

Stefan Tube

Introduction

This example illustrates the use of the Maxwell-Stefan diffusion model available with the Transport of Concentrated Species interface. It models multicomponent gas-phase diffusion in a Stefan tube in 1D. In this case, it is a liquid mixture of acetone and methanol that evaporates into air.

The concentration profiles are modeled at steady-state and validated against experimental data by Taylor and Krishna (Ref. 6).

Model Definition

The Stefan tube, shown in Figure 1, is a simple device used for measuring diffusion coefficients in binary vapors.



Figure 1: Schematic diagram of a Stefan tube.

At the bottom of the tube is a pool of mixture. The vapor that evaporates from this pool diffuses to the top of the tube, where a stream of air, flowing across the top of the tube, keeps the mole fraction of diffusing vapor there to be zero. The mole fraction of vapor above the liquid interface is at equilibrium. Because there is no horizontal flux inside the tube, you can analyze the problem using a 1D model geometry representing the distance between the liquid mixture surface and the top of the tube. The system composition of acetone, methanol, and air has been extensively investigated; both diffusion coefficients and composition have been measured at various positions within Stefan tubes. This makes it an ideal system for this model.

As a comparison, one experiment measured the mole fraction at the liquid interface to be $x_{Ac} = 0.319$ and $x_{Me} = 0.528$ where the pressure, p, was 99.4 kPa and the temperature, T, was 328.5 K. The length of the diffusion path was 0.238 m. The respective Maxwell-Stefan diffusion coefficients, D_{ij} , of the three binary pairs were calculated and are used in the model according to Table 1.

COMPONENT	LABEL	D_{ij}	VALUE
Acetone	I	D_{12}	8.48·10 ⁻⁶ m ² /s
Methanol	2	D_{13}	13.72·10 ⁻⁶ m ² /s
Air	3	D_{23}	19.91·10 ⁻⁶ m ² /s

TABLE I: LABELS AND MAXWELL-STEFAN DIFFUSION COEFFICIENTS

To model this problem, use the Transport of Concentrated Species interface with the Maxwell-Stefan diffusion model. It solves for the fluxes in terms of mass fractions for two of the three components. The mass fraction, ω , of the third is given by the two other ones. The three equations are:

$$\nabla \cdot \left[-\rho \omega_1 \sum_k [D_{1k} (\nabla x_k + (x_k - \omega_k)((\nabla p)/p))] + D^T ((\nabla T)/T) \right] = R - (\rho \mathbf{u} \cdot \nabla \omega_1)$$
$$\nabla \cdot \left[-\rho \omega_{2(1)} \sum_k [D_{2k} (\nabla x_k + (x_k - \omega_k)((\nabla p)/p))] + D^T ((\nabla T)/T) \right] = R - (\rho \mathbf{u} \cdot \nabla \omega_2)$$
$$\omega_3 = 1 - \omega_1 - \omega_2$$

where *D* is the diffusion coefficient (SI unit: m^2/s), *p* is the pressure (SI unit: Pa), *T* is the temperature (SI unit: K), **u** is the velocity (SI unit: m/s), *x* and ω are mole and mass fractions, respectively, and the mixture density, ρ_{mix} (SI unit: kg/m³), is a function of the average mixture mole fraction, M_{mix} (SI unit: kg/mol), according to Equation 2:

$$M_{\rm mix} = \sum_{i} x_i M_i \tag{1}$$

$$\rho_{\rm mix} = \frac{p}{RT} M_{\rm mix} \tag{2}$$

In this case, there is no imposed fluid velocity. However, there will appear a fluid velocity due to the diffusive fluxes. At the top of the tube the mass fractions are fixed, with the fraction of air being unity. At the bottom (at the liquid interface), the fractions are also fixed according to the previously mentioned experimental conditions. The fact that there is no air flux at the interface results in the following relation for the convective velocity, at steady state:

$$u = \frac{n_{\text{diff},3}}{\omega_3 \rho}$$

where $n_{\text{diff},3}$ is the diffusive mass flux of air (SI unit: kg/(m²·s)).

Results

Both the modeled and experimental steady-state mole fractions as a function of position are shown in Figure 2.



Figure 2: Modeled and experimental (Ref. 6) steady-state mole fractions of: acetone, methanol, and air, in the Stefan tube.

We can see that the model reproduces the results from Ref. 6 well, which means the Maxwell-Stefan equations can describe the mass transport process in the system accurately.

