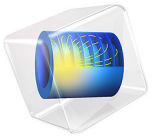

Species Transport in the Gas Diffusion Layers of a PEM

Introduction

This example focuses on the species transport within the gas diffusion layers (GDLs) of a proton exchange membrane (PEM) fuel cell. The geometry models a cell with two adjacent flow channels of different pressures, a situation that may occur in a cell with serpentine flow channels, or in a cell using a interdigitated flow field design. The model uses current balances, mass transport equations (Maxwell-Stefan diffusion for reactants, water and nitrogen gas), and momentum transport (Darcy's law for the gas flows) to simulate a PEM fuel cell's behavior.

Model Definition

The modeled section of the fuel cell consists of three domains: an anode (Ω_a), a proton exchange membrane (Ω_m), and a cathode (Ω_c) as indicated in Figure 1.

Electrode height: 2 mm
Electrode width:0.25 mm
Membrane thickness: 0.1 mm
Collector height: 1 mm

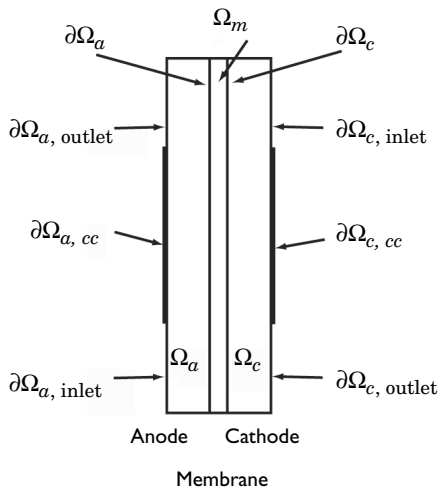

Figure 1: Model geometry with domain and boundary labels.

Each of the electrodes (gas diffusion layers) is in contact with an interdigitated gas distributor, which has an inlet channel ($\partial\Omega_{a,inlet}$), a current collector ($\partial\Omega_{a,cc}$), and an outlet channel ($\partial\Omega_{a,outlet}$). The same notation is used for the cathode side.

Humidified hydrogen and air are supplied to the inlet channels of the anode and cathode, respectively. Hydrogen reacts and is consumed at the anodic active layer to form protons that carry the ionic current to the cathode. Each proton is assumed to drag three molecules

of water from the anode to the cathode, resulting in the following reaction formula for the anode:

$$H_2 + 2\lambda_{H2O}H_2O \Rightarrow 2\left(H^+ + \lambda_{H2O}H_2O\right) + 2e^- \quad (1)$$

Where λ_{H2O} is the number of water molecules that are transported per proton through the membrane by water-proton interaction.

At the cathode, oxygen reacts together with the protons to form water at the active layer according to:

$$O_2 + 4\left(H^+ + \lambda_{H2O}H_2O\right) + 4e^- \Rightarrow (2 + 4\lambda_{H2O})H_2O \quad (2)$$

Both feed gases (humidified hydrogen and humidified air) are treated as ideal and are transported through diffusion and convection. The electrodes are treated as homogeneous porous media with uniform morphological properties such as porosity and permeability. The gas within each of the electrodes exists as a continuous phase so Darcy's law applies.

An agglomerate model describes the electrode reactions in the active catalyst layers. The agglomerates consist of catalyst and carbon particles embedded in polymer electrolyte. The equations for the agglomerate model originate from the analytical solution of a diffusion-reaction problem in a spherical porous particle (Ref. 5 and Ref. 6). At the anodic active catalyst layer, hydrogen is the diffusing and reacting species in the agglomerates, while oxygen is the diffusing and reacting species in the agglomerates at the cathode. An agglomerate model of the cathodic active catalyst layer of a PEM fuel cell has been presented by Broka and others (Ref. 7 and Ref. 8).

CHARGE BALANCES

The Hydrogen Fuel Cell interface is used for modeling the potential distributions in the three domains, with the charge-transfer current density of the active layers described as interior boundary conditions, using Thin H2/O2 Gas Diffusion Electrode nodes. The local current density expressions for the anode and cathode, i_a and i_c, are specified according to the equation

$$i_e = \frac{R_{agg}}{3} j_{agg,e}$$

where the index e stands for "a" (anode) or "c" (cathode), R_{agg} is the agglomerate radius (SI unit: m) and $j_{agg,a}$ and $j_{agg,c}$ (SI unit: A/m^3) are the current densities given by the agglomerate model. Further, L_{act} is the active layer (thin gas diffusion electrode) thickness

(m) and ε_{mac} its porosity (the macroscopic porosity). The specific surface area of the thin gas diffusion electrode (SI unit: 1/m) is specified according to the following equation as

$$a_v = \frac{3}{R_{agg}}(1-\varepsilon_{mac})$$

AGGLOMERATE MODEL FOR ANODE AND CATHODE

The agglomerate model describes the current density in an active layer consisting of agglomerates of ionic conductor material and electrically conducting particles covered partially with catalyst. The local current density can be expressed analytically by solving a combination of the diffusion equation and the Butler-Volmer electrode kinetic equation for an agglomerate with constant electric and ionic potentials. The resulting equations for the current density in the anode and cathode are (Ref. 7)

$$j_{agg,e} = 6n_eF\left(\frac{D_{agg}}{R_{agg}^2}\right)(1-\lambda_e\coth\lambda_e)\beta_e$$

where, again, the index e stands for "a" (anode) or "c" (cathode), and

$$\lambda_a = \sqrt{\frac{i_{0a}SR_{agg}^2}{2Fc_{H_2,ref}D_{agg}}} \qquad \lambda_c = \sqrt{\frac{i_{0c}SR_{agg}^2}{4Fc_{O_2,ref}D_{agg}}\exp\left(-\frac{F}{2RT}\eta_c\right)}$$

$$\beta_a = \left[c_{H_2,agg} - c_{H_2,ref}\exp\left(\frac{-2F}{RT}\eta_a\right)\right] \qquad \beta_c = c_{O_2,agg}$$

In these equations, D_{agg} is the agglomerate gas diffusivity (SI unit: m^2/s), n_e is a "charge transfer" number (1 for the anode and –2 for the cathode), S is the specific area of the catalyst inside the agglomerate (SI unit: 1/m), and F is Faraday's constant (SI unit: C/mol). Furthermore, $c_{i,ref}$ are the reference concentrations of the species (SI unit: mol/m^3), $c_{i,agg}$ are the corresponding concentrations in the agglomerate surface (SI unit: mol/m^3), i_{0a} and i_{0c} are the exchange current densities (SI unit: A/m^2), R is the gas constant, T is the temperature (SI unit: K), and the overvoltages at the anode and the cathode are given by

$$\eta_a = \phi_s - \phi_l - E_{eq,a} \qquad \eta_c = \phi_s - \phi_l - E_{eq,c}$$

where E_{eq} (SI unit: V) denotes the equilibrium voltage.

