

# Flow of Viscoelastic Fluid Past a Cylinder

# Introduction

Many complex fluids of interest exhibit a combination of viscous and elastic behavior under strain. Examples of such fluids are polymer solutions and melts, oil, toothpaste, and clay, among many others. The Oldroyd-B fluid presents one of the simplest constitutive models capable of describing the viscoelastic behavior of dilute polymeric solutions under general flow conditions. Despite the apparent simplicity of the constitutive relation, the dynamics that arise in many flows are complicated enough to present a considerable challenge to numerical simulations.

# Model Definition

This example studies a flow of Oldroyd-B fluid past a cylinder between two parallel plates. The flow is considered as being two-dimensional (2D). The aspect ratio of the cylinder radius to the to the channel half-width is 1/2.

The fluid is a dilute solution of polymer in a Newtonian liquid solvent of viscosity  $\mu_s$ . The total stress is presented as

$$\sigma = -p\mathbf{I} + 2\mu_{s}\mathbf{S}(\mathbf{u}) + \mathbf{T}_{\rho}$$

where  $\mathbf{u} = (u, v)$  is the flow velocity vector, p is the pressure, and

$$\mathbf{S}(\mathbf{u}) = \frac{1}{2} [\nabla \mathbf{u} + (\nabla \mathbf{u})^T]$$

is the strain rate. The extra stress contribution due to the polymer is given by the following Oldroyd-B constitutive relation:

$$\mathbf{T}_{e} + \lambda \mathbf{T}_{e}^{\nabla} = 2\mu_{p} \mathbf{S}(\mathbf{u})$$
(1)

where the upper convective derivative operator is defined as

The polymer is characterized by two physical parameters: the viscosity  $\mu_p$  and the relaxation time  $\lambda$ .

# NONDIMENSIONAL FORMULATION

The Weissenberg number is defined as:

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Wi = 
$$\lambda \frac{U_{\text{in}}}{R}$$

where  $U_{in}$  is the average fluid velocity at the inlet, R is the radius of the cylinder, and  $\lambda$  is the polymer relaxation time.

A zero Weissenberg number gives a pure viscous fluid (no elasticity), while the infinite Weissenberg number limit corresponds to purely elastic response. Due to the convective nature of the constitutive relation, solution stability is lost with increasing fluid elasticity. In practice, already values Wi > 1 are considered as a high for many flows of an Oldroyd-B fluid.

The flow is stationary, and the problem becomes dimensionless by using R,  $U_{in}$ , and the total viscosity  $\mu = \mu_s + \mu_p$ . The Reynolds number is defined as

$$Re = \frac{R\mu U_{in}}{\rho}$$
(2)

#### **BOUNDARY CONDITIONS**

Because of the flow symmetry, it is sufficient to model only the upper halves of the channel and the cylinder. At the channel centerline, use the symmetry conditions of zero normal flow and zero total tangential stress. At the channel walls and the cylinder surface, the model uses no slip boundary conditions. At the inlet, the fully developed parabolic velocity profile and the corresponding extra stresses components are specified:

$$u = \frac{3}{2}(1 - y^2)$$
$$T_{11} = 2\mu_p \operatorname{Wi}\left(\frac{\partial u}{\partial y}\right)^2$$
$$T_{12} = \mu_p \frac{\partial u}{\partial y}$$
$$T_{22} = 0$$

At the outlet, use the pressure boundary condition for developed flow; the only stress acting at the boundary is due to the pressure force  $p_{out}$ :

$$\sigma \cdot \mathbf{n} = -p_{out}\mathbf{n}$$

The analysis gradually increases the Weissenberg number from 0 to 1 using the parametric solver. Figure 1 and Figure 2 show the flow field and stress distribution for the value Wi = 0.7. Figure 3 shows the drag coefficient as a function of the Weissenberg number. The result is in good agreement with the experimental and simulation results presented in Ref. 2.



Figure 1: Flow field near cylinder and stress distribution for Wi = 0.7.



Figure 2: Stress distribution along the cylinder surface and wake centerline for Wi = 0.7.



Figure 3: Drag on the cylinder.

# References

1. T.J. Craven, J.M. Rees, and W.B. Zimmerman, "Stabilized finite element modelling of Oldroyd-B viscoelastic flow," *COMSOL Conference 2006*, Birmingham, U.K., 2006.

2. M.A. Alves, F.T. Pinho, and P.J. Oliveira, "The flow of viscoelastic fluids past a cylinder: finite-volume high-resolution methods," *J. Non-Newtonian Fluid Mech.*, vol. 97, pp. 207–232, 2001.

Application Library path: CFD\_Module/Single-Phase\_Flow/ cylinder\_flow\_viscoelastic

# Modeling Instructions

From the File menu, choose New.

#### NEW

In the New window, click 🔗 Model Wizard.