The Maxwell-Stefan diffusion formulation includes the conservation of mass. In the absence of chemical reactions (source terms) and convective contributions, the Maxwell-Stefan formulation results in zero net mass flux. In this example, the convective term is included, which you can see in the velocity profile in Figure 3.



Figure 3: Velocity of the gas mixture in the Stefan tube.

References

1. C.F. Curtiss and R.B. Bird, "Multicomponent diffusion," *Ind. Eng. Chem. Res.*, vol. 38, p. 2515, 1999.

2. R.B. Bird, W. Stewart, and E. Lightfoot, *Transport Phenomena*, John Wiley & Sons, New York, 1960.

3. G.A.J. Jaumann, Wien. Akad. Sitzungsberichte (Math.-Naturw. Klasse), vol. 120, p. 385, 1911.

4. J.O. Hirschfelder, C.F. Curtiss, and R.B. Bird, *Molecular Theory of Gases and Liquids*, Wiley, USA, 1954.

5. E.N. Fuller, P.D. Schettler, and J.C. Giddings, Ind. Eng. Chem., vol. 58, p. 19, 1966.

6. R. Taylor and R. Krishna, *Multicomponent Mass Transfer*, John Wiley & Sons, NY, p. 21, 1993.

Application Library path: Chemical_Reaction_Engineering_Module/ Mixing_and_Separation/stefan_tube

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click ID.
- 2 In the Select Physics tree, select Chemical Species Transport> Transport of Concentrated Species (tcs).
- 3 Click Add.
- 4 Click Add Mass Fraction.
- 5 In the Mass fractions table, enter the following settings:
- w1

w2

wЗ

- 6 Click Study.
- 7 In the Select Study tree, select Preset Studies>Stationary.
- 8 Click Done.

GEOMETRY I

Interval 1 (i1)

- I On the Geometry toolbar, click Interval.
- 2 In the Settings window for Interval, locate the Interval section.
- 3 In the **Right endpoint** text field, type 0.238.
- 4 Click Build All Objects.

GLOBAL DEFINITIONS

Next, add a set of model parameters by importing their definitions from a data text file provided with the **Application Library**.

Parameters

- I On the Home toolbar, click Parameters.
- 2 In the Settings window for Parameters, locate the Parameters section.
- **3** Click Load from File.
- **4** Browse to the model's Application Libraries folder and double-click the file stefan_tube_parameters.txt.

TRANSPORT OF CONCENTRATED SPECIES (TCS)

- I In the Model Builder window, under Component I (compl) click Transport of Concentrated Species (tcs).
- 2 In the Settings window for Transport of Concentrated Species, locate the Transport Mechanisms section.
- 3 From the Diffusion model list, choose Maxwell-Stefan.
- 4 Locate the Species section. From the From mass constraint list, choose w3.
- **5** In the **Model Builder** window's toolbar, click the **Show** button and select **Discretization** in the menu.
- 6 Click to expand the Discretization section. From the Mass fraction list, choose Quadratic.

Transport Properties 1

- I In the Model Builder window, expand the Transport of Concentrated Species (tcs) node, then click Transport Properties I.
- 2 In the Settings window for Transport Properties, locate the Model Input section.
- **3** In the T text field, type TO.
- **4** In the p_A text field, type p0.
- 5 Locate the Convection section. Specify the u vector as

-tcs.dflux_w3x/(w3*tcs.rho) x

- **6** Locate the **Density** section. In the M_{w1} text field, type M_ace.
- 7 In the M_{w2} text field, type M_met.
- **8** In the $M_{\rm w3}$ text field, type M_air.

9 Locate the **Diffusion** section. In the D_{ik} table, enter the following settings:

1	D12	D13
D12	1	D23
D13	D23	1

Initial Values 1

I	In the Model Builder window, under Component I (compl)>	
	Transport of Concentrated Species (tcs) click Initial Values I.	

- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the $\omega_{0,w1}$ text field, type w_ace0.
- **4** In the $\omega_{0,w2}$ text field, type w_met0.

Mass Fraction 1

- I On the Physics toolbar, click Boundaries and choose Mass Fraction.
- **2** Select Boundary 1 only.
- 3 In the Settings window for Mass Fraction, locate the Mass Fraction section.
- 4 Select the Species wI check box.
- **5** In the $\omega_{0,w1}$ text field, type w_ace0.
- 6 Select the **Species w2** check box.
- 7 In the $\omega_{0,w2}$ text field, type w_met0.