You set the anodic and cathodic reference states equal to the molar fractions at the inlet channels of the anode and cathode, respectively, at 1 atm. The dissolved hydrogen and oxygen concentrations at the surface of the agglomerates are related to the molar fractions of the respective species in the gas phase through Henry's law

$$c_{\text{agg, H2}} = \frac{p_{\text{H}} x_{\text{H}}}{K_{\text{H}}}$$

$$c_{\text{agg, O2}} = \frac{p_{\text{O2}} x_{\text{O2}}}{K_{\text{O2}}}$$

where K is Henry's constant (SI unit: Pa·m^3/mol).

CHARGE BALANCES, CONTINUED

The potential difference between the cathode and anode current collectors corresponds to the total cell voltage. Choose the potential at the anode current collector as the reference level by setting it to zero. Then the total cell voltage serves as the boundary condition at the cathode current collector:

$$\phi_s = 0 \quad \text{at } \partial\Omega_{\text{a, cc}}$$
$$\phi_s = V_{\text{cell}} \text{ at } \partial\Omega_{\text{c, cc}}$$

For the other boundaries you have electric insulation boundary conditions.

POROUS MEDIA FLUID FLOW

To model the gas flows in the gas backings, this example uses the Darcy's law in the Hydrogen Fuel Cell interface. The gas velocity is given by the continuity equation according to

$$\nabla \cdot (\rho \mathbf{u}) = 0 \qquad \text{in } \Omega_{\text{a}} \text{ and } \Omega_{\text{c}}$$

where ρ is the mixture density of the gas phase (SI unit: kg/m^3) and $\mathbf{u}$ denotes the gas velocity (SI unit: m/s). Darcy's law for porous media states that the gradient of pressure, the viscosity of the fluid, and the structure of the porous media determine the velocity:

$$\mathbf{u} = -\frac{k_p}{\eta} \nabla p$$

Here k_p denotes the electrode's permeability (SI unit: m^2), η represents the gas viscosity (SI unit: Pa·s), and p is the pressure (SI unit: Pa). The ideal gas law gives the gas phase's mixture density, ρ:

$$\rho = \frac{p}{RT}\sum_i M_i x_i \tag{3}$$

In this equation, R denotes the gas constant (SI unit: J/(mol·K)), T is the temperature (SI unit: K), M is the molar mass (SI unit: kg/mol), and x is the mole fraction.

At the inlets and outlets you specify the pressure:

$$p = p_{\mathrm{a,\,in}} \text{ at } \partial\Omega_{\mathrm{a,\,inlet}}$$
$$p = p_{\mathrm{ref}} \text{ at } \partial\Omega_{\mathrm{a,\,outlet}}$$
$$p = p_{\mathrm{c,\,in}} \text{ at } \partial\Omega_{\mathrm{c,\,inlet}}$$
$$p = p_{\mathrm{ref}} \text{ at } \partial\Omega_{\mathrm{c,\,outlet}}$$

At the thin gas diffusion electrode boundary for the anode and cathode, the gas velocity is calculated automatically by the Hydrogen Fuel Cell interface, from the total mass flow given by the electrochemical reaction rate and the stoichiometric coefficients of Equation 1 and Equation 2, using Faraday's law.

MAXWELL-STEFAN MASS TRANSPORT

The model takes into account two species in the anode — H_2 and H_2O — and three at the cathode — O_2, H_2O, and N_2. The Hydrogen Fuel Cell interface uses Maxwell-Stefan multicomponent diffusion governed by the following equation

$$\frac{\partial}{\partial t}\rho w_i + \nabla\cdot\left[-\rho w_i\sum_{j=1}^{N} D_{ij}\left\{\frac{M}{M_j}\left(\nabla w_j + w_j\frac{\nabla M}{M}\right) + (x_j - w_j)\frac{\nabla p}{p}\right\} + w_i\rho\mathbf{u} + D_i^T\frac{\nabla T}{T}\right] = R_i$$

o solve for the mass fractions, w_i. This particular PEM fuel cell model assumes that the temperature-driven diffusion is insignificant and sets the source term, R, to zero. The Maxwell-Stefan binary diffusion coefficients, D_{ij} (SI unit: m^2/s), are calculated automatically by the interface.

The feed-gas mole fractions are specified at the inlets. At the outlets, convective flux boundary conditions are applied, meaning that the flux is convection dominated. At the thin gas diffusion electrode boundaries, the mass fluxes of the species are automatically determined from the electrochemical reaction rate and stoichiometric coefficients, using

Faraday's law. The Stefan velocity contributions are also automatically calculated by the interface.

Results and Discussion

Figure 2 shows the current distribution in the PEM fuel cell. There are significant current spikes present at the corners of the current collectors.

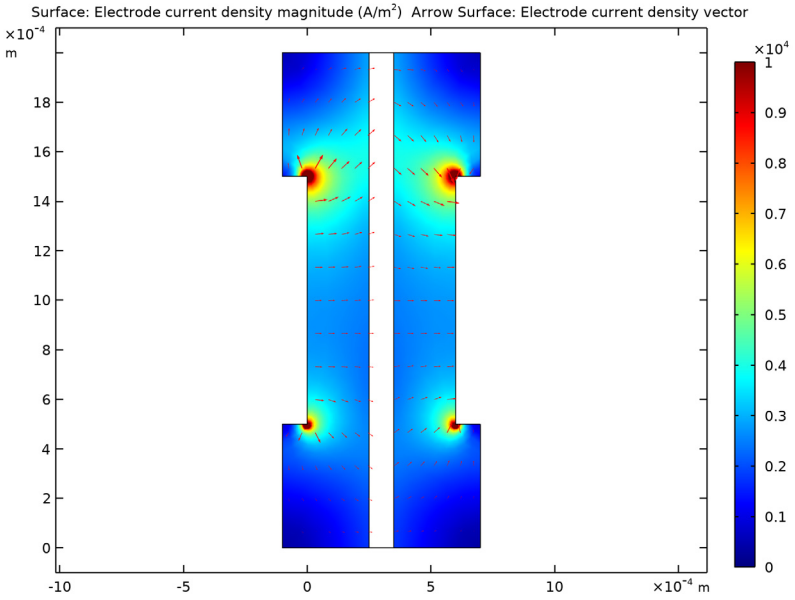

Figure 2: Current density (surface plot) and current vector field (arrow plot) in the fuel cell operating at 0.7 V. The anode is on the left and the cathode is on the right.