#### MODEL WIZARD

- I In the Model Wizard window, click **2D**.
- 2 In the Select Physics tree, select Fluid Flow>Single-Phase Flow>Viscoelastic Flow (vef).
- 3 Click Add.
- 4 Click 🔿 Study.
- 5 In the Select Study tree, select General Studies>Stationary.
- 6 Click 🗹 Done.

# ROOT

- I In the Model Builder window, click the root node.
- 2 In the root node's Settings window, locate the Unit System section.
- **3** From the **Unit system** list, choose **None**.

The equations you will solve are formulated in dimensionless form.

#### GEOMETRY I

Rectangle 1 (r1)

- I In the **Geometry** toolbar, click **Rectangle**.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 25.
- 4 In the **Height** text field, type 2.
- 5 Locate the Position section. In the x text field, type -10.
- 6 Click 틤 Build Selected.

Rectangle 2 (r2)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 6.
- **4** In the **Height** text field, type **2**.
- 5 Locate the **Position** section. In the **x** text field, type -2.
- 6 Click 틤 Build Selected.

Circle 1 (c1)

- I In the **Geometry** toolbar, click  $\bigcirc$  **Circle**.
- 2 In the Settings window for Circle, click 📳 Build Selected.

## Difference I (dif1)

- I In the Geometry toolbar, click i Booleans and Partitions and choose Difference.
- 2 Select the objects rI and r2 only.
- 3 In the Settings window for Difference, locate the Difference section.
- **4** Find the **Objects to subtract** subsection. Select the **Delta Activate Selection** toggle button.
- **5** Select the object **cl** only.
- 6 Click 틤 Build Selected.

#### **GLOBAL DEFINITIONS**

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.

Name	Expression	Value	Description	
Re	1e-3	0.001	Reynolds number	
Wi	0.05	0.05	Weissenberg number	
mu_s	0.59	0.59	Solvent relative viscosity	
mu_p	1-mu_s	0.41	Polymer relative viscosity	

**3** In the table, enter the following settings:

## **VISCOELASTIC FLOW (VEF)**

Fluid Properties 1

- I In the Model Builder window, under Component I (compl)>Viscoelastic Flow (vef) click Fluid Properties I.
- 2 In the Settings window for Fluid Properties, locate the Fluid Properties section.
- **3** From the  $\rho$  list, choose **User defined**. In the associated text field, type Re.
- **4** Find the **Constitutive relation** subsection. From the μ<sub>s</sub> list, choose **User defined**. In the associated text field, type mu\_s.
- **5** In the table, enter the following settings:

Branch	Viscosity	Relaxation time
I	mu_p	Wi

Inlet 1

- I In the Physics toolbar, click Boundaries and choose Inlet.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Inlet, locate the Velocity section.
- 4 Click the Velocity field button.
- **5** Specify the **u**<sub>0</sub> vector as

1.5\*(1-(y/2)^2) x 0 y

- 6 Locate the Viscoelastic Stress section. From the list, choose Symmetric.
- 7 In the  $T_{e0}$  table, enter the following settings:

2*Wi*mu_p*uy^2	mu_p*uy	0
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mu_p*uy	0	0
0	0	0

Outlet I

- I In the Physics toolbar, click Boundaries and choose Outlet.
- **2** Select Boundary 11 only.
- 3 In the Settings window for Outlet, locate the Pressure Conditions section.
- 4 Clear the Suppress backflow check box.

Symmetry I

- I In the Physics toolbar, click Boundaries and choose Symmetry.
- **2** Click the  $\longleftrightarrow$  **Zoom Extents** button in the **Graphics** toolbar.
- **3** Select Boundaries 2, 5, 7, and 9 only.

Proceed to set up boundary probe to compute the drag coefficient.

# DEFINITIONS

Boundary Probe 1 (bnd1)

- I In the Definitions toolbar, click probes and choose Boundary Probe.
- 2 In the Settings window for Boundary Probe, locate the Probe Type section.
- 3 From the Type list, choose Integral.
- 4 Locate the Source Selection section. Click Clear Selection.
- **5** Select Boundaries 12 and 13 only.
- 6 In the Variable name text field, type Cd.
- 7 Locate the Expression section. In the Expression text field, type -2\*(vef.T\_stressx).
- 8 Select the **Description** check box.
- 9 In the associated text field, type Cd.

#### MESH I

Size

In the Model Builder window, under Component I (comp1) right-click Mesh I and choose Edit Physics-Induced Sequence.

Size 1

- I Select Boundaries 5, 7, 12, and 13 only.
- 2 In the Settings window for Size, locate the Element Size section.

- 3 From the Predefined list, choose Extra fine.
- 4 Click 🖷 Build Selected.

#### Mapped I

- I In the Mesh toolbar, click Mapped.
- 2 In the Settings window for Mapped, locate the Domain Selection section.
- 3 From the Geometric entity level list, choose Domain.
- 4 Select Domains 1 and 3 only.

