Input Entities section. From the Geometric entity level list, choose Boundary.
- 4 Select Boundaries 77–81 only.

Symmetry

- I In the **Definitions** toolbar, click **here Explicit**.
- 2 In the Settings window for Explicit, type Symmetry in the Label text field.
- 3 Locate the Input Entities section. From the Geometric entity level list, choose Boundary.

4 Select the Group by continuous tangent check box.

Select one of the uppermost and lowermost boundaries, which now automatically will select all uppermost and lowermost boundaries thanks to the continuous tangency.



The next selections are needed to evaluate the equivalent heat transfer coefficient.

Outlets

- I In the **Definitions** toolbar, click 📑 **Union**.
- 2 In the Settings window for Union, type Outlets in the Label text field.
- 3 Locate the Geometric Entity Level section. From the Level list, choose Boundary.
- 4 Locate the Input Entities section. Under Selections to add, click + Add.
- **5** In the Add dialog box, in the Selections to add list, choose Upper Outlets and Lower Outlets.
- 6 Click OK.

MATERIALS

Define the material properties.

Stainless Steel

I In the Materials toolbar, click 🚦 Blank Material.

2 In the Settings window for Material, type Stainless Steel in the Label text field.

3 Locate the Material Contents section. In the table, enter the following settings:

Property	Variable	Value	Unit	Property group
Thermal conductivity	k_iso ; kii = k_iso, kij = 0	15	W/(m·K)	Basic
Density	rho	7800	kg/m³	Basic
Heat capacity at constant pressure	Ср	420	J/(kg·K)	Basic

ADD MATERIAL

- I In the Materials toolbar, click 🙀 Add Material to open the Add Material window.
- **2** Go to the **Add Material** window.
- 3 In the tree, select Built-in>Water, liquid.
- 4 Click Add to Component in the window toolbar.
- 5 In the Materials toolbar, click 🙀 Add Material to close the Add Material window.

MATERIALS

Water, liquid (mat2)

- I In the Settings window for Material, locate the Geometric Entity Selection section.
- 2 From the Selection list, choose Channels.

HEAT TRANSFER IN SOLIDS AND FLUIDS (HT)

Set the reference temperature to an estimated value of (T_cold+T_hot)/2 where the flow operates.

- I In the Model Builder window, under Component I (comp1) click Heat Transfer in Solids and Fluids (ht).
- 2 In the Settings window for Heat Transfer in Solids and Fluids, locate the Physical Model section.
- **3** In the $T_{\rm ref}$ text field, type (T_cold+T_hot)/2.

Fluid I

- I In the Model Builder window, under Component I (compl)> Heat Transfer in Solids and Fluids (ht) click Fluid I.
- 2 In the Settings window for Fluid, locate the Domain Selection section.

3 From the Selection list, choose Channels.

Inflow I

- I In the Physics toolbar, click 📄 Boundaries and choose Inflow.
- 2 In the Settings window for Inflow, locate the Boundary Selection section.
- **3** From the Selection list, choose Upper Inlets.
- **4** Locate the **Upstream Properties** section. In the T_{ustr} text field, type T_hot.

Inflow 2

- I In the **Physics** toolbar, click **Boundaries** and choose **Inflow**.
- 2 In the Settings window for Inflow, locate the Boundary Selection section.
- 3 From the Selection list, choose Lower Inlets.
- **4** Locate the **Upstream Properties** section. In the T_{ustr} text field, type T_cold.

Outflow I

- I In the Physics toolbar, click 🔚 Boundaries and choose Outflow.
- 2 In the Settings window for Outflow, locate the Boundary Selection section.
- 3 From the Selection list, choose Upper Outlets.

Outflow 2

- I In the Physics toolbar, click 📄 Boundaries and choose Outflow.
- 2 In the Settings window for Outflow, locate the Boundary Selection section.
- **3** From the Selection list, choose Lower Outlets.

Symmetry I

- I In the Physics toolbar, click 📄 Boundaries and choose Symmetry.
- 2 In the Settings window for Symmetry, locate the Boundary Selection section.
- 3 From the Selection list, choose Symmetry.