To further analyze the cell's behavior, plot the current density at the active layer as a function of cell height (y) as in Figure 3.

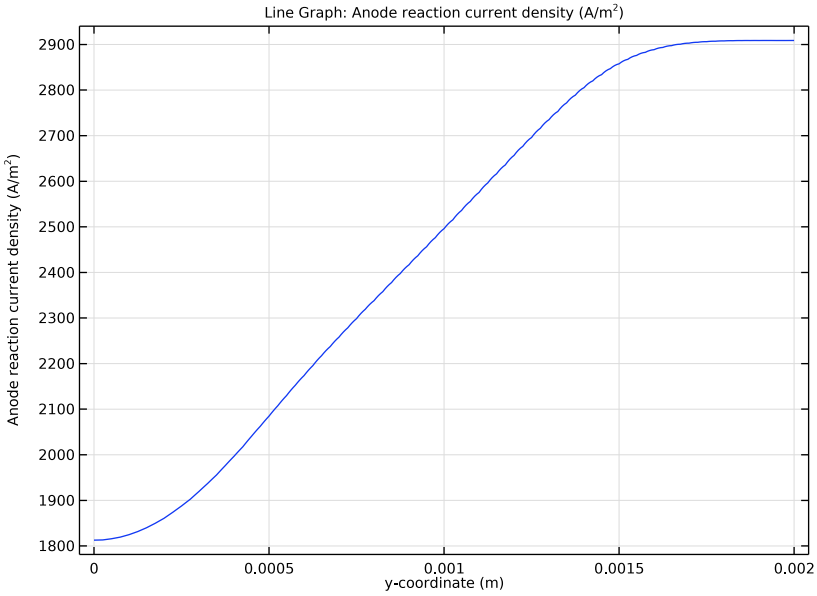

Figure 3: Current-density distribution at the active layer at the anode.

The current density is uneven with the highest density in the cell's upper region. This means that the oxygen-reduction reaction rate in the cathode determines the current-density distribution. The maximum current density arises close to the air inlet.

The convective fluxes generally dominate mass transport in the cell. To study the convective effects, plot the velocity field as in Figure 4.

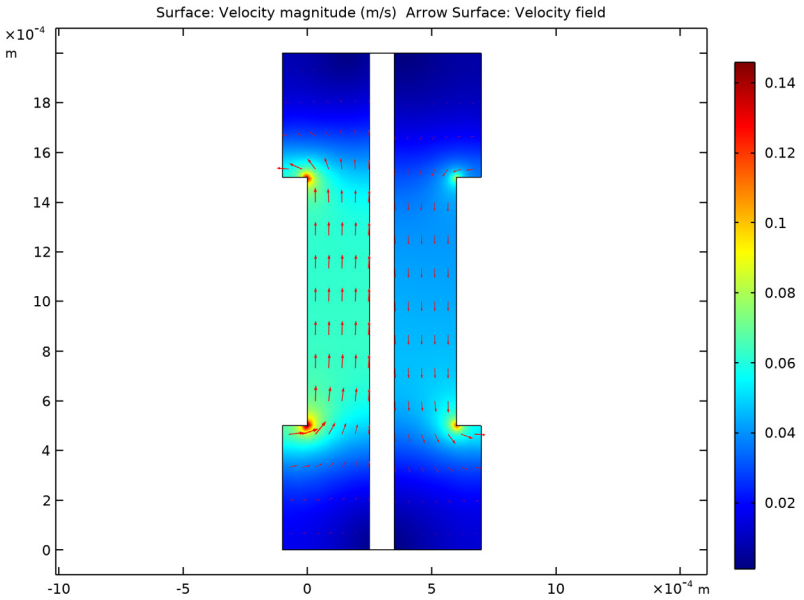

Figure 4: Gas velocity field in the anode and cathode compartments.

The flow-velocity magnitude attains its highest values at the current collector corners.

Figure 5 shows the reactant (oxygen and hydrogen) weight fractions in the cathode and anode gases. Surprisingly, the hydrogen fraction increases as the anode gas flows from the inlet (at the bottom) to the outlet (at the top). This is the result of the electro-osmotic drag of water through the membrane, which results in a higher flux than the consumption of hydrogen. This means that the resulting convective flux of anode gas toward the membrane causes the weight fraction of hydrogen to go up. In the cathode gas, there is an expected decrease in oxygen content along the flow direction.

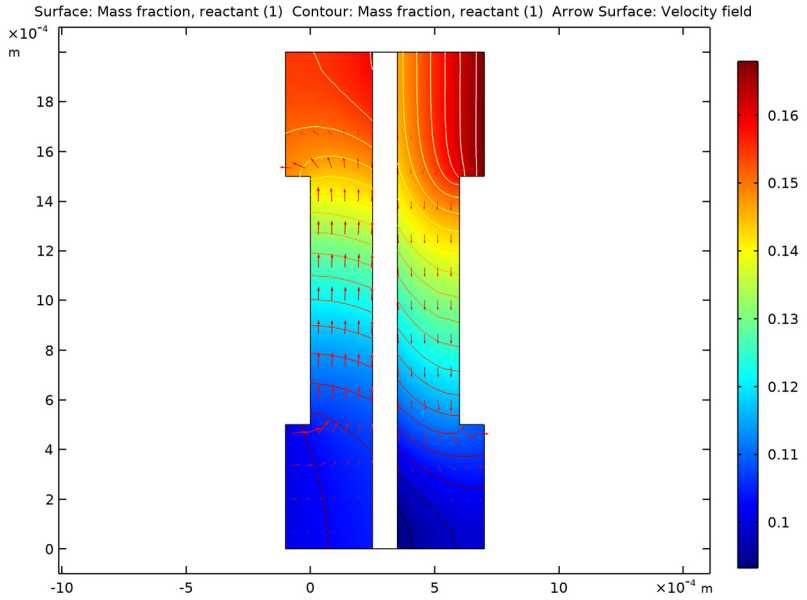

Figure 5: Reactant mass fractions, normalized by their inlet values, on the anode side (left) and cathode side (right). The reactant in the anode is hydrogen and that in the cathode is oxygen.