#### Distribution I

- I Right-click Mapped I and choose Distribution.
- **2** Select Boundaries 2 and 3 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the **Distribution type** list, choose **Predefined**.
- 5 In the Number of elements text field, type 20.
- 6 In the **Element ratio** text field, type 5.
- 7 Click 📄 Build Selected.

#### Distribution 2

- I In the Model Builder window, right-click Mapped I and choose Distribution.
- **2** Select Boundaries 9 and 10 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 25.
- 6 In the **Element ratio** text field, type 5.
- 7 Select the **Reverse direction** check box.
- 8 Click 📗 Build All.

## STUDY I

#### Step 1: Stationary

- I In the Model Builder window, under Study I click Step I: Stationary.
- 2 In the Settings window for Stationary, click to expand the Study Extensions section.
- **3** Select the **Auxiliary sweep** check box.
- 4 Click + Add.

5 From the list in the Parameter name column, choose Wi (Weissenberg number).

- 6 Click Range.
- 7 In the Range dialog box, type 0 in the Start text field.
- 8 In the **Stop** text field, type 1.
- 9 In the **Step** text field, type 0.05.

IO Click Replace.

II In the Settings window for Stationary, locate the Study Extensions section.

12 From the Run continuation for list, choose No parameter.

**I3** From the **Reuse solution from previous step** list, choose **Yes**.

**I4** In the **Home** toolbar, click **= Compute**.

# RESULTS

#### Velocity (vef)

To monitor the variation of the drag on the cylinder due to the flow, click on the **Probe Plot** tab once it becomes available.

Once the solution is complete, the plot of the flow field appears. Adjust the view to magnify the region around the cylinder, then add a contour plot for the extra stresses. Follow these steps:

#### DEFINITIONS

# View I

- I In the Model Builder window, under Component I (compl)>Definitions click View I.
- 2 In the Settings window for View, locate the View section.
- **3** Select the **Lock axis** check box.

#### Axis

- I In the Model Builder window, expand the View I node, then click Axis.
- 2 In the Settings window for Axis, locate the Axis section.
- **3** In the **x minimum** text field, type -2.
- 4 In the **x maximum** text field, type 6.
- 5 In the **y minimum** text field, type -4.
- 6 In the **y maximum** text field, type 4.

#### RESULTS

#### Velocity (vef)

- I In the Model Builder window, under Results click Velocity (vef).
- 2 In the Settings window for 2D Plot Group, locate the Plot Settings section.
- 3 From the View list, choose View I.
- 4 Locate the Data section. From the Parameter value (Wi) list, choose 0.7.
- 5 Locate the Plot Settings section. Clear the Plot dataset edges check box.

#### Contour I

- I Right-click Velocity (vef) and choose Contour.
- 2 In the Settings window for Contour, click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Component I (comp1)>Viscoelastic Flow> Viscoelastic variables>Viscoelastic extra stress tensor, branch I kg/(m·s²)>vef.Te\_1xx Viscoelastic extra stress tensor, branch I, xx component.
- 3 Locate the Levels section. In the Total levels text field, type 40.
- 4 Locate the Coloring and Style section. From the Color table list, choose GrayScale.
- 5 In the Velocity (vef) toolbar, click **O** Plot.

You should now obtain the plot shown in Figure 1.

To plot the stress variation along the cylinder surface and in the wake, follow these steps:

#### ID Plot Group 4

In the Home toolbar, click 📠 Add Plot Group and choose ID Plot Group.

#### Line Graph I

- I Right-click ID Plot Group 4 and choose Line Graph.
- **2** Select Boundaries 7, 12, and 13 only.
- In the Settings window for Line Graph, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>
  Viscoelastic Flow>Viscoelastic variables>Viscoelastic extra stress tensor, branch I kg/ (m·s²)>vef.Te\_lxx Viscoelastic extra stress tensor, branch I, xx component.
- **4** In the **ID Plot Group 4** toolbar, click **ID Plot**.

#### ID Plot Group 4

- I In the Model Builder window, click ID Plot Group 4.
- 2 In the Settings window for ID Plot Group, locate the Data section.
- **3** From the **Parameter selection (Wi)** list, choose **From list**.

- 4 In the Parameter values (Wi) list, select 0.7.
- 5 Locate the Axis section. Select the Manual axis limits check box.
- 6 In the **x minimum** text field, type 0.
- 7 In the **x maximum** text field, type 6.
- 8 In the **y minimum** text field, type -5.
- 9 In the y maximum text field, type 115.
- **IO** In the **ID Plot Group 4** toolbar, click **ID Plot**.

This will produce the stress plot shown in Figure 2.

Finally, check the complete probe plot of the drag coefficient and compare it to that shown in Figure 3.

### Drag coefficient

- I In the Model Builder window, right-click Probe Plot Group 3 and choose Rename.
- 2 In the Rename ID Plot Group dialog box, type Drag coefficient in the New label text field.
- 3 Click OK.

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