Mass Fraction 2

- I On the Physics toolbar, click Boundaries and choose Mass Fraction.
- **2** Select Boundary 2 only.
- 3 In the Settings window for Mass Fraction, locate the Mass Fraction section.
- 4 Select the **Species w1** check box.
- 5 Select the Species w2 check box.

MESH I

- I In the Model Builder window, under Component I (compl) click Mesh I.
- 2 In the Settings window for Mesh, locate the Mesh Settings section.
- **3** From the **Element size** list, choose **Extra fine**.
- 4 Click Build All.

STUDY I

On the Home toolbar, click Compute.

RESULTS

Table I

I On the **Results** toolbar, click **Table**.

Import the experimental data for comparison.

- 2 In the Settings window for Table, type Experimental Mole Fractions in the Label text field.
- 3 Locate the Data section. Click Import.
- **4** Browse to the model's Application Libraries folder and double-click the file stefan_tube_exp.csv.

In order to reproduce the plot in Figure 2, do the following:

Mass Fraction (tcs)

- I In the Model Builder window, under Results click Mass Fraction (tcs).
- 2 In the Settings window for ID Plot Group, type Mole Fraction in the Label text field.

Line Graph

- I In the Model Builder window, expand the Results>Mole Fraction node, then click Line Graph.
- 2 Click in the Graphics window and then press Ctrl+A to select all domains.
- 3 In the Settings window for Line Graph, click to expand the Title section.
- 4 Click Replace Expression in the upper-right corner of the y-axis data section. From the menu, choose Model>Component I>Transport of Concentrated Species>tcs.x_wl Mole fraction.
- 5 Locate the y-Axis Data section. Clear the Description check box.
- 6 Locate the Title section. From the Title type list, choose None.
- 7 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 8 In the Expression text field, type x.
- **9** Click to expand the **Coloring and style** section. Locate the **Coloring and Style** section. In the **Width** text field, type **2**.
- 10 Click to expand the Legends section. Select the Show legends check box.
- II From the Legends list, choose Manual.

12 In the table, enter the following settings:

Legends

Acetone

Line Graph 2

- I Right-click Results>Mole Fraction>Line Graph and choose Duplicate.
- In the Settings window for Line Graph, click Replace Expression in the upper-right corner of the y-axis data section. From the menu, choose Model>Component I>
 Transport of Concentrated Species>tcs.x_w2 Mole fraction.
- 3 Locate the Legends section. In the table, enter the following settings:

Legends

Methanol

Line Graph 3

- I Right-click Results>Mole Fraction>Line Graph 2 and choose Duplicate.
- 2 In the Settings window for Line Graph, click Replace Expression in the upper-right corner of the y-axis data section. From the menu, choose Model>Component I> Transport of Concentrated Species>tcs.x_w3 Mole fraction.
- **3** Locate the **Legends** section. In the table, enter the following settings:

Legends

Air

Table Graph 1

- I In the Model Builder window, under Results right-click Mole Fraction and choose Table Graph.
- 2 In the Settings window for Table Graph, locate the Data section.
- 3 From the x-axis data list, choose Column I.
- 4 Locate the Coloring and Style section. Find the Line markers subsection. From the Marker list, choose Cycle.
- 5 Find the Line style subsection. From the Line list, choose None.
- 6 Click to expand the Legends section. Select the Show legends check box.
- 7 From the Legends list, choose Manual.

8 In the table, enter the following settings:

Legends

Acetone exp.

Methanol exp.

Air exp.

Mole Fraction

- I In the Model Builder window, under Results click Mole Fraction.
- 2 In the Settings window for ID Plot Group, locate the Plot Settings section.
- **3** Select the **x-axis label** check box.
- **4** In the associated text field, type Position (m).
- 5 Click to expand the Legend section. From the Position list, choose Upper left.

To reproduce Figure 3, proceed as follows:

I D Plot Group 2

- I On the Results toolbar, click ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Velocity Field in the Label text field.
- 3 Locate the Plot Settings section. Select the x-axis label check box.
- **4** In the associated text field, type Position (m).

Line Graph 1

- I Right-click Velocity Field and choose Line Graph.
- 2 Click in the Graphics window and then press Ctrl+A to select all domains.
- 3 In the Settings window for Line Graph, click Replace Expression in the upper-right corner of the y-axis data section. From the menu, choose Model>Component I> Transport of Concentrated Species>Velocity field>tcs.u Velocity field, x component.
- 4 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- **5** In the **Expression** text field, type **x**.
- 6 Click to expand the Coloring and style section. Locate the Coloring and Style section. In the Width text field, type 2.
- 7 On the Velocity Field toolbar, click Plot.

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