Although oxygen consumption is small, the concentration overvoltage in the agglomerates gives a substantial contribution to the concentration overvoltage. A small change in the oxygen flow gives a substantial change in cell polarization.

Figure 6 depicts the water mass fraction in the anode and cathode gases as well as the diffusive flux of water in the anode. It is apparent that water is transported through both diffusion and convection to the membrane on the anode side. The results show a minimum occurring in the upper corner of the membrane on the anode side. This is known to limit fuel cell performance. If the anode gas becomes too dry, the membrane dries out, resulting in decreasing ionic conductivity and the cell subsequently fails.

On the other hand, on the cathode side water levels increase with the direction of flow, and a local maximum in water current occurs in the lower corner to the membrane. This might also be critical because water droplets can clog the pores and effectively hinder gas transport to the active layer.

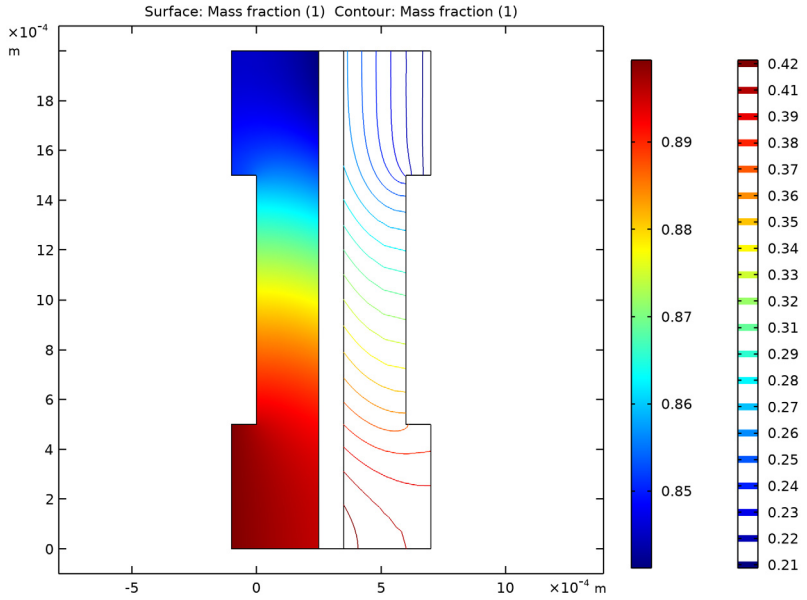

Figure 6: Water mass fraction in the anode (left, surface plot) and the cathode (right, contour plot).

References

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2. C. Marr and X. Li, "Composition and Performance Modelling of Catalyst Layer in a Proton Exchange Membrane Fuel Cell," *J. Power Sources*, vol. 77, pp. 17–27, 1999.

3. P. Futerko and I.-M. Hsing, "Two-Dimensional Finite Element Method Study of the Resistance of Membranes in Polymer Electrolyte Fuel Cells," *Electrochimica Acta*, vol. 45, pp. 1741–1751, 2000.

4. D.M. Bernardi and M.W. Verbrugge, "Mathematical Model of a Gas Diffusion Electrode Bonded to a Polymer Electrolyte," *AIChe J.*, vol. 37, pp. 1151–1163, 1991.

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6. R.B. Bird, W.E. Stewart, and E.N. Lightfoot, *Transport Phenomena*, John Wiley & Sons, 1960.

7. K. Broka and P. Ekdunge, "Modelling the PEM fuel cell cathode," *J. Appl. Electrochem.*, vol. 27, pp. 281–289, 1997.

8. K. Dannenberg, P. Ekdunge, and G. Lindbergh, "Mathematical model of the PEMFC", *J. Appl. Electrochem.*, vol. 30, pp. 1377–1387, 2000.

Application Library path: `Fuel_Cell_and_Electrolyzer_Module/Fuel_Cells/pem_gdl_species_transport_2d`

Modeling Instructions

From the **File** menu, choose **New**.

NEW

In the **New** window, click **Model Wizard**.

MODEL WIZARD

1. In the **Model Wizard** window, click **2D**.
2. In the **Select Physics** tree, select **Electrochemistry>Hydrogen Fuel Cells>Proton Exchange (fc)**.
3. Click **Add**.
4. Click **Study**.
5. In the **Select Study** tree, select **Preset Studies for Selected Physics Interfaces>Stationary with Initialization**.
6. Click **Done**.

GEOMETRY 1

Create the geometry using rectangles.

Rectangle 1 (r1)

1. In the **Geometry** toolbar, click **Rectangle**.
2. In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.
3. In the **Width** text field, type `2.5e-4`.

4 In the **Height** text field, type `2e-3`.

Rectangle 2 (r2)

1 In the **Geometry** toolbar, click  **Rectangle**.

2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.

3 In the **Width** text field, type `1e-4`.

4 In the **Height** text field, type `2e-3`.

5 Locate the **Position** section. In the **x** text field, type `2.5e-4`.

Rectangle 3 (r3)

1 In the **Geometry** toolbar, click  **Rectangle**.

2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.

3 In the **Width** text field, type `2.5e-4`.

4 In the **Height** text field, type `2e-3`.

5 Locate the **Position** section. In the **x** text field, type `3.5e-4`.

Rectangle 4 (r4)

1 In the **Geometry** toolbar, click  **Rectangle**.

2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.

3 In the **Width** text field, type `1e-4`.

4 In the **Height** text field, type `5e-4`.

5 Locate the **Position** section. In the **x** text field, type `-1e-4`.

Array 1 (arr1)

1 In the **Geometry** toolbar, click  **Transforms** and choose **Array**.

2 Select the object **r4** only.

3 In the **Settings** window for **Array**, locate the **Size** section.

4 In the **x size** text field, type `2`.

5 In the **y size** text field, type `2`.

6 Locate the **Displacement** section. In the **x** text field, type `7e-4`.

7 In the **y** text field, type `1.5e-3`.

Union 1 (uni1)

1 In the **Geometry** toolbar, click  **Booleans and Partitions** and choose **Union**.

2 Select the objects **arr1(1,1)**, **arr1(1,2)**, and **r1** only.

3 In the **Settings** window for **Union**, locate the **Union** section.

4 Clear the **Keep interior boundaries** check box.

Union 2 (uni2)

1 In the **Geometry** toolbar, click **Booleans and Partitions** and choose **Union**.

2 Select the objects **arr1(2,1)**, **arr1(2,2)**, and **r3** only.

3 In the **Settings** window for **Union**, locate the **Union** section.

4 Clear the **Keep interior boundaries** check box.

5 In the **Geometry** toolbar, click **Build All**.

GLOBAL DEFINITIONS

Proceed to load a set of global model parameters from a text file provided with the Application Library.