So far, the boundary conditions for heat transfer have been specified. Continue with the setup of the flow equation.

LAMINAR FLOW (SPF)

The density variations are small enough to consider the fluid as incompressible. Change the compressibility option accordingly in the physics interface. The reference temperature is set in the Heat Transfer interface.

- I In the Model Builder window, under Component I (compl) click Laminar Flow (spf).
- 2 In the Settings window for Laminar Flow, locate the Physical Model section.

3 From the **Compressibility** list, choose **Incompressible flow**.

4 Locate the Domain Selection section. From the Selection list, choose Channels.

Because of the different inlet temperatures, the densities for the hot and cold stream vary and produce different velocities when the laminar inflow boundary condition is used. In order to have the same velocity profile on each inlet, define the laminar inflow boundary condition for the hot and cold inlet boundaries separately.

Inlet 1

- I In the Physics toolbar, click 🔚 Boundaries and choose Inlet.
- 2 In the Settings window for Inlet, locate the Boundary Selection section.
- 3 From the Selection list, choose Upper Inlets.
- 4 Locate the Boundary Condition section. From the list, choose Fully developed flow.
- 5 Locate the Fully Developed Flow section. In the U_{av} text field, type u_avg.

Inlet 2

- I In the Physics toolbar, click 🔚 Boundaries and choose Inlet.
- 2 In the Settings window for Inlet, locate the Boundary Selection section.
- 3 From the Selection list, choose Lower Inlets.
- 4 Locate the Boundary Condition section. From the list, choose Fully developed flow.
- 5 Locate the Fully Developed Flow section. In the U_{av} text field, type u_avg.

Outlet I

- I In the Physics toolbar, click 🔚 Boundaries and choose Outlet.
- 2 In the Settings window for Outlet, locate the Boundary Selection section.
- **3** From the Selection list, choose Upper Outlets.

Outlet 2

- I In the Physics toolbar, click 🔚 Boundaries and choose Outlet.
- 2 In the Settings window for Outlet, locate the Boundary Selection section.
- 3 From the Selection list, choose Lower Outlets.

Symmetry I

- I In the Physics toolbar, click 📄 Boundaries and choose Symmetry.
- 2 In the Settings window for Symmetry, locate the Boundary Selection section.
- **3** From the **Selection** list, choose **Symmetry**.

After solving the model, the equivalent heat transfer coefficient is evaluated according to Equation 2. To do so, define the following nonlocal coupling.

MULTIPHYSICS

Nonisothermal Flow 1 (nitf1)

- I In the Model Builder window, under Component I (compl)>Multiphysics click Nonisothermal Flow I (nitfl).
- 2 In the Settings window for Nonisothermal Flow, locate the Material Properties section.
- **3** Select the **Boussinesq approximation** check box.

DEFINITIONS

Average on Upper Channel Walls

- I In the Definitions toolbar, click 🖉 Nonlocal Couplings and choose Average.
- 2 In the Settings window for Average, type Average on Upper Channel Walls in the Label text field.
- **3** Locate the **Source Selection** section. From the **Geometric entity level** list, choose **Boundary**.
- 4 Select Boundaries 40, 42, 45, 47, 49, 52, 54, 56, 59, 61, 63, 66, 68, 70, and 73 only.

To select more easily these boundaries, use the **Paste** button and insert the list of numbers above in the **Paste Selection** dialog box.

STUDY I

In the **Home** toolbar, click **= Compute**.

RESULTS

Temperature (ht)

COMSOL Multiphysics automatically creates four default plots: a temperature plot, an isothermal contour plot, a slice plot for the velocity field, and contour plot for the pressure field. The isothermal contours will be modified, to create the plot shown in Figure 2.

Isothermal Contours (ht) In the Model Builder window, click Isothermal Contours (ht).

Surface 1

I In the Isothermal Contours (ht) toolbar, click T Surface.

2 In the Settings window for Surface, locate the Data section.

- 3 From the Dataset list, choose Exterior Walls.
- 4 Click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component I (compl)>Heat Transfer in Solids and Fluids>Temperature>T Temperature K.
- 5 Click to expand the Inherit Style section. From the Plot list, choose Isosurface.
- 6 In the Isothermal Contours (ht) toolbar, click **O** Plot.