Parameters 1

1 In the **Model Builder** window, under **Global Definitions** click **Parameters 1**.

2 In the **Settings** window for **Parameters**, locate the **Parameters** section.

3 Click **Load from File**.

4 Browse to the model's Application Libraries folder and double-click the file `pem_gdl_species_transport_2d_parameters.txt`.

DEFINITIONS

Set up a number of selections on the geometry. These will be used later when setting up the physics.

Anode GDL

1 In the **Definitions** toolbar, click **Explicit**.

2 Select Domain 1 only.

3 Right-click **Explicit 1** and choose **Rename**.

4 In the **Rename Explicit** dialog box, type `Anode GDL` in the **New label** text field.

5 Click **OK**.

Membrane

1 In the **Definitions** toolbar, click **Explicit**.

2 Select Domain 2 only.

3 Right-click **Explicit 2** and choose **Rename**.

4 In the **Rename Explicit** dialog box, type `Membrane` in the **New label** text field.

5 Click **OK**.

Cathode GDL

1 In the **Definitions** toolbar, click **Explicit**.

2 Select Domain 3 only.

3 Right-click **Explicit 3** and choose **Rename**.

4 In the **Rename Explicit** dialog box, type `Cathode GDL` in the **New label** text field.

5 Click **OK**.

Anode GDE

1 In the **Definitions** toolbar, click **Explicit**.

2 In the **Settings** window for **Explicit**, locate the **Input Entities** section.

3 From the **Geometric entity level** list, choose **Boundary**.

4 Select Boundary 10 only.

5 Right-click **Explicit 4** and choose **Rename**.

6 In the **Rename Explicit** dialog box, type `Anode GDE` in the **New label** text field.

7 Click **OK**.

Cathode GDE

1 In the **Definitions** toolbar, click **Explicit**.

2 In the **Settings** window for **Explicit**, locate the **Input Entities** section.

3 From the **Geometric entity level** list, choose **Boundary**.

4 Select Boundary 13 only.

5 Right-click **Explicit 5** and choose **Rename**.

6 In the **Rename Explicit** dialog box, type `Cathode GDE` in the **New label** text field.

7 Click **OK**.

Anode GDL Variables

Define a number of domain- and boundary-specific variables. These will be used both for setting up the physics and in postprocessing.

1 In the **Definitions** toolbar, click **Local Variables**.

2 In the **Model Builder** window, right-click **Variables 1** and choose **Rename**.

3 In the **Rename Variables** dialog box, type `Anode GDL Variables` in the **New label** text field.

4 Click **OK**.

5 In the **Settings** window for **Variables**, locate the **Geometric Entity Selection** section.

6 From the **Geometric entity level** list, choose **Domain**.

7 From the **Selection** list, choose **Anode GDL**.

8 Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
wReact	fc.wH2		Mass fraction, reactant

Cathode GDL Variables

1 In the **Definitions** toolbar, click **Local Variables**.

2 Right-click **Variables 2** and choose **Rename**.

3 In the **Rename Variables** dialog box, type `Cathode GDL Variables` in the **New label** text field.

4 Click **OK**.

5 In the **Settings** window for **Variables**, locate the **Geometric Entity Selection** section.

6 From the **Geometric entity level** list, choose **Domain**.

7 From the **Selection** list, choose **Cathode GDL**.

8 Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
wReact	fc.wO2		Mass fraction, reactant

Anode GDE Variables

1 In the **Definitions** toolbar, click **Local Variables**.

2 In the **Model Builder** window, right-click **Variables 3** and choose **Rename**.

3 In the **Rename Variables** dialog box, type `Anode GDE Variables` in the **New label** text field.

4 Click **OK**.

5 In the **Settings** window for **Variables**, locate the **Geometric Entity Selection** section.

6 From the **Geometric entity level** list, choose **Boundary**.

7 From the **Selection** list, choose **Anode GDE**.

8 Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
cH2_agg	fc.p*fc.xH2/KH2		Henry's law hydrogen agglomerate concentration
eta_a	fc.phis-fc.phil-E_eq_a	V	Anodic overpotential
beta_a	cH2_agg-cH2_ref*exp(-2*F_const*eta_a/(R_const*T))		
lda_a	sqrt(i0_a*S*R_agg^2/(2*F_const*cH2_ref*D_agg))		Anodic current density subexpression
i_a	K*(1-lda_a*coth(lda_a))*beta_a*(R_agg/3)		Anode current density

Cathode GDE Variables

1 In the **Definitions** toolbar, click **Local Variables**.

2 Right-click **Variables 4** and choose **Rename**.

3 In the **Rename Variables** dialog box, type `Cathode GDE Variables` in the **New label** text field.

4 Click **OK**.

5 In the **Settings** window for **Variables**, locate the **Geometric Entity Selection** section.

6 From the **Geometric entity level** list, choose **Boundary**.

7 From the **Selection** list, choose **Cathode GDE**.

8 Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
cO2_agg	fc.p*fc.xO2/KO2		Henry's law oxygen agglomerate concentration
eta_c	fc.phis-fc.phil-E_eq_c	V	Cathodic overvoltage

Name	Expression	Unit	Description
lda_c	sqrt(i0_c*S*R_agg^2* exp(-F_const*eta_c/ (2*R_const*T))/(4* F_const*cO2_ref* D_agg))		Cathodic current density subexpression
i_c	-2*K*(1-lda_c* coth(lda_c))*cO2_agg* (R_agg/3)		Cathode current density

HYDROGEN FUEL CELL (FC)

Set up the current distribution and transport model. Include mass transport using Maxwell-Stefan diffusion and momentum transport using Darcy's Law in both the anode and cathode gas mixtures. Also, define the reference pressure level in the interface properties. Note that the default gas species are hydrogen and water on the anode side, and oxygen, nitrogen and water on the cathode side. Start with adding the relevant domain nodes.

1 In the **Settings** window for **Hydrogen Fuel Cell**, locate the **H2 Gas Mixture** section.

2 Find the **Transport mechanisms** subsection. Select the **Use Darcy's Law for momentum transport** check box.

3 Locate the **O2 Gas Mixture** section. Select the **Use Darcy's Law for momentum transport** check box.

4 Click to expand the **Reference Pressure Level** section. In the p_{ref} text field, type 0.

Membrane 1

1 Right-click **Component 1 (comp1)>Hydrogen Fuel Cell (fc)** and choose **Membrane**.

2 In the **Settings** window for **Membrane**, locate the **Domain Selection** section.

3 From the **Selection** list, choose **Membrane**.

H2 Gas Diffusion Layer 1

1 In the **Physics** toolbar, click **Domains** and choose **H2 Gas Diffusion Layer**.

2 In the **Settings** window for **H2 Gas Diffusion Layer**, locate the **Domain Selection** section.

3 From the **Selection** list, choose **Anode GDL**.

O2 Gas Diffusion Layer 1

1 In the **Physics** toolbar, click **Domains** and choose **O2 Gas Diffusion Layer**.

2 In the **Settings** window for **O2 Gas Diffusion Layer**, locate the **Domain Selection** section.

3 From the **Selection** list, choose **Cathode GDL**.

Thin H2 Gas Diffusion Electrode 1

1 In the **Physics** toolbar, click **Boundaries** and choose **Thin H2 Gas Diffusion Electrode**.

2 In the **Settings** window for **Thin H2 Gas Diffusion Electrode**, locate the **Boundary Selection** section.

3 From the **Selection** list, choose **Anode GDE**.

Thin O2 Gas Diffusion Electrode 1

1 In the **Physics** toolbar, click **Boundaries** and choose **Thin O2 Gas Diffusion Electrode**.

2 In the **Settings** window for **Thin O2 Gas Diffusion Electrode**, locate the **Boundary Selection** section.

3 From the **Selection** list, choose **Cathode GDE**.

Electrolyte Phase 1

Set up the electrolyte conductivity in the **Electrolyte Phase** node.

1 In the **Model Builder** window, click **Electrolyte Phase 1**.

2 In the **Settings** window for **Electrolyte Phase**, locate the **Electrolyte Charge Transport** section.

3 In the σ_l text field, type `kappa_m`.

Inspect the settings in the **H2 Gas Phase** and **O2 Gas Phase** nodes. Note that the density and viscosity of the gas mixture, and the binary diffusion coefficients are calculated automatically when the respective default settings are used.

H2 Gas Diffusion Layer 1

Set up the properties of the **H2 Gas Diffusion Layer** and **O2 Gas Diffusion Layer** nodes.

1 In the **Model Builder** window, click **H2 Gas Diffusion Layer 1**.

2 In the **Settings** window for **H2 Gas Diffusion Layer**, locate the **Electrode Charge Transport** section.

3 In the σ_s text field, type `kappa_s`.

4 Locate the **Gas Transport** section. In the ε_g text field, type `eps_mac`.

5 In the κ_g text field, type `kappa_p`.

O2 Gas Diffusion Layer 1

1 In the **Model Builder** window, click **O2 Gas Diffusion Layer 1**.

2 In the **Settings** window for **O2 Gas Diffusion Layer**, locate the **Electrode Charge Transport** section.

3 In the σ_s text field, type `kappa_s`.

4 Locate the **Gas Transport** section. In the ε_g text field, type `eps_mac`.

5 In the κ_g text field, type `kappa_p`.

Thin H2 Gas Diffusion Electrode 1

Set up the properties of the **Thin H2 Gas Diffusion Electrode** node. The details of electrode kinetics are set in the child node.

1 In the **Model Builder** window, click **Thin H2 Gas Diffusion Electrode 1**.

2 In the **Settings** window for **Thin H2 Gas Diffusion Electrode**, locate the **Electrode Thickness** section.

3 In the d_{gde} text field, type `l_act`.

Thin H2 Gas Diffusion Electrode Reaction 1

1 In the **Model Builder** window, expand the **Thin H2 Gas Diffusion Electrode 1** node, then click **Thin H2 Gas Diffusion Electrode Reaction 1**.

2 In the **Settings** window for **Thin H2 Gas Diffusion Electrode Reaction**, locate the **Stoichiometric Coefficients** section.

3 In the ν_{H2O} text field, type `2*drag`.

4 Locate the **Equilibrium Potential** section. From the E_{eq} list, choose **User defined**. Locate the **Electrode Kinetics** section. From the $i_{loc,expr}$ list, choose **User defined**. In the associated text field, type `i_a`.

5 Locate the **Active Specific Surface Area** section. In the a_v text field, type `Av`.

Thin O2 Gas Diffusion Electrode 1

Similarly, set up the properties of the **Thin O2 Gas Diffusion Electrode** node. The details of electrode kinetics are set in the child node.

1 In the **Model Builder** window, click **Thin O2 Gas Diffusion Electrode 1**.

2 In the **Settings** window for **Thin O2 Gas Diffusion Electrode**, locate the **Electrode Thickness** section.

3 In the d_{gde} text field, type `l_act`.

Thin O2 Gas Diffusion Electrode Reaction 1

1 In the **Model Builder** window, expand the **Thin O2 Gas Diffusion Electrode 1** node, then click **Thin O2 Gas Diffusion Electrode Reaction 1**.

2 In the **Settings** window for **Thin O2 Gas Diffusion Electrode Reaction**, locate the **Stoichiometric Coefficients** section.

3 In the ν_{H2O} text field, type `2+4*drag`.

4 Locate the **Equilibrium Potential** section. From the E_{eq} list, choose **User defined**. Locate the **Electrode Kinetics** section. From the $i_{loc,expr}$ list, choose **User defined**. In the associated text field, type `i_c`.

5 Locate the **Active Specific Surface Area** section. In the a_v text field, type `Av`.

Finally, set up the boundary conditions and initial values.

Electronic Conducting Phase 1

Set the initial value for electric potential in the cathode electrode to the cell potential. (The default zero initial values are used for both potentials in the rest of the geometry.)

1 In the **Model Builder** window, click **Electronic Conducting Phase 1**.

Initial Values, O2 Domains 1

1 In the **Physics** toolbar, click **Attributes** and choose **Initial Values, O2 Domains**.

2 Select Domain 3 only.

3 In the **Settings** window for **Initial Values, O2 Domains**, locate the **Initial Values** section.

4 In the ϕ_s text field, type `V_cell`.

Electronic Conducting Phase 1

In the **Model Builder** window, click **Electronic Conducting Phase 1**.

Electric Ground 1

1 In the **Physics** toolbar, click **Attributes** and choose **Electric Ground**.

2 Select Boundary 8 only.

Electronic Conducting Phase 1

In the **Model Builder** window, click **Electronic Conducting Phase 1**.

Electric Potential 1

1 In the **Physics** toolbar, click **Attributes** and choose **Electric Potential**.

2 Select Boundary 17 only.

3 In the **Settings** window for **Electric Potential**, locate the **Electric Potential** section.

4 In the $\phi_{s,bnd}$ text field, type `V_cell`.

H2 Gas Phase 1

In the **Model Builder** window, click **H2 Gas Phase 1**.

H2 Inlet 1

1 In the **Physics** toolbar, click **Attributes** and choose **H2 Inlet**.

2 Select Boundary 1 only.

3 In the **Settings** window for **H2 Inlet**, locate the **Mixture Specification** section.

4 In the $x_{0,\mathrm{H2O}}$ text field, type `xH2Oa_in`.

5 Locate the **Flow Boundary Condition** section. In the p_0 text field, type `p_a_in`.

H2 Gas Phase 1

In the **Model Builder** window, click **H2 Gas Phase 1**.

H2 Outlet 1

1 In the **Physics** toolbar, click **Attributes** and choose **H2 Outlet**.

2 Select Boundary 4 only.

3 In the **Settings** window for **H2 Outlet**, locate the **Outlet** section.

4 In the p_0 text field, type `p_ref`.

Initial Values 1

1 In the **Model Builder** window, click **Initial Values 1**.

2 In the **Settings** window for **Initial Values**, locate the **Initial Values** section.

3 In the $x_{0,\mathrm{H2O}}$ text field, type `xH2Oa_in`.

4 In the p_0 text field, type `p_ref`.

O2 Gas Phase 1

In the **Model Builder** window, click **O2 Gas Phase 1**.

O2 Inlet 1

1 In the **Physics** toolbar, click **Attributes** and choose **O2 Inlet**.

2 Select Boundary 22 only.

3 In the **Settings** window for **O2 Inlet**, locate the **Mixture Specification** section.

4 In the $x_{0,\mathrm{H2O}}$ text field, type `xH2Oc_in`.

5 In the $x_{0,\mathrm{N2}}$ text field, type `xN2_in`.

6 Locate the **Flow Boundary Condition** section. In the p_0 text field, type `p_c_in`.

O2 Gas Phase 1

In the **Model Builder** window, click **O2 Gas Phase 1**.

O2 Outlet 1

1 In the **Physics** toolbar, click **Attributes** and choose **O2 Outlet**.

2 Select Boundary 21 only.

3 In the **Settings** window for **O2 Outlet**, locate the **Outlet** section.

4 In the p_0 text field, type `p_ref`.

Initial Values 1

1 In the **Model Builder** window, click **Initial Values 1**.

2 In the **Settings** window for **Initial Values**, locate the **Initial Values** section.

3 In the $x_{0,\mathrm{H2O}}$ text field, type `xH2Oc_in`.

4 In the $x_{0,\mathrm{N2}}$ text field, type `xN2_in`.

5 In the p_0 text field, type `p_ref`.

GLOBAL DEFINITIONS

Default Model Inputs

Since we will be using the same temperature everywhere in the model, we will define the temperature only once in the **Default Model Inputs** node. This node may be accessed by multiple physics nodes.

1 In the **Model Builder** window, under **Global Definitions** click **Default Model Inputs**.

2 In the **Settings** window for **Default Model Inputs**, locate the **Browse Model Inputs** section.

3 In the tree, select **General>Temperature (K) - minput.T**.

4 Find the **Expression for remaining selection** subsection. In the **Temperature** text field, type `T`.

MESH 1

Steep gradients are expected close to the electrodes and at the corner points where the ribs of the flow plates are suppressed into the GDL. Create a mesh with finer resolution at these parts of the geometry.

Size 1

1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Mesh 1** and choose **Size**.

2 In the **Settings** window for **Size**, locate the **Geometric Entity Selection** section.

3 From the **Geometric entity level** list, choose **Boundary**.

4 Select Boundaries 10 and 13 only.

5 Locate the **Element Size** section. Click the **Custom** button.

6 Locate the **Element Size Parameters** section. Select the **Maximum element size** check box.

7 In the associated text field, type `2.5e-5`.

Size 2

1 In the **Model Builder** window, right-click **Mesh 1** and choose **Size**.

2 In the **Settings** window for **Size**, locate the **Geometric Entity Selection** section.

3 From the **Geometric entity level** list, choose **Point**.

4 Select Points 6, 7, 14, and 15 only.

5 Locate the **Element Size** section. Click the **Custom** button.

6 Locate the **Element Size Parameters** section. Select the **Maximum element size** check box.

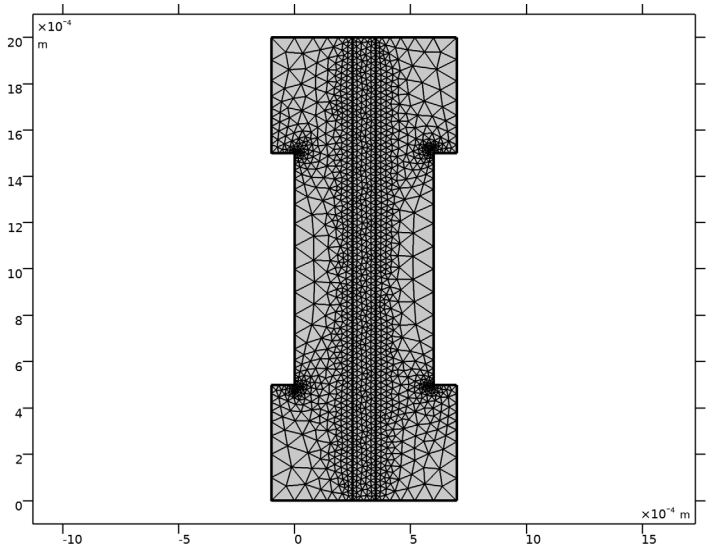
7 In the associated text field, type `1e-5`.

Free Triangular 1

1 In the **Mesh** toolbar, click  **Free Triangular**.

2 Right-click **Mesh 1** and choose **Build All**.

The finalized mesh should now look as follows:



STUDY 1

The problem is now ready for solving. In the first step, solve for secondary current distribution initialization.

Step 1: Current Distribution Initialization

1 In the **Model Builder** window, under **Study 1** click **Step 1: Current Distribution Initialization**.

2 In the **Settings** window for **Current Distribution Initialization**, locate the **Study Settings** section.

3 From the **Current distribution type** list, choose **Secondary**.

4 In the **Home** toolbar, click **Compute**.

RESULTS

The following steps reproduce the figures found in the Results and Discussion section.

GDL Current Density Distribution

1 In the **Home** toolbar, click **Add Plot Group** and choose **2D Plot Group**.

2 In the **Settings** window for **2D Plot Group**, type `GDL Current Density Distribution` in the **Label** text field.

Surface 1

1 Right-click **GDL Current Density Distribution** and choose **Surface**.

2 In the **Settings** window for **Surface**, click **Replace Expression** in the upper-right corner of the **Expression** section. From the menu, choose **Component 1 (comp1)> Hydrogen Fuel Cell>fc.IsMag - Electrode current density magnitude - A/m²**.

3 Click to expand the **Range** section. Select the **Manual color range** check box.

4 In the **Maximum** text field, type `1e4`.

Arrow Surface 1

1 In the **Model Builder** window, right-click **GDL Current Density Distribution** and choose **Arrow Surface**.

2 In the **Settings** window for **Arrow Surface**, click **Replace Expression** in the upper-right corner of the **Expression** section. From the menu, choose **Component 1 (comp1)> Hydrogen Fuel Cell>fc.Isx,fc.Isy - Electrode current density vector**.

3 In the **GDL Current Density Distribution** toolbar, click **Plot**.

4 Click the **Zoom Extents** button in the **Graphics** toolbar.

Anode Reaction Current Density

1 In the **Home** toolbar, click **Add Plot Group** and choose **1D Plot Group**.

2 In the **Settings** window for **1D Plot Group**, type `Anode Reaction Current Density` in the **Label** text field.

Line Graph 1

1 Right-click **Anode Reaction Current Density** and choose **Line Graph**.

2 In the **Settings** window for **Line Graph**, locate the **Selection** section.

3 From the **Selection** list, choose **Anode GDE**.

4 Click **Replace Expression** in the upper-right corner of the **y-Axis Data** section. From the menu, choose **Component 1 (comp1)>Definitions>Variables>i_a - Anode current density - A/m²**.

5 Locate the **y-Axis Data** section. In the **Expression** text field, type `i_a*Av*l_act`.

6 Select the **Description** check box.

7 In the associated text field, type `Anode reaction current density`.

8 Click **Replace Expression** in the upper-right corner of the **x-Axis Data** section. From the menu, choose **Component 1 (comp1)>Geometry>Coordinate>y - y-coordinate**.

9 In the **Anode Reaction Current Density** toolbar, click **Plot**.

10 Click the **Zoom Extents** button in the **Graphics** toolbar.

Velocity Field

1 In the **Home** toolbar, click **Add Plot Group** and choose **2D Plot Group**.

2 In the **Settings** window for **2D Plot Group**, type `Velocity Field` in the **Label** text field.

Surface 1

1 Right-click **Velocity Field** and choose **Surface**.

2 In the **Settings** window for **Surface**, click **Replace Expression** in the upper-right corner of the **Expression** section. From the menu, choose **Component 1 (comp1)> Hydrogen Fuel Cell>fc.U - Velocity magnitude - m/s**.

Arrow Surface 1

1 In the **Model Builder** window, right-click **Velocity Field** and choose **Arrow Surface**.

2 In the **Settings** window for **Arrow Surface**, click **Replace Expression** in the upper-right corner of the **Expression** section. From the menu, choose **Component 1 (comp1)> Hydrogen Fuel Cell>fc.u,fc.v - Velocity field**.

3 In the **Velocity Field** toolbar, click **Plot**.

4 Click the **Zoom Extents** button in the **Graphics** toolbar.

Reactant Mass Fraction

1 In the **Home** toolbar, click **Add Plot Group** and choose **2D Plot Group**.

2 In the **Settings** window for **2D Plot Group**, type `Reactant Mass Fraction` in the **Label** text field.

Surface 1

1 Right-click **Reactant Mass Fraction** and choose **Surface**.

2 In the **Settings** window for **Surface**, locate the **Expression** section.

3 In the **Expression** text field, type `wReact`.

Contour 1

1 In the **Model Builder** window, right-click **Reactant Mass Fraction** and choose **Contour**.

2 In the **Settings** window for **Contour**, locate the **Expression** section.

3 In the **Expression** text field, type `wReact`.

4 Locate the **Coloring and Style** section. From the **Color table** list, choose **Thermal**.

5 Clear the **Color legend** check box.

Arrow Surface 1

1 Right-click **Reactant Mass Fraction** and choose **Arrow Surface**.

2 In the **Settings** window for **Arrow Surface**, click **Replace Expression** in the upper-right corner of the **Expression** section. From the menu, choose **Component 1 (comp1)> Hydrogen Fuel Cell>fc.u,fc.v - Velocity field**.

3 In the **Reactant Mass Fraction** toolbar, click **Plot**.

4 Click the **Zoom Extents** button in the **Graphics** toolbar.

Water Mass Fraction

1 In the **Home** toolbar, click **Add Plot Group** and choose **2D Plot Group**.

2 In the **Settings** window for **2D Plot Group**, type `Water Mass Fraction` in the **Label** text field.

Surface 1

1 Right-click **Water Mass Fraction** and choose **Surface**.

2 In the **Settings** window for **Surface**, locate the **Expression** section.

3 In the **Expression** text field, type `fc.wH2O_H2`.

Contour 1

1 In the **Model Builder** window, right-click **Water Mass Fraction** and choose **Contour**.

2 In the **Settings** window for **Contour**, locate the **Expression** section.

3 In the **Expression** text field, type `fc.wH2O_O2`.

4 In the **Water Mass Fraction** toolbar, click **Plot**.

5 Click the **Zoom Extents** button in the **Graphics** toolbar.