To visualize the velocity field as in Figure 4, follow the steps below:

Slice

- I In the Model Builder window, expand the Velocity (spf) node.
- 2 Right-click Slice and choose Delete.

Velocity (spf)

In the Model Builder window, click Velocity (spf).

Surface 1

- I In the Velocity (spf) toolbar, click T Surface.
- 2 In the Settings window for Surface, click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component I (compl)>Laminar Flow> Velocity and pressure>spf.U - Velocity magnitude - m/s.
- 3 Locate the Expression section. From the Unit list, choose mm/s.
- 4 In the Velocity (spf) toolbar, click **I** Plot.

To show the temperature on the outlet boundaries only, as in Figure 3, first produce a new dataset for the selection built before. Then use this dataset for a surface plot of the temperature.

Outlets

- I In the Results toolbar, click More Datasets and choose Surface.
- 2 In the Settings window for Surface, type Outlets in the Label text field.
- 3 Locate the Selection section. From the Selection list, choose Outlets.

Outlet Temperature

- I In the Results toolbar, click 间 3D Plot Group.
- 2 In the Settings window for 3D Plot Group, type Outlet Temperature in the Label text field.

Surface 1

I In the **Outlet Temperature** toolbar, click Temperature.

- 2 In the Settings window for Surface, locate the Data section.
- 3 From the Dataset list, choose Outlets.
- 4 Locate the Coloring and Style section. From the Color table list, choose ThermalLight.
- **5** In the **Outlet Temperature** toolbar, click **O Plot**.

Mixing-Cup Temperatures

- I In the **Results** toolbar, click (8.5) Global Evaluation.
- 2 In the Settings window for Global Evaluation, type Mixing-Cup Temperatures in the Label text field.
- 3 Click Replace Expression in the upper-right corner of the Expressions section. From the menu, choose Component I (comp1)>Heat Transfer in Solids and Fluids>Temperature> Weighted average temperature>ht.ofl1.Tave Weighted average temperature K.
- **4** Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
ht.ofl1.Tave	degC	Weighted average temperature (Upper Outlets)
ht.ofl2.Tave	degC	Weighted average temperature (Lower Outlets)

5 Click **=** Evaluate.

TABLE

I Go to the Table window.

The mixing-cup temperature at upper outlets is about 40.5°C and at the lower outlets about 43°C.

RESULTS

To calculate the maximum pressure drop proceed as follows:

Maximum Pressure Drop

- I In the Results toolbar, click ^{8.85}_{e-12} More Derived Values and choose Maximum> Surface Maximum.
- 2 In the Settings window for Surface Maximum, locate the Selection section.
- 3 From the Selection list, choose All boundaries.
- 4 Click Replace Expression in the upper-right corner of the Expressions section. From the menu, choose Component I (compl)>Laminar Flow>Velocity and pressure>p Pressure Pa.
- 5 In the Label text field, type Maximum Pressure Drop.

6 Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description
р	Ра	Maximum pressure drop

7 Click **=** Evaluate.

TABLE

I Go to the Table window.

The maximum pressure is 90 Pa. The minimum pressure is defined by the outlet boundary conditions and is zero. Thus, the maximum pressure drop is also 90 Pa.

Now, evaluate the equivalent heat transfer coefficient as defined in Equation 2. You can use the integration operators defined previously in **Component I>Definitions**.

RESULTS

Heat Transfer Coefficient

- I In the Results toolbar, click (8.5) Global Evaluation.
- 2 In the Settings window for Global Evaluation, locate the Expressions section.
- **3** In the table, enter the following settings:

Expression	Unit	Description
aveop1(ht.ntflux)/(T_hot-T_cold)	W/(m^2*K)	Heat transfer coefficient

4 In the Label text field, type Heat Transfer Coefficient.

5 Click **=** Evaluate.

TABLE

I Go to the Table window.

The equivalent heat transfer coefficient is about $3000 \text{ W/(m}^2 \cdot \text{K})$